



Final report

## SIM.M.FF-S9.2016

Water flow: 10 m<sup>3</sup>/h ... 130 m<sup>3</sup>/h

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## 1 Summary

The objective of the Supplementary Comparison (SC) SIM.M.FF-S9 for water flow measurement was to support and prove the Calibration and Measurement Capabilities (CMC) of the participating NMIs of Chile (CISA), Peru (INACAL), Bolivia (IBMETRO) and Argentina (INTI). As pilot laboratories, the national metrology institutes of Germany (PTB) and CENAM (Mexico) supported the comparison with reference values. The comparison was organized as a single round robin, started in January 2016 at PTB and finished in August 2019, also at PTB. A combined setup of a turbine meter and Coriolis meter was used as a transfer standard. The nominal calibration conditions of the SC were defined in the flow range between 10 m<sup>3</sup>/h and 130 m<sup>3</sup>/h, 20 °C fluid temperature and 3 bar line pressure.

In order to estimate the uncertainties  $u_{TS}$ , both transfer meter were subjected to extensive characterisation measurements at pilot laboratory PTB. The following parameters were researched in detail: fluid temperature, line pressure, reproducibility, flow stability and meter sensitivity to different inflow conditions. The  $E_N$  values for turbine meter were calculated based on PTB data, only. The  $E_N$  values for Coriolis meter are partly linked to Key Comparison CCM.FF-K1.2015 and were calculated by using a common reference value of PTB and CENAM data.

The uncertainty of turbine meter  $u_{TS}$  was clearly dominated by the sensitivity to disturbed inflow conditions which leads to large values of  $u_{TS}$  with  $> 0.20$  %. Beside one calibration, all labs passed the  $E_N$  criteria of  $\leq 1.20$ . But, due to large values of  $u_{TS}$ , the calibrations for all labs were evaluated as inconclusive. The evaluation criteria  $u_{comp}/u_{base}$  exceeded the critical value of 2.00 for all calibrations. Finally, the turbine meter was not suitable for a confirmation of the submitted CMC values.

The calibration results of Coriolis meter were characterized by a strong dependency on zero setting. The observed effect was adjusted for the data of both reference laboratories by introducing a new method for autozero correction. Maximum uncertainty values for Coriolis  $u_{TS}$  were estimated with 0.069 % at low flowrates and 0.033 % at high flowrates. Beside two calibrations, all laboratories complied with the  $E_N$  criteria of  $< 1.20$ . In contrast to turbine meter, the evaluation criteria  $u_{comp}/u_{base}$  exceeded the critical value of 2.00 at one calibration, only. In consequence, the calibrations by using Coriolis meter were suitable for a confirmation of the submitted CMC values.

In summary, the comparison was successfully finished for a confirmation of the submitted CMC values, related to mass calibrations. For volume related CMC's this comparison was not suitable.

### Acknowledgements

We would like to thank all participants for taking part within this comparison and for their support. This round robin would not be possible without all your help, discussions and organization. Our acknowledgements include all participating staff of the laboratories - scientists, technicians and administration.

A special thank goes to Carl Felix Wolff - (PTB - International Cooperation Department) who supported the comparison by his organizing and his maintaining contact with the partners.

The comparison was partially financially supported by the German Federal Ministry for Economic Cooperation and Development (BMZ) - PNs: 2012.2296.7-95259, 2015.2037.8-95306 and 2017.2073.9-95328.

## 2 Introduction and objective

The objective of the Supplementary Comparison SIM.M.FF-S9 for water flow measurement was to support and prove the Calibration and Measurement Capabilities (CMC) of the participating National Metrology Institutes as part of the CIPM MRA (<http://kcdb.bipm.org>).

The CMC-values of participating laboratories (Table 1) were evaluated by establishing a “Supplementary Comparison Reference Value” (*SCRV*) and the Degree of Equivalence ( $E_N$ ) between laboratories and *SCRV*.

The basic subject of the calibrations was to determine the meter *K*-factor of the transfer flowmeters. Depending on the operating principle of the used transfer meters, following meter-*K*-factors were the subject of measurements and had to be determined during calibrations:

### Meter #1:

**Turbine flowmeter**      volume-related frequency output:  
 $K_V$                       (pulses/unit volume)

### Meter #2:

#### Coriolis flowmeter:

- a)      mass-related frequency output:  
 $K_m$                       (pulses/unit mass)
- b)      volume-related frequency output:  
 $K_V$                       (pulses/unit volume)

## 3 Participants and measurement schedule

Participant list and measurement schedule are presented in Table 1. After three years of preparation, the comparison officially started in January 2016.

**Table 1:** Participant list and measurement periods of standard calibration program (day #1 until day #3 of Table 4), \* pilot laboratories. Additional calibrations at pilot laboratory PTB are listed in Table 6.

NMI	Country	RMO	Contact	Calibration period
PTB*	Germany	EURAMET	enrico.frahm@ptb.de	13.01. - 15.01.2016
CISA	Chile	SIM	j.vargas@ci-sa.com	28.04. – 04.05.2016
INACAL	Peru	SIM	cochoa@inacal.gob.pe	13.03. – 16.03.2017
IBMETRO	Bolivia	SIM	fespejo@ibmetro.org	01.03. – 05.03.2018
INTI	Argentina	SIM	marsil@inti.gob.ar	06.12. – 14.12.2018
CENAM*	Mexico	SIM	rarias@cenam.mx	03.06. – 05.06.2019
PTB*	Germany	EURAMET	enrico.frahm@ptb.de	08.08. – 12.08.2019

## 4 Description of the transfer standard

### 4.1 Transfer meter setup

The transfer meter setup (Figure 1) consisted a turbine flowmeter (Figure 2) at the inflow and a Coriolis flowmeter (Figure 3) at the outflow. The technical details of the meters are listed in Table 2 and Table 3. For flow conditioning, tube bundles were installed before and after turbine meter. Beside the two transfer flowmeters, all additional items were provided by pilot laboratory (PTB):

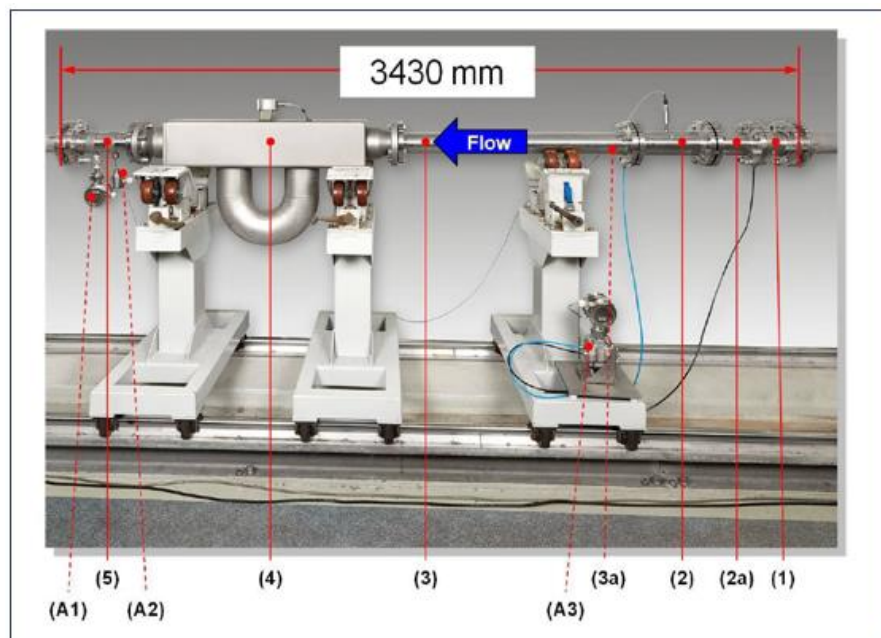
- Pipework for meter installation (Figure 4)
- Cables for connecting transfer meters and the auxiliary devices to electronic boxes
- Electronic box (Figure 5).

In order to provide optimum reproducibility conditions, the flowmeters and the inter-connecting pipework were equipped with pin-in-hole alignment capabilities. All elements of pipework were manufactured in stainless steel.

In addition to the used flowmeters, auxiliary measurands for diagnostic purposes were included in the transfer meter setup:

- Water density (based on a signal delivered by the Coriolis flowmeter)
- Fluid temperature by temperature transmitter
- Fluid pressure by pressure transmitter
- Pressure drop across the turbine meter by differential pressure transmitter

A detailed description of the setup is given in the Technical Protocol of this SC [1].

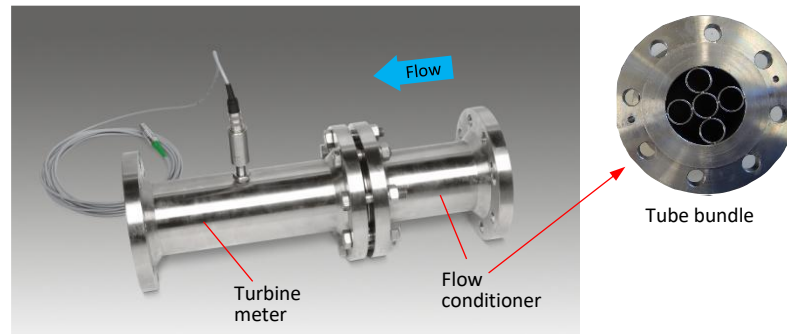


**Figure 1:** Transfer meter setup and pipework - Sample installation at pilot laboratory

- |  |  |
|--|--|
| (1) Inlet pipe section                                     | (2) Turbine meter                            |
| (2a) Tube-bundle flow conditioner dedicated to the turbine |  |
| (3) Connecting pipe section                                | (3a) Integrated tube-bundle flow conditioner |
| (4) Coriolis flowmeter                                     | (5) Outlet pipe section                      |

*Auxiliary devices:*

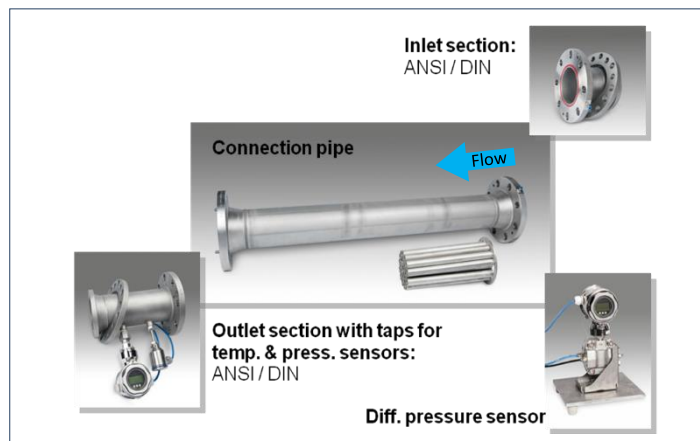
- (A1) Pressure transmitter
- (A2) Temperature transmitter
- (A3) Differential pressure transmitter



**Figure 2:** Transfer meter #1 - Turbine meter, DN80 mm



**Figure 3:** Transfer meter #2 - Coriolis flowmeter, DN80 mm



**Figure 4:** Transfer setup – pipework

**Table 2:** Transfer meter #1 - Turbine flowmeter (Figure 2)

<b>Manufacturer:</b>	KEM Küppers Elektromechanik GmbH	Germany
<b>Type:</b>	HM 080.71.FDE040-TS15-D	
<b>Serial No.:</b>	01130721	
<b>Pipe size:</b>	DN80	Nominal: 80 mm
<b>Signal pick-up:</b>	Type: VTE*/P-Ex Carrier-frequency pulse amplifier Serial No.: 02497623	Signal voltage: ca. 24 V
<b>Output signal:</b>	Frequency	(0 Hz) ... 450 Hz (at 240 m <sup>3</sup> /h)
	Nominal meter <i>K</i> -factor: $K_{v,nom}$	11.4850 pulses/L
<b>Additional equipment:</b>	Tube-bundle flow conditioner	Permanently installed at the inflow to meter

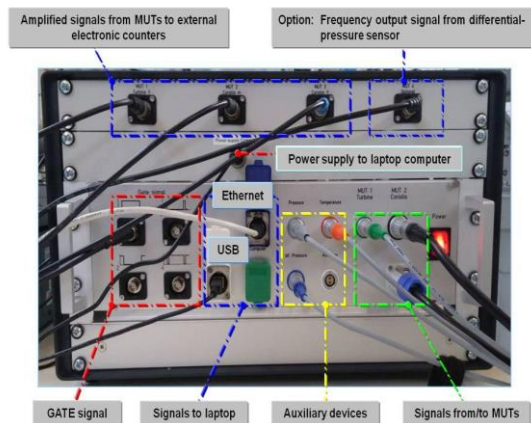
**Table 3:** Transfer meter #2 - Coriolis flowmeter (Figure 3)

<b>Manufacturer:</b>	Rota Yokogawa GmbH & Co KG	Germany
<b>Type:</b>	ROTAMASS	
<b>Serial No.:</b>	D1K601386 (flow sensor) D1K601375 (flow transmitter and indicator)	
<b>Pipe size:</b>	DN80	Nominal: 80 mm
<b>Signal output #1:</b>	Mass-flowrate related: frequency	0 kHz ... 10 kHz
	Nominal meter K-factor: $K_{m,nom}$	144.056 pulses/kg
<b>Signal output #2:</b>	Volume-flowrate related: frequency	0 kHz ... 10 kHz
	Nominal meter K-factor: $K_{v,nom}$	28.800 pulses/L
<b>Signal output #3:</b>	Fluid density: current signal	4 mA ... 20 mA

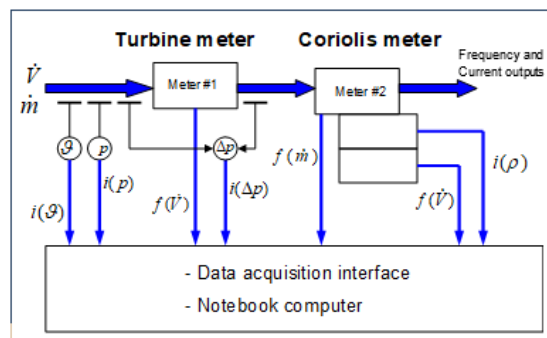
## 4.2 Additional data logging

For the reported SC an additional datalogging system was designed. Beside standard impulse logging of the laboratory, an electronic device was provided by the pilot laboratory (PTB) for a separate and independent data recording. Basically, electric pulses from transfer meters and additional process parameter, measured by the auxiliary devices (chapter 4.1), were logged by the electronic box (Figure 5). Also, power supply of the measurement instruments was provided by the box. The detailed use of the electronic box is described in SC Technical Protocol [1].

The electronic box was developed as a parallel working system, which does not affect the standard impulse count recording of the laboratories.



**Figure 5:** Front side of the electronic box - Connectivity to MUTs, external electronic counters and laptop computer



**Figure 6:** Electronic box - signal acquisition

## 5 Measurement program

### 5.1 Calibration program at participating laboratories

The objective of the measurement program was to verify the CMC entries of the participating laboratories. Therefore, it was necessary for all laboratories to calibrate the setup under comparable measurement conditions. All participants were asked to calibrate the transfer setup as far as possible under the following SC reference conditions.

**SC reference conditions:**

**Fluid temperature:** 20 °C

**Line pressure:** 3 bar (measured as positive back pressure after Coriolis meter)

**Nominal flowrates:** listed in Table 4

**Setup:** using the complete SC setup (Figure 1).

**Table 4:** Main tasks and flowrates of calibration days in participating laboratories as defined in SC Technical Protocol [1]

Calibration day	Main task	Preparations before calibration	Autozero setting at Coriolis meter	Repeated measurements	Nominal flowrate	Post-processing
					m <sup>3</sup> /h	
Day #1	Lab-to-lab reproducibility	Installation of transfer meters	yes	5	10, 30, 60, 100, 130	Transfer package remains in calibration line
Day #2	Main calibration of KC1 and Day-to-day reproducibility	-	no	5	10, 30, 60, 100, 130	Transfer package remains in calibration line
Day #3	Repeatability at selected flowrates	-	no	10	30, 60, 130	Transfer package is removed from calibration line

### 5.2 Calibration methods and uncertainties of participating laboratories

During SC each laboratory had to calibrate the setup by using their standard calibration method, which was subjected to the CMC entry (Table 5). Each laboratory provided the pilot laboratory with a description of the calibration procedure and an overview to the used calibration rig (Chapter 11.1.) All laboratories had an independent traceability in realization of their standards.

**Table 5:** Participating laboratories, calibration methods and CMC-values within the range of SC flowrates

NMI/DI	Country	Calibration method and reference	CMC Water CIPM MRA Database ( $k = 2$ )	
			$U(\text{Mass})$	$U(\text{Volume})$
			%	%
PTB	Germany	Gravimetric / flying-start-stop	0.020	0.020
CISA	Chile	Gravimetric / flying-start-stop	0.150	0.150
INACAL	Peru	Gravimetric / flying-start-stop	0.076	0.076
IBMETRO	Bolivia	Master meter / flying-start-stop	0.100	0.100
INTI	Argentina	Volumetric tank / standing-start-stop (10 m <sup>3</sup> /h until 60 m <sup>3</sup> /h)	0.070	0.060
		Master meter / standing-start-stop (100 m <sup>3</sup> /h until 130 m <sup>3</sup> /h)	0.220	0.200
CENAM	Mexico	Gravimetric / flying-start-stop	0.030	0.038

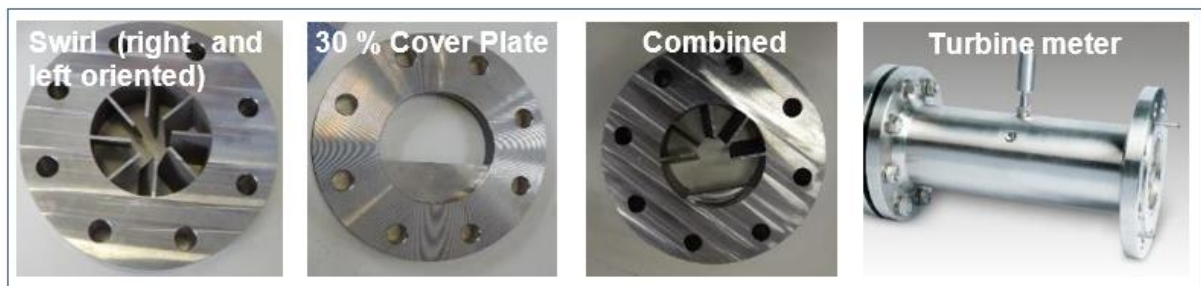


### 5.3 Meter characterisation at pilot laboratory (PTB)

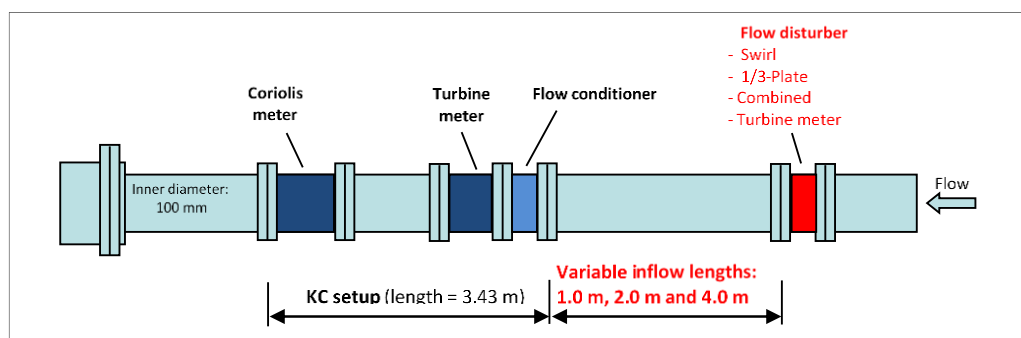
The transfer setup was subjected to extensive characterisation measurements at pilot laboratory (Table 6). These calibrations were made under clearly defined conditions, which are basically derived from SC reference conditions (Chapter 5.1). The goal of the characterisation measurements was to analyze the impact of the following parameters to transfer meter setup: fluid temperature, line pressure and reproducibility. The results aimed in a detailed knowledge about meter uncertainties  $u_{TS}$ . Additionally, a strong dependency of turbine meter characteristics to different inflow condition was assumed (Chapter 7.6). In order to consider this type of effects, data of KC1 calibrations were used within the presented SC report. During KC1 calibration an identical turbine meter was used, but with an inner diameter of 100 mm instead of 80 mm. For a simulation of real inflow conditions, the KC1 transfer setup was calibrated with several flow disturber (Figure 7) and different inflow lengths (Figure 8).

**Table 6:** Characterisation measurements at pilot laboratory

Task of calibrations	Nominal flowrate	Temperature	Line pressure	Repeated measurements	Measurement periods at pilot laboratory
	m <sup>3</sup> /h	°C	bar		
Temperature dependency	10, 30, 60, 100, 130, 150	10, 15, 20, 25, 30	3	5	16.06.2015 - 02.07.2015
Pressure dependency	10, 30, 60, 100, 130, 150	20	2, 3, 4	5	01.09.2015 - 03.09.2015
Long term reproducibility	10, 30, 60, 100, 130	20	3	5	25.11.2015
Inflow conditions (with DN100 setup of KC1)	30, 100, 200	20	3	5	03/2019 during KC1 calibrations



**Figure 7:** Used flow disturber for meter characterisation during KC1 - inner pipe diameter: 100 mm



**Figure 8:** Calibration setup for meter characterisation during KC1 using several flow disturber and inflow lengths

## 6 Data calculation and evaluation criteria

### 6.1 Meter $K$ -factor and temperature correction for final meter error $x_i$

According to the flowrates of Table 4, the meter  $K$ -factor was calculated for each calibration by using Equation (1) for turbine meter and, respectively, by Equation (2) for Coriolis meter.

$$K_V = \frac{N}{(V_{ref} \cdot 1000)} \quad (1)$$

$$K_m = \frac{N}{m_{ref}} \quad (2)$$

where	$K_V$	- $K$ -factor of turbine meter (pulses/L)
	$K_m$	- $K$ -factor of Coriolis meter (pulses/kg)
	$N$	- Counted number of pulses by the transfer meter (pulses)
	$V_{ref}$	- Volume, measured by the reference standard (m <sup>3</sup> )
	$m_{ref}$	- Mass, measured by the reference standard (kg)

The relative measurement error  $e$  was calculated for each  $K$ -factor by:

$$e_V = \frac{K_V - K_{V,nom}}{K_{V,nom}} \cdot 100 \% \quad (3)$$

$$e_m = \frac{K_m - K_{m,nom}}{K_{m,nom}} \cdot 100 \% \quad (4)$$

where	$e_V$	- Relative measurement error of turbine meter – volume (%)
	$e_m$	- Relative measurement error of Coriolis meter - mass (%)
	$K_{V,nom}$	- Nominal $K$ -factor of turbine meter (pulses/L)
	$K_{m,nom}$	- Nominal $K$ -factor of Coriolis meter - mass output (pulses/kg)

### 6.2 Postprocessing of reported data and estimation of relative meter error $x_i$

#### Autozero correction of Coriolis data

The data of Coriolis meter were characterized by a strong drift in meter error. Especially at low flowrates, the meter showed differences of up to 1.33 % between calibration periods 2016 and 2019 (Figure 9). This observed drift was interpreted as an instability of meter autozero setting, which was confirmed by manufacturer of the meter [2]. Data of the turbine meter, which were recorded at the same time, did not show such a highly drift at low flowrates (Figure 13). Additionally, the recorded autozero value of the Coriolis meter was +59.615 kg/h during calibrations in 2016 and, respectively, -92.115 kg/h in 2019, which do underline the discussed autozero instability.

In consequence, a correction of Coriolis data was introduced as followed. The differences between flowrates of Coriolis meter and lab reference were calculated and plotted against reference flowrate itself (Figure 10). The interception term of the fitted linear function was detected as the "zero missetting" value, separately for **each** calibration day, but over full flow scale (Table 7). The original flowrates of Coriolis meter were corrected by this method and a new meter error was calculated (Figure 11).

This method is based on the following two assumptions: The Coriolis meter is a linear device and the non-linear characteristics of the results in Figure 9 were not caused by leakage effects of the calibration facility. Both pilot laboratories can guarantee the nonexistence of leakage during reported calibrations, which was verified by previous comparisons (e.g. CCM-K1.2015). In consequence, the **correction method was only applied to the results of pilot laboratories**.

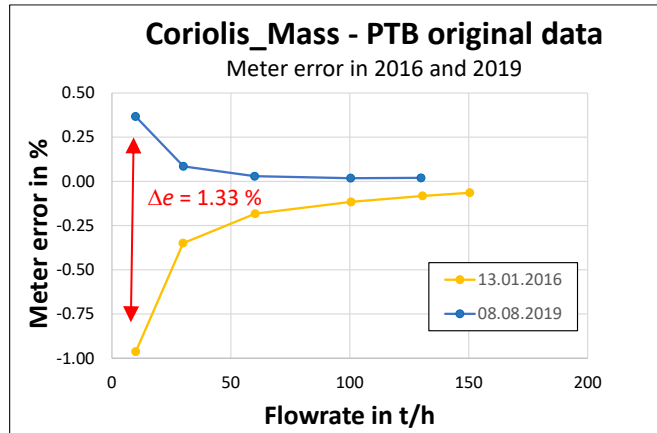


Figure 9: Meter drift of Coriolis\_Mass - original PTB data of day #1 in 2016 and 2019

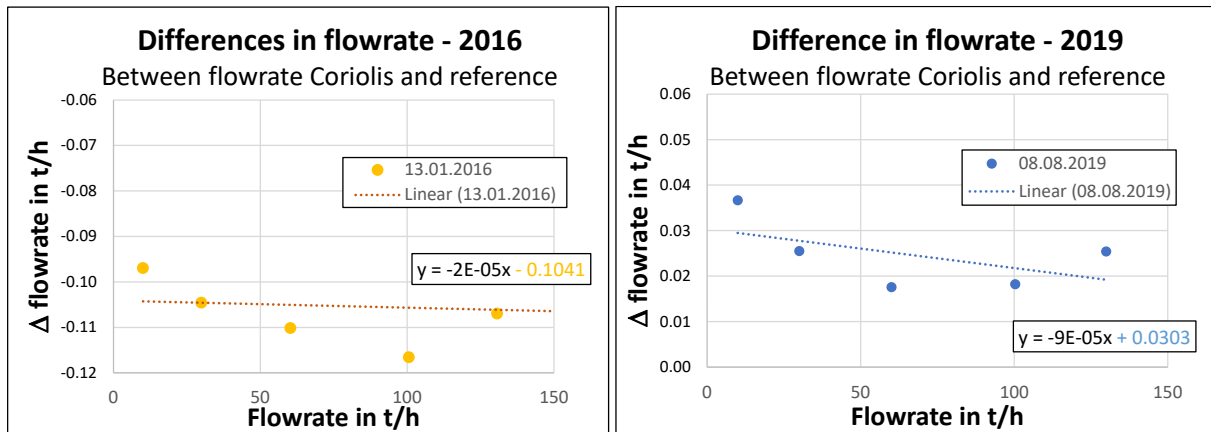


Figure 10: Example of differences in flowrate between Coriolis and reference data - original PTB data of day #1 in 2016 and 2019; interception value of fitted linear function for correction of Coriolis data

Table 7: Correction values for Coriolis\_Mass data, based on autozero discussion and estimated interception, e.g. in Figure 10

Pilot laboratory and calibration period	Correction value for Coriolis_Mass flowrate		
	Day #1	Day #2	Day #3
	t/h	t/h	t/h
PTB_1 in 01/2016	-0.104	-0.084	-0.068
PTB_2 in 08/2019	0.030	0.039	0.065
CENAM in 06/2019	-0.003	-0.008	-0.015

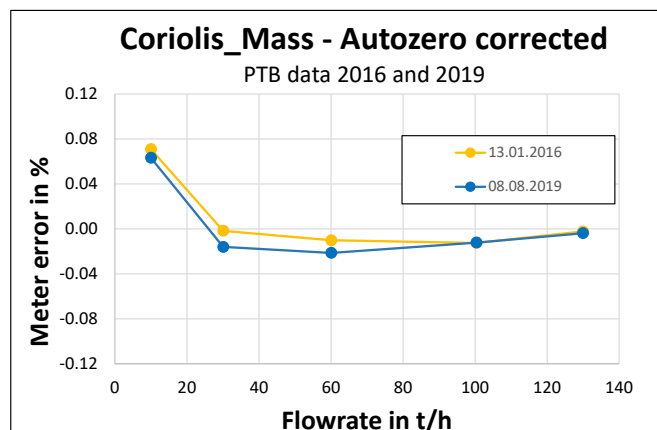


Figure 11: Example of autozero corrected final Coriolis\_Mass data - PTB of day #1 in 2016 and 2019

### Temperature correction

Both transfer meters showed a systematic temperature dependency in meter error (Section 7.3). All reported meter error of participated laboratories, including autozero corrected data of pilot laboratories, were corrected by applying Equation (22) until Equation (25) and Table 15, to aim a temperature corrected meter error  $e_{v,cor}$  for volume and  $e_{m,cor}$  for mass.

For final evaluation by  $E_N$  values, a mean meter error ( $x_i$ ) was calculated separately for each laboratory, transfer meter and flowrate (Equation 5), based on calibration results of day #1 and day #2 (Table 4).

$$x_i = \frac{\sum_{k=1}^n (e_{cor,k})}{n} \quad (5)$$

where

- $x_i$  - Temperature corrected meter error for  $E_N$ -value evaluation
- $n$  - Number of measurements at calibrated test point
- $i$  - Laboratory index

### 6.3 Uncertainty $u_{x,i}$ of reported and temperature corrected values $x_i$

As described in [2], [3] and [4], the uncertainty of reported values  $x_i$  include uncertainties introduced by the participant's flow reference ( $u_{base,i}$ ), by transfer meter ( $u_{TS}$ ) and by repeatability of the reported values (Equation 6). The used input parameter of  $u_{base,i}$  do represent the CMC values of Table 5 which were under evaluation during this comparison. Uncertainty calculations of  $u_{TS}$  were based on Equation (18), for Turbine meter, respectively, for Coriolis meter on Equation (19). Final values of  $u_{TS}$  are given in Table 10 and Table 11. The term  $\frac{s}{\sqrt{n}}$  (Equation 6) represents the repeatability of measurements made in the participating laboratory [3], based on calibration results of day #1 and day #2 (Table 4).

$$u_{x,i} = \sqrt{u_{base,i}^2 + u_{comp}^2} = \sqrt{u_{base,i}^2 + u_{TS}^2 + \frac{s^2}{n}} \quad (6)$$

where

- $u_{x,i}$  - Uncertainty of reported and temperature corrected meter error (%)
- $u_{base,i}$  - Uncertainty of laboratory reference, here it is equal to CMC<sub>i</sub> (%)
- $u_{comp}$  - Uncertainty of transfer meter measurements (%)
- $u_{TS}$  - Uncertainty of transfer meter (%)
- $s$  - Standard deviation of the mean of measurements at one flowrate point (%)

All values of  $u$  are valid for  $k = 1$ .

## 6.4 Coriolis meter - Method for $E_N$ value calculation and linkage to KC1

### 6.4.1 Linkage of SIM comparison to Key Comparison KC1

The evaluation of Coriolis data is partly based on a linkage to key comparison CCM.FF-K1.2015 (KC1). The pilot laboratories CENAM and PTB took part in KC1 and supported the presented SIM comparison by the higher-ordered results of KC1 (Figure 12). The applied procedure is described in follow and was applied for Coriolis\_Mass data only.

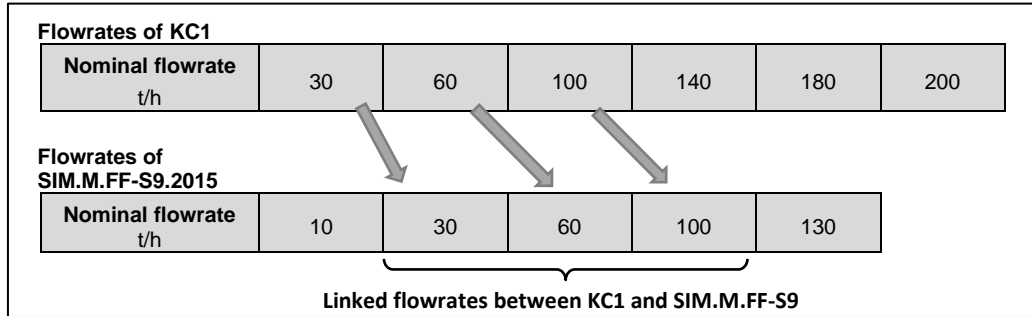


Figure 12: Linkage between comparison KC1 and SIM.M.FF-S9

### SCC<sub>i</sub> - Supplementary comparison correction value

$$SCC_i = x_{KC1,i} - KCRV \quad (7)$$

where

- $SCC_i$  - Supplementary comparison correction for laboratory  $i$  (%)
- $KCRV$  - Key Comparison Reference value of KC1 (%)
- $x_{KC1,i}$  - Results of laboratory  $i$  during KC1 (%)

### Uncertainty of SCC<sub>i</sub>

$$u(SCC_i) = \sqrt{u_{x,KC1,i}^2 - u_{KCRV}^2} \quad (8)$$

where

- $u_{SCC,i}$  - Uncertainty of SCC for laboratory  $i$  (%)
- $u_{x,KC1,i}$  - Uncertainty of calibration results of laboratory  $i$  during KC1 (%)
- $u_{KCRV}$  - Uncertainty of KCRV during KC1 (%)

Table 8: Input parameter and results of SCC<sub>i</sub> for PTB, based on KC1 data

Nominal Flowrate	KCRV	$u(KCRV)$	$x_{KC1,i}$	$u(x_{KC1,i})$	SCC <sub>i</sub>	$u(SCC_i)$
		$k = 1$		$k = 1$		$k = 1$
t/h	%	%	%	%	%	%
30	0.041	0.010	0.045	0.024	0.004	0.022
60	0.038	0.007	0.041	0.016	0.004	0.014
100	0.033	0.006	0.032	0.014	-0.001	0.013

Table 9: Input parameter and results of SCC<sub>i</sub> for CENAM, based on KC1 data

Nominal Flowrate	KCRV	$u(KCRV)$	$x_{KC1,i}$	$u(x_{KC1,i})$	SCC <sub>i</sub>	$u(SCC_i)$
		$k = 1$		$k = 1$		$k = 1$
t/h	%	%	%	%	%	%
30	0.041	0.010	0.047	0.027	0.006	0.025
60	0.038	0.007	0.049	0.019	0.012	0.018
100	0.033	0.006	0.045	0.018	0.012	0.017

#### 6.4.2 Supplementary Comparison reference value $SCRV_{Cor}$ and its uncertainty

The Supplementary Comparison Reference Value for Coriolis\_Mass data was calculated following the procedure A of [6]:

##### Input data and uncertainties at linked flowrates of 30 t/h, 60 t/h and 100 t/h:

- ⇒ original data of CENAM and PTB were corrected by using  $SCC_i$  (Equation 9)
- ⇒ the uncertainties of the corrected value were calculated by using (Equation 10)

##### Input data and uncertainties at flowrates of 10 t/h and 130 t/h:

- ⇒ the results of equation (5) were used as  $x_{Cor,i}$
- ⇒ the uncertainties of equation (5) were used as  $u(x_{Cor,i})$

$$x_{Cor,i} = x_i - SCC_i \quad (9)$$

where  $x_{Cor,i}$  - By  $SCC_i$  corrected results of reference laboratory  $i$  during SIM comparison (%)

$$u(x_{Cor,i}) = \sqrt{u_{x,i}^2 + u_{SCC,i}^2} \quad (10)$$

where  $u(x_{Cor,i})$  - Uncertainty of  $x_{Cor,i}$  for reference laboratory  $i$  during SIM comparison (%)

The reference value  $SCRV_{Cor}$  was calculated for each flowrate as a weighted mean error of both reference laboratories, including standard uncertainties  $u(x_{Cor,i})$  of the measurements as the weights:

$$SCRV_{Cor} = \frac{\left( \frac{x_{Cor,i}}{u_{x,Cor,i}^2} + \frac{x_{Cor,j}}{u_{x,Cor,j}^2} \right)}{\left( \frac{1}{u_{x,Cor,i}^2} + \frac{1}{u_{x,Cor,j}^2} \right)} \quad (11)$$

where  $SCRV_{Cor}$  - Reference value of the comparison for Coriolis\_Mass meter (%)

The standard uncertainty  $u(SCRV_{Cor})$  is given with:

$$\frac{1}{u_{SCRV,Cor}^2} = \frac{1}{u_{x,Cor,i}^2} + \frac{1}{u_{x,Cor,j}^2} \quad (12)$$

where  $u(SCRV_{Cor})$  - Standard uncertainty of  $SCRV_{Cor}$  with  $k = 1$  (%)

In equations 11 and 12,  $i$  stands for PTB and  $j$  for CENAM.

#### 6.4.3 Determination of $d_i$ and $E_N$ -values

The differences of participating laboratories to  $SCRV_{Cor}$  were calculated with Equation (13), the extended uncertainty of the difference with Equation (14). The final  $E_N$  values for comparison evaluation were calculated by using Equation (15).

$$d_i = SCRV_{Cor} - x_i \quad (13)$$

where  $d_i$  - Degree of equivalence (DoE) as the difference of SIM-participant  $i$  to  $SCRV_{Cor}$  (%)

##### Uncertainty of $d_i$

$$U(d_i) = 2 \cdot \sqrt{u_{x,i}^2 + u_{SCRV,Cor}^2} \quad (14)$$

where  $U(d_i)$  - Uncertainty of  $d_i$  of participant  $i$  during SIM comparison with  $k = 2$  (%)

##### $E_{N,i}$ - value of participant

$$E_{N,i} = d_i / U(d_i) \quad (15)$$

where  $E_{N,i}$  - Normalized Degree of Equivalence as the difference of SIM-participant  $i$  to  $SCRV_{Cor}$  (%)

## 6.5 Turbine meter - Method for $E_N$ value calculation

### 6.5.1 Supplementary Comparison reference value $SCRV_{Turb}$ and its uncertainty

The Supplementary Comparison Reference Value  $SCRV_{Turb}$  for turbine meter is based on PTB data as the reference laboratory, only. Over full flow scale, the calibration results  $x_i$  (Equation 5) of PTB were used as  $SCRV_{Turb}$  as well as the uncertainty  $u(x_i)$  of PTB-data (Equation 6) were used as  $u(SCRV_{Turb})$ .

### 6.5.2 Determination of $d_i$ and $E_N$ -values

The differences of participants to  $SCRV_{Turb}$  were calculated with Equation (13), the expanded uncertainty of the difference with Equation (17). The final  $E_N$  values for comparison evaluation were calculated by using Equation (15).

$$d_i = SCR_{V_{Turb}} - x_i \quad (16)$$

where  $d_i$  - difference of SIM-participant  $i$  to  $SCR_{V_{Turb}}$  %

$$U(d_i) = 2 \cdot \sqrt{u_{x,i}^2 + u_{SCR_{V_{Turb}}}^2} \quad (17)$$

where  $U(d_i)$  - Uncertainty of  $d_i$  of participant  $i$  during SIM comparison with  $k = 2$  (%)

## 6.6 Evaluation criteria of comparison data

For final data evaluation and decision table the following criteria were used - based on [3], [4] and [5]:

- The participant **passed the comparison** if  $E_{N,i} \leq 1.0$  and  $u_{comp}/u_{base} \leq 2$   
The results of participating laboratory  $i$  agreed within 95 % confidence level uncertainty expectations with the  $SCRV$  ( $k = 2$ ).
- The participant passed the comparison at **“warning level”** if  $1.0 < E_{N,i} \leq 1.2$  and  $u_{comp}/u_{base,i} \leq 2$
- The comparison can not confirm the participant’s uncertainty if  $E_{N,i} \leq 1.2$  and  $u_{comp}/u_{base,i} > 2$   
The results were **inconclusive**, because the calibrations did not show sufficient low uncertainties to discern lab to  $SCRV$  below certain level. The transfer meter and/or the calibrations were not suitable for a confirmation of the declared CMC values.
- The participant **failed the comparison** if  $E_{N,i} > 1.2$   
The results did indicate that the agreement was outside of uncertainty expectations.

## 7 Laboratory conditions, transfer meter characteristics and meter uncertainties

In accordance to the WGFF recommendation for comparison calculations [4], the standard uncertainty  $u_{TS}$  of the transfer meter is the root-sum-of-square (RSS) of several transfer meter characteristics. For this comparison the considered meter characteristics and input uncertainties of turbine meter are given in Equation (18), for Coriolis meter in Equation (19). The final values of  $u_{TS}$  were calculated separately for each flowrate (Table 10 and Table 11).

**Note:** The uncertainties of  $u_{TS}$  are specified and valid for the presented comparison under the given measurement conditions. The values of  $u_{TS}$  may change if the setup or calibration conditions do deviate to this comparison.

$$\text{Turbine meter: } u_{TS} = \sqrt{u_{\text{drift}}^2 + u_{\text{reprod}}^2 + u_{\text{temp}}^2 + u_{\text{pres}}^2 + u_{\text{flow}}^2 + u_{\text{inflow}}^2} \quad (18)$$

$$\text{Coriolis}_{\text{Mass}}: u_{TS} = \sqrt{u_{\text{drift}}^2 + u_{\text{reprod}}^2 + u_{\text{temp}}^2 + u_{\text{pres}}^2 + u_{\text{flow}}^2} \quad (19)$$

where

- $u_{\text{drift}}$  - Uncertainty due to drift of transfer meter (%)
- $u_{\text{reprod}}$  - Uncertainty due to reproducibility characteristics of transfer meter (%)
- $u_{\text{temp}}$  - Uncertainty caused by temperature characteristics of transfer meter (%)
- $u_{\text{pres}}$  - Uncertainty caused by pressure characteristics of transfer meter (%)
- $u_{\text{flow}}$  - Uncertainty due to sensitivity of transfer meter to instable flow conditions (%)
- $u_{\text{inflow}}$  - Uncertainty due to sensitivity of turbine meter to different inflow conditions (%)

All values of  $u$  are expressed as  $k = 1$ .

**Table 10:** Final values of meter uncertainties  $u_{TS}$  for turbine meter (with  $k = 1$ )

Nominal flowrate	Meter uncertainty $u_{TS}$ for turbine meter	Input uncertainties for $u_{TS}$					
		$u_{\text{drift}}$	$u_{\text{reprod}}$	$u_{\text{temp}}$	$u_{\text{pres}}$	$u_{\text{flow}}$	$u_{\text{inflow}}$
m <sup>3</sup> /h	%	%	%	%	%	%	%
10	0.207	0.034	0.010	0.014	0.017	0.006	0.203
30	0.207	0.034	0.007	0.009	0.017	0.006	0.203
60	0.211	0.057	0.003	0.002	0.017	0.006	0.203
100	0.215	0.071	0.004	0.001	0.017	0.006	0.203
130	0.219	0.080	0.005	0.000	0.017	0.006	0.203

**Table 11:** Final values of meter uncertainties  $u_{TS}$  for Coriolis\_Mass (with  $k = 1$ )

Nominal flowrate	Meter uncertainty $u_{TS}$ for Coriolis_Mass meter	Input uncertainties for $u_{TS}$				
		$u_{\text{drift}}$	$u_{\text{reprod}}$	$u_{\text{temp}}$	$u_{\text{pres}}$	$u_{\text{flow}}$
t/h	%	%	%	%	%	%
30	0.069	0.040	0.024	0.043	0.029	0.006
60	0.056	0.010	0.010	0.045	0.029	0.006
100	0.035	0.008	0.010	0.013	0.029	0.006
140	0.032	0.006	0.009	0.004	0.029	0.006
180	0.033	0.010	0.010	0.006	0.029	0.006



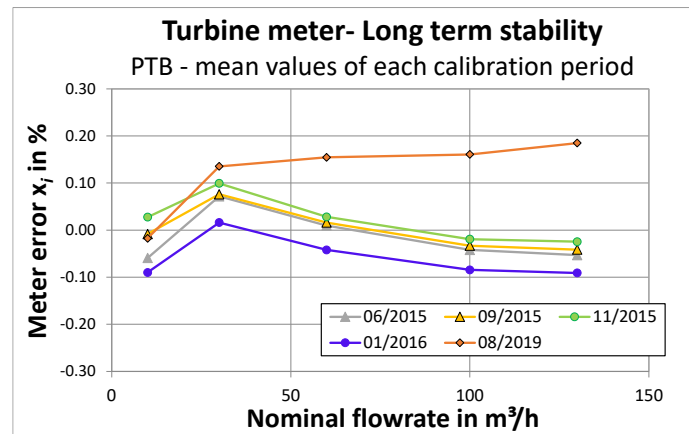
## 7.1 Drift of transfer meter - uncertainty $u_{drift}$

The uncertainty due to meter drift  $u_{drift}$  was quantified by performing repeated calibrations at pilot laboratory #1 (Table 1 and Table 6), using the reference standard as described in Figure 1 under reference conditions of 3 bar and 20 °C fluid temperature. For each calibration period a mean value was calculated (Figure 13 and Figure 14). The final values of  $u_{drift}$  (Table 12) were calculated by using Equation (20), separately for each flowmeter and flowrate.

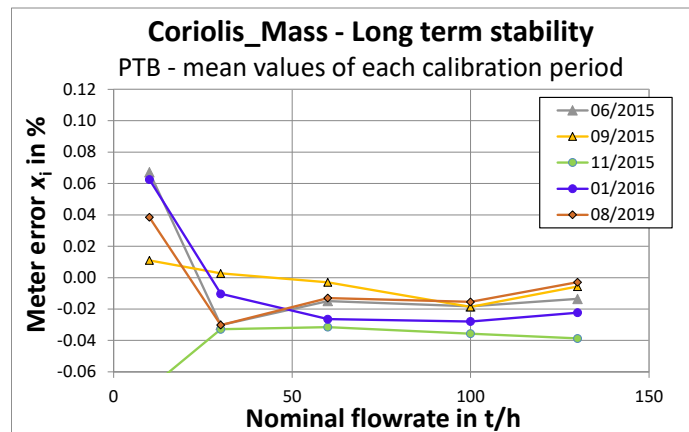
$$u_{drift} = \frac{Max(x_i) - Min(x_i)}{2 \cdot \sqrt{3}} \quad (20)$$

where

$u_{drift}$  - Uncertainty ( $k = 1$ ) due to long term stability of transfer meter (%)  
 $x_i$  - Averaged and corrected meter error (%)



**Figure 13:** Long term stability of turbine meter - Mean values of corrected meter error  $x_i$  for each calibration period, measured at PTB laboratory under reference conditions of 3 bar line pressure and 20 °C fluid temperature



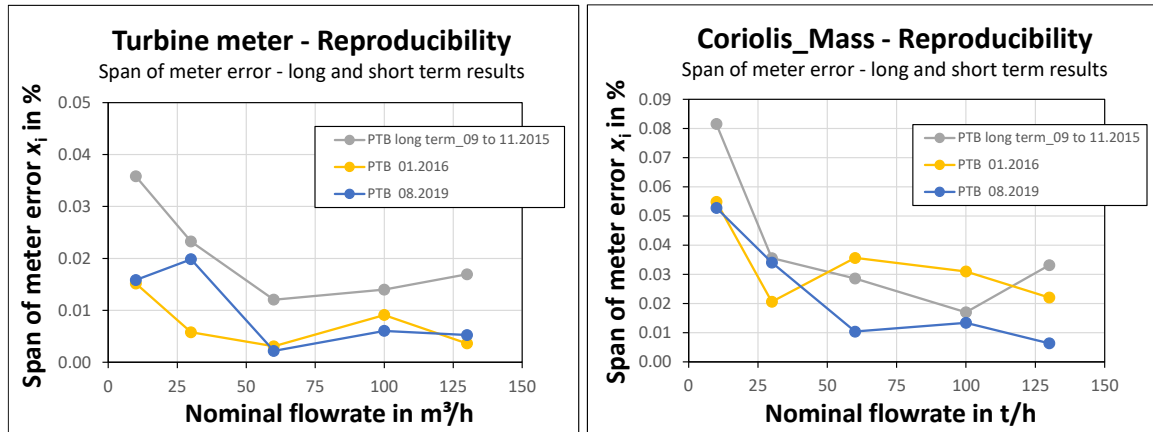
**Figure 14:** Long term stability of Coriolis\_Mass - Mean values of corrected meter error  $x_i$  for each calibration period, measured at PTB laboratory under reference conditions of 3 bar line pressure and 20 °C fluid temperature

**Table 12:** Uncertainties  $u_{drift}$  caused by drift of meter error – turbine meter and Coriolis\_Mass

	Nominal Flowrate				
	10 m <sup>3</sup> /h	30 m <sup>3</sup> /h	60 m <sup>3</sup> /h	100 m <sup>3</sup> /h	130 m <sup>3</sup> /h
$k = 1$					
$u_{drift}$ Turbine meter in %	0.034	0.034	0.057	0.071	0.080
$u_{drift}$ Coriolis_Mass in %	0.040	0.010	0.008	0.006	0.010

## 7.2 Quantification of reproducibility - uncertainty $u_{\text{reprod}}$

The uncertainty due to reproducibility characteristics  $u_{\text{reprod}}$  of the transfer meter were estimated at pilot laboratory, based on maximum values of long- and short-term reproducibility. For each period, a span of meter error  $[\text{Max}(x_i) - \text{Min}(x_i)]$  was calculated (Figure 15). Because of non-normal distributed data, the uncertainty  $u_{\text{reprod}}$  was calculated separately for each flow rate by using maximum values of observed span (Equation 21). It was assumed that the final values of  $u_{\text{reprod}}$  (Table 13) did include the following sources of uncertainty: short term drift between calibration day #1 until day #3, residual uncertainty after correction of autozero (at Coriolis meter) and reassembly of the transfer setup.



**Figure 15:** Results of reproducibility calibrations at pilot laboratory – Span of corrected meter error  $x_i$  (max - min) during each calibration period - measured at PTB laboratory under reference conditions of 3 bar line pressure and 20 °C fluid temperature

$$u_{\text{reprod}} = \frac{\text{Max} [\text{Max}(x_i) - \text{Min}(x_i)]}{2 \cdot \sqrt{3}} \quad (21)$$

where  $u_{\text{reprod}}$  - Uncertainty ( $k = 1$ ) due to reproducibility characteristics of transfer meter (%)

**Table 13:** Uncertainties  $u_{\text{reprod}}$  due to reproducibility characteristics of the transfer meters

$k = 1$	Nominal Flowrate				
	10 m <sup>3</sup> /h	30 m <sup>3</sup> /h	60 m <sup>3</sup> /h	100 m <sup>3</sup> /h	130 m <sup>3</sup> /h
$u_{\text{reprod}}$ Turbine meter in %	0.010	0.007	0.003	0.004	0.005
$u_{\text{reprod}}$ Coriolis_Mass in %	0.024	0.010	0.010	0.009	0.010

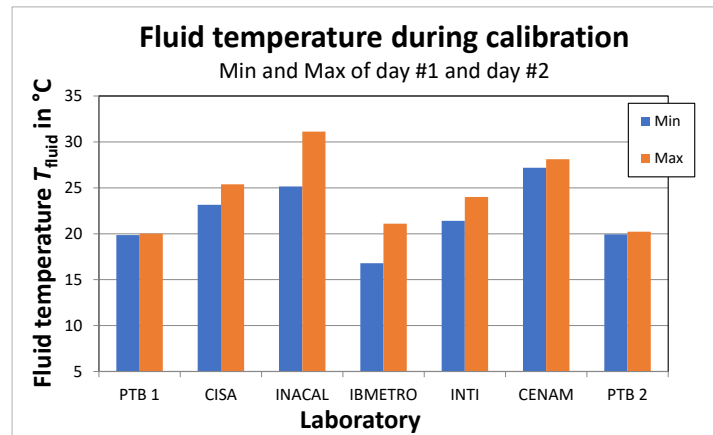
### 7.3 Temperature dependency - uncertainty $U_{temp}$

#### Laboratory conditions

During calibrations in participating laboratories, the span of fluid temperature ranged between 16.80 °C and 31.13 °C. The maximum variation of fluid temperature within one participating lab, expressed as  $\max(T_{fluid}) - \min(T_{fluid})$ , was reported with 5.99 °C (Table 14, Figure 16).

**Table 14:** Fluid temperatures  $T_{fluid}$  (°C) in participating laboratories during calibrations

NMI	PTB 1	CISA	INACAL	IBMETRO	INTI	CENAM	PTB 2
Max	20.01	25.39	31.13	21.10	24.00	28.12	20.22
Min	19.85	23.16	25.15	16.80	21.40	27.19	19.94
Max - Min	0.16	2.23	5.99	4.30	2.60	0.93	0.28
Mean	19.92	24.29	28.02	18.73	22.77	27.65	20.06



**Figure 16:** Fluid temperature  $T_{fluid}$  during calibrations in participating laboratories - Maximum and minimum of calibration on day #1 and day #2

#### Meter characteristics

The temperature characterisation measurements were realised in pilot laboratory (PTB) in 2015. The goal of characterisation measurements was to analyze meter error characteristics if the fluid temperature deviates from nominal temperature. All reported data were corrected by the following procedure, because both meters showed a distinctive dependency of meter error due to changes in fluid temperature (Figure 17).

The correction is based on the relationship between a) deviation  $\Delta T_{Fluid}$  (Equation 22) of current fluid temperature  $T_{Fluid}$  to nominal temperature  $T_{nom}$  and b) deviation  $\Delta e_{nom}$  (Equation 23) of meter error at current temperature conditions  $e$  to meter error  $e_{nom}$ , calibrated at nominal temperature. The relationship between  $\Delta T$  and  $\Delta e_{nom}$  was analyzed separately for each transfer meter by fitting a second-degree polynomial function using least squares fits (Figure 18 and Figure 19).

The resulting model parameter of Table 15 were used to calculate a correction value of meter error  $\Delta e_{cor}$  (Equation 24) and the final meter error  $e$  at current temperature conditions (Equation 25).

$$\Delta T_{\text{fluid}} = T_{\text{fluid}} - T_{\text{nom}} \tag{22}$$

where  $\Delta T_{\text{fluid}}$  - Difference of current fluid temperature to nominal temperature of 20 °C (°C)  
 $T_{\text{fluid}}$  - Current fluid temperature (°C)  
 $T_{\text{nom}}$  - Nominal fluid temperature of 20 °C

$$\Delta e_{\text{nom}} = e - e_{\text{nom}} \tag{23}$$

where  $\Delta e_{\text{nom}}$  - Difference of meter error (%)  
 $e$  - Meter error at current temperature conditions (%)  
 $e_{\text{nom}}$  - Meter error at nominal temperature of 20 °C (%)

$$\Delta e_{\text{cor}} = a + b \cdot \Delta T_{\text{fluid}} + c \cdot \Delta T_{\text{fluid}}^2 \tag{24}$$

where  $\Delta e_{\text{cor}}$  - Correction value of meter error (%)  
 $a, b, c$  - Parameter of fitted polynomial model (Table 15) (-)

$$e_{\text{cor}} = e - \Delta e_{\text{cor}} \tag{25}$$

where  $e_{\text{cor}}$  - Temperature corrected meter error (%)

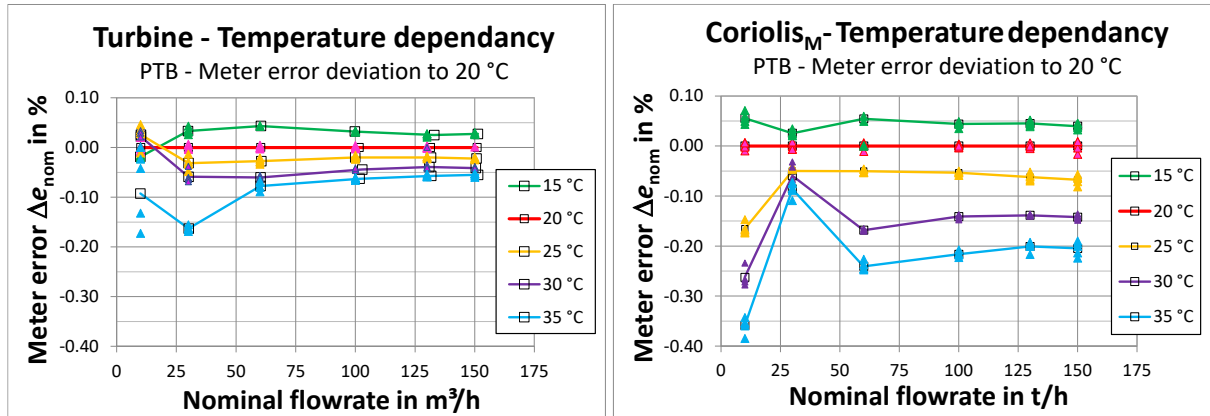


Figure 17: Temperature dependencies of turbine meter and Coriolis\_Mass - Differences of meter error  $\Delta e_{\text{nom}}$ , expressed as results of Equation (23). All calibrations were made at pilot laboratory (PTB) in 2015.

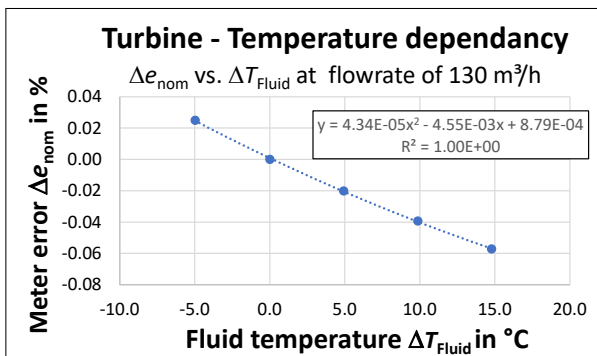


Figure 18: Temperature dependency of Turbine meter - Example relationship between  $\Delta T_{\text{fluid}}$  and  $\Delta e_{\text{nom}}$  at flowrate of 100 m³/h (results of Equation 22 and Equation 23) in order to estimate model parameters of Equation (24).

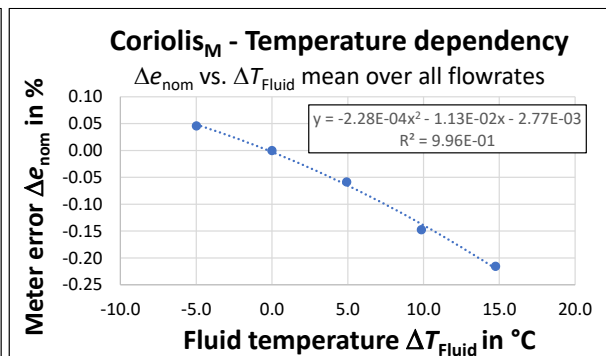


Figure 19: Temperature dependency of Coriolis\_M meter - relationship between  $\Delta T_{\text{fluid}}$  and  $\Delta e_{\text{nom}}$ , this mean function is based on flowrates between 60 t/h and 150 t/h (Equation 22 and Equation 23) in order to estimate model parameters of Equation (24).

**Table 15:** Model Parameter for temperature dependent correction of meter error  $e$  by using Equation (13) until Equation (25) for turbine meter and Coriolis\_Mass meter

Nominal flowrate in m <sup>3</sup> /h	Turbine meter – model parameter			Coriolis_Mass – model parameter		
	a	b	c	a	b	c
10	2.11E-02	6.01E-03	-8.75E-04	-2.77E-03	-1.13E-02	-2.28E-04
30	1.10E-02	-5.13E-03	-4.11E-04			
60	2.20E-03	-7.41E-03	1.33E-04			
100	2.74E-03	-5.38E-03	6.38E-05			
130	8.79E-04	-4.55E-03	4.34E-05			

**Meter uncertainty  $u_{temp}$** 

The presented method was successfully applied during model evaluation by using the temperature characterisation measurements at pilot laboratory (PTB) in 2015 (Figure 21). Especially for Coriolis\_Mass, a meter uncertainty reduction ( $u_{temp}$ ) of up to 94 % was gained if the meter error  $e$  was corrected by the described method. This clear improvement of  $u_{temp}$  over full flow scale can be explained by the distinctive temperature dependency of both meters.

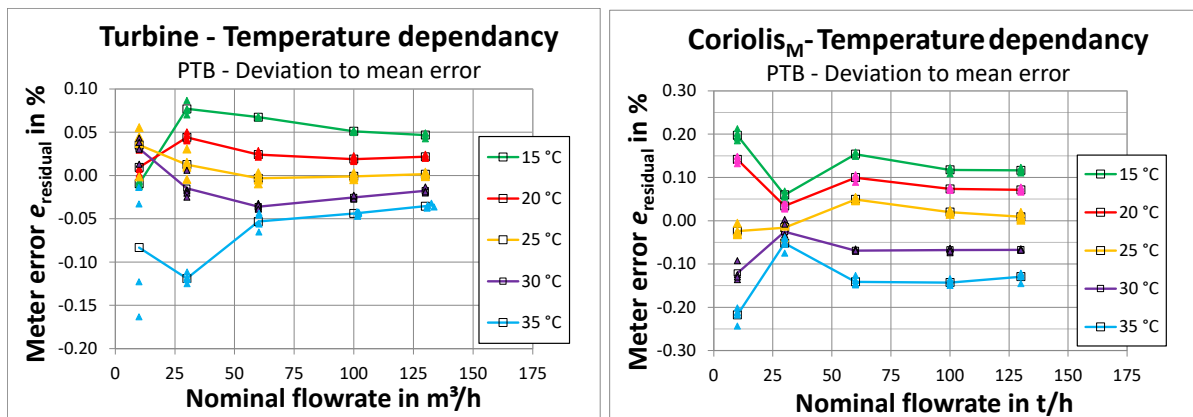
The calculation of  $u_{TS}$  itself is based on the following procedure and assumptions. The temperature range of reported laboratory data  $T_{fluid}$  does not exceed the investigated range of 20°C +/- 15 °C during characterisation measurements at pilot laboratory (Figure 16). The sensitivities of original meter error  $e$  and corrected meter error  $e_{cor}$  can also be expressed as specific model residuals  $e_{residual}$  to mean values over all temperatures (Equation 26 and Figure 20). Maximum and minimum values of  $e_{residual}$  were used to calculate  $u_{temp}$  (Table 16) with an assumption of a rectangular probability distribution (Equation 27). For calculation of  $E_N$  values, all reported meter errors ( $e_V$  and  $e_m$ ) of participating laboratories were corrected by the described method (Equation 22 until Equation 25).

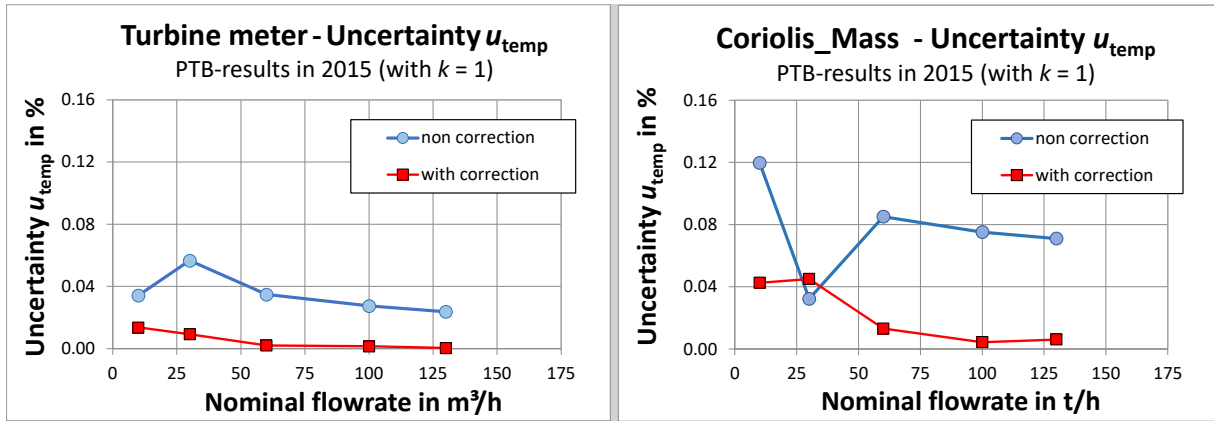
$$e_{residual} = e - e_{mean} \quad (26)$$

where  $e_{residual}$  - Model residuals (%)  
 $e_{mean}$  - Mean values of meter error at one flow rate over all temperatures (%)

$$u_{temp} = \frac{\max(e_{residual}) - \min(e_{residual})}{2\sqrt{3}} \quad (27)$$

where  $u_{temp}$  - Meter uncertainty caused by temperature effects (%)

**Figure 20:** Temperature dependencies of Turbine meter and Coriolis\_Mass - Residuals to mean values of Equation (26) for original meter error  $e$



**Figure 21:** Meter uncertainties  $u_{temp}$  for turbine meter and Coriolis\_Mass - based on non-corrected meter error  $e$  and on corrected meter error  $e_{cor}$  in 2015 - using Equation (22) until Equation (27).

**Table 16:** Final uncertainties of meter temperature sensitivity  $u_{temp}$

$u_{temp} (k = 1)$	Nominal Flowrate				
	10 m <sup>3</sup> /h	30 m <sup>3</sup> /h	60 m <sup>3</sup> /h	100 m <sup>3</sup> /h	130 m <sup>3</sup> /h
<b>Turbine meter in %</b>	0.014	0.009	0.002	0.001	0.000
<b>Coriolis_Mass in %</b>	0.043	0.045	0.013	0.004	0.006

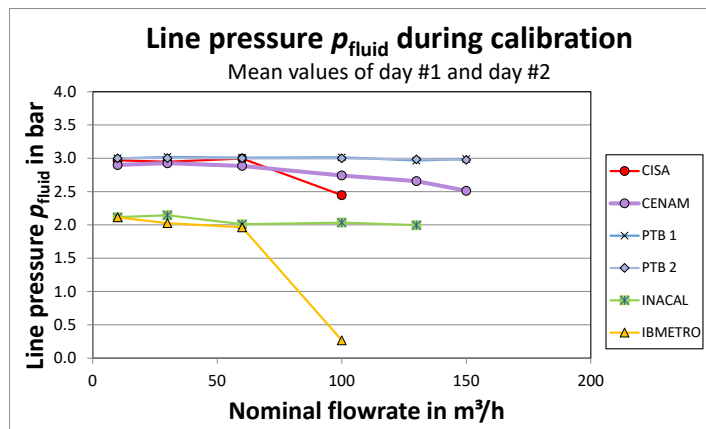
### 7.4 Pressure dependency - uncertainty $u_{pres}$

#### Laboratory conditions

The span of line pressure in participating laboratories  $p_{fluid}$  ranged between 0.27 bar and 3.00 bar (positive pressure after calibration setup) Figure 22.

**Table 17:** Line pressure  $p_{fluid}$  (bar) in participating laboratories during calibrations on day#1 and day#2; \*) values for INTI representing general facility specifications

NMI	PTB 1	CISA	INACAL	IBMETRO	INTI*)	CENAM	PTB 2
Max	3.02	3.00	2.15	2.11	3.5	2.93	3.00
Min	2.97	2.45	2.00	0.27	2.2	2.51	2.98
Max - Min	0.06	0.55	0.15	1.85		0.41	0.03
Mean	3.00	2.84	2.06	1.59		2.77	2.99

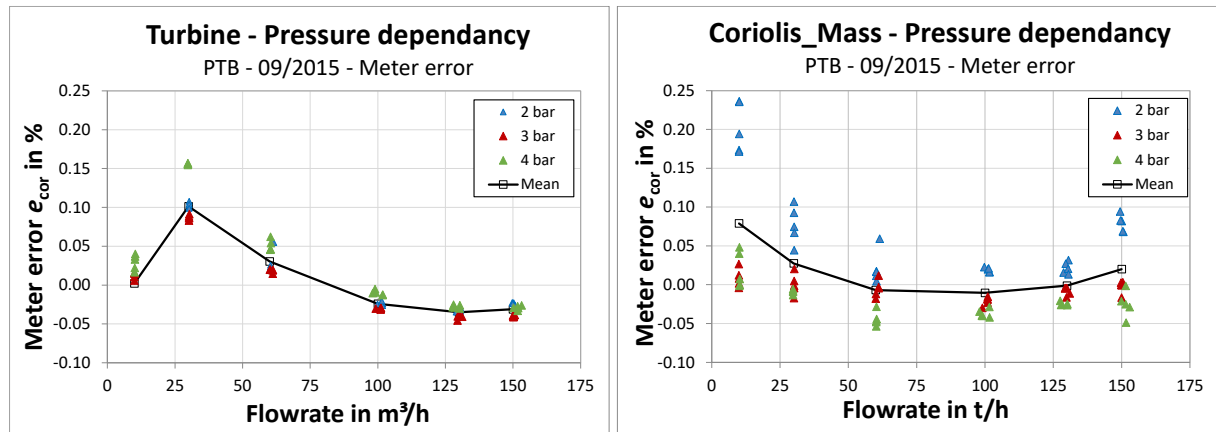


**Figure 22:** Line pressure during calibrations in participating laboratories – Mean values at each flowrate of calibration day #1 and day #2

### Meter characteristics

Pressure dependencies of transfer meters were analyzed at pilot laboratory (PTB) during characterisation measurements in 2015 (Table 6). Due to technical restrictions, calibrations were only possible at line pressure between 2 bar and 4 bar (Figure 23).

The deviations of meter error to mean values, expressed as residuals are presented in Figure 24. For pressure differences of +/- 1 bar, the sensitivity of meter error does not exceed +/- 0.03 % for turbine meter and +/- 0.05 % for Coriolis\_Mass.

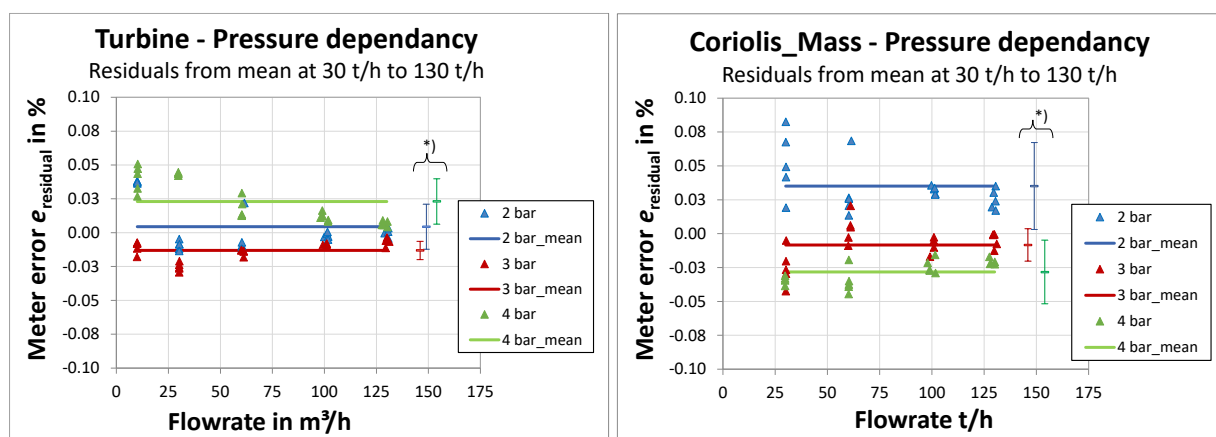


**Figure 23:** Pressure dependencies of turbine and Coriolis meter - Calibration results and mean values of characterization measurements at pilot laboratory PTB in 2015

### Meter uncertainty $u_{pres}$

For uncertainty calculation of  $u_{pres}$  it was assumed that the following conservative estimation of meter sensitivities did include the pressure range between 0.27 bar and 3.02 bar of reported data (Figure 22). The pressure sensitivities were treated as uncertainty contribution for turbine meter by  $u_{pres} = 0.030 \% / \sqrt{3}$  and for Coriolis by  $u_{pres} = 0.050 \% / \sqrt{3}$ , based on a rectangular probability distribution.

The results for turbine meter ( $u_{pres} = 0.017 \%$ ) and Coriolis ( $u_{pres} = 0.029 \%$ ), were used as constant values, valid for full investigated flow scale. For final calculation of  $E_N$  values, no pressure corrections were made to the data submitted by participating laboratories.

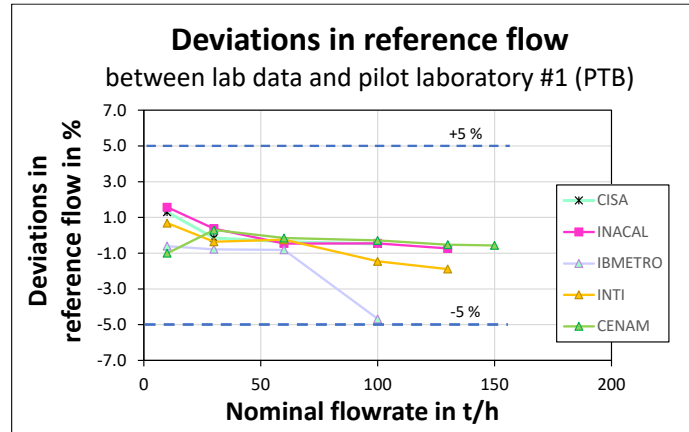


**Figure 24:** Pressure dependencies of turbine meter and Coriolis\_Mass - Residuals to mean values of temperature corrected meter error  $e_{cor}$ . \*) represents the standard deviation of  $e_{cor}$  for each pressure rate. For Coriolis meter the values at 10 t/h were not considered because of the still present autozero effect (Figure 23)

## 7.5 Dependency on flow stability - uncertainty $u_{flow}$

### Laboratory conditions

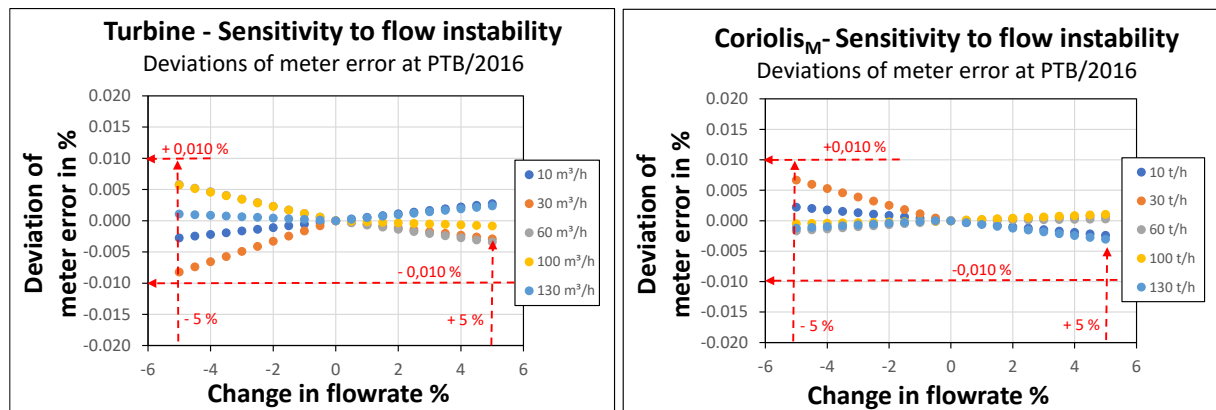
For data analysis of flow stability, the deviations of reference flow between pilot laboratory (PTB) and participating laboratories were analyzed. The mean values of observed differences did not exceed +/- 3 % of flowrate at pilot laboratory (Figure 25).



**Figure 25:** Flow stability  $\dot{m}$  (t/h), expressed as deviations in reference flow between pilot laboratory (PTB) calibrated in 01/2016 and reported values of participating laboratories

### Meter characteristics

For analyzing meter error sensitivity to changes in flowrate, calibration results at reference laboratory (PTB) were evaluated. Between single calibration points, the meter error of a standard calibration ( $T_{fluid} = 20\text{ }^{\circ}\text{C}$ ,  $p_{fluid} = 3\text{ bar}$ ) was linearly interpolated. Within this model, the sensitivities of meter error were estimated by varying flowrates to maximum values of +/- 5.0 % with a resolution of 0.5 % (Figure 26). Based on the previously discussed maximum limits in flowrate stability of +/- 5 % (Figure 25), both meters showed a maximum sensitivity in meter error of +/- 0.010 % (Figure 26).



**Figure 26:** Sensitivity of transfer meters to flow instability - based on PTB data set in 01/2016

### Meter uncertainty $u_{flow}$

The estimated maximum values of flow meter sensitivity were used for calculation of  $u_{flow}$ . For both meters, the flow stability sensitivities were treated as a rectangular uncertainty contribution, with  $u_{flow} = 0.010\text{ \%} / \sqrt{3}$ . It was assumed, that the results of  $u_{flow} = 0.006\text{ \%}$  were valid for full investigated flow scale. For final calculation of  $E_N$  values, no flow stability corrections were made to the data submitted by participating laboratories.



## 7.6 Dependency of inflow conditions to Turbine meter

### Laboratory conditions

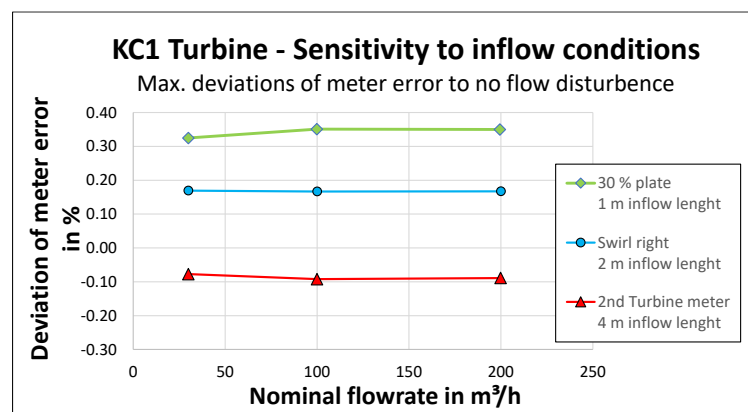
The span of undisturbed inflow length in participating laboratories ranged between 0.1 m and 4.6 m. Typical fittings like valves, tube bundle or elbows were installed at the inflow of calibration line (Table 18).

**Table 18:** Reported inflow lengths of undisturbed flow and pipe installation at the inflow of calibration line in participating laboratories

NMI	PTB (pilot lab)	CISA	INACAL	IBMETRO	INTI
Undisturbed inflow length	8.5 m	4.6 m	0.1 m	3.5 m	> 2.0 m
Pipe installation before inflow	tube bundle, line reducer	line reducer	elbow, tube bundle	line reducer, valve	line reducer, valve

### Turbine meter characteristics

The used turbine meter was identical to the type of flow meter, which was used during KC1, but with an inner diameter of 80 mm instead of 100 mm. During KC1, the turbine meter showed a distinctive sensitivity to disturbed inflow conditions. Within the ranges of reported SC inflow lengths (Table 18), the turbine meter of KC1 showed maximum sensitivities of meter error (Figure 27) in positive direction with +0.351 % (disturber type: 30 % closed orifice plate, inflow length: 1 m), in negative direction - 0.092 % (disturber type: 2<sup>nd</sup> turbine meter, inflow length: 4 m).



**Figure 27:** Maximum observed sensitivity of turbine meter to different flow disturber and inflow lengths - based on PTB calibrations in 03/2019 during KC1 comparison with a DN100 mm turbine meter

### Meter uncertainty

This research was necessary, because of significant differences in turbine meter calibrations between participating laboratories. Whereas, for flowrates higher than 10 m<sup>3</sup>/h, the maximum span of Coriolis meter error reached 0.222 % between laboratories (Figure 42, without INTI). At the same time the results of turbine meter differ up to 1.048 % (Figure 29). Such differences could not be explained by a standard estimation of transfer meter uncertainties. Behind this background and according to KC1 procedure, an additional uncertainty parameter ( $u_{inflow}$ ) was introduced for turbine meter to consider the influence of different inflow conditions to calibration characteristics of turbine meter.

With reference to the minimum reported inflow length of 0.10 m at participating laboratories (Table 18), the maximum observed meter error deviation at 1 m inflow length (Figure 27) was used for the estimation of turbine meter sensitivity  $u_{inflow}$ . The inflow sensitivity was treated as a rectangular uncertainty contribution with  $u_{inflow} = 0.351 \% / \sqrt{3} = 0.203 \%$ . It was assumed, that the results of  $u_{inflow} = 0.096 \%$  are valid for full investigated flow scale. For final calculation of  $E_N$  values, no corrections for different inflow conditions were made to the submitted data of turbine meter.

## 8 Results and final data evaluation

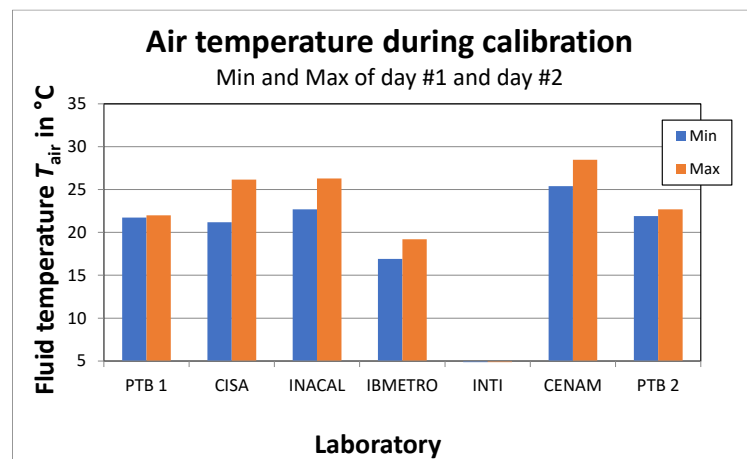
### 8.1 Ambient air temperature

#### Laboratory conditions

The span of air temperature in participating laboratories ranged between 18.24 °C and 32.31 °C. The maximum variation of air temperature within a participating lab, expressed as  $\max(T_{\text{air}}) - \min(T_{\text{air}})$  was reported with 5.40 °C (Table 19, Figure 28).

**Table 19:** Air temperatures  $T_{\text{air}}$  (°C) in participating laboratories during calibrations on day#1 and day#2; \*) values for INTI representing general facility specifications

NMI	PTB 1	CISA	INACAL	IBMETRO	INTI	CENAM	PTB 2
Max	21.99	26.16	26.30	19.20		28.48	22.70
Min	21.73	21.19	22.70	16.90		25.40	21.90
Max - Min	0.26	4.97	3.60	2.30		3.07	0.80
Mean	21.88	24.76	24.74	17.95	25 °C ± 3 °C	26.65	22.46



**Figure 28:** Air temperature  $T_{\text{air}}$  during calibrations in participating laboratories - maximum and minimum of calibration day #1 and day #2

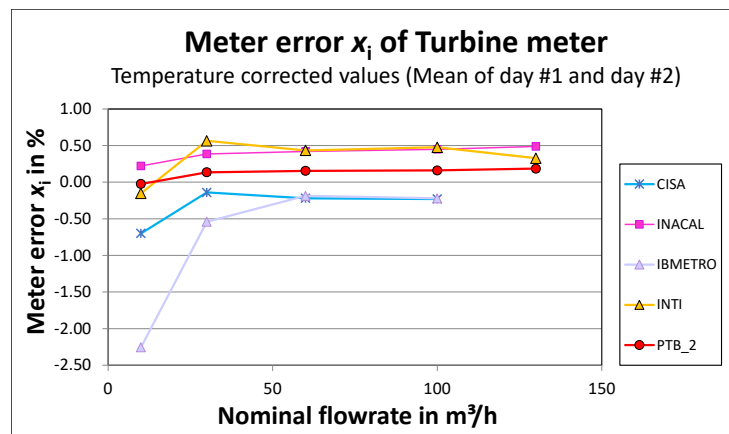
## 8.2 Turbine transfer meter

### 8.2.1 Summarized results

#### Laboratory results

**Table 20:** Relative measurement error  $x_i$  (%) of turbine meter at participated laboratories - temperature corrected mean values of day #1 and day #2, comparison reference value  $SCRV_{Turb}$  and  $U(SCRV_{Turb})$

Flowrate	CISA	INACAL	IBMETRO	INTI	PTB_2 = $SCRV_{Turb}$	$U(SCRV_{Turb})$ $k = 2$
$m^3/h$	%	%	%	%	%	%
10	-0.700	0.222	-2.255	-0.153	-0.025	0.414
30	-0.140	0.386	-0.541	0.564	0.135	0.414
60	-0.220	0.420	-0.187	0.433	0.154	0.423
100	-0.230	0.450	-0.221	0.476	0.161	0.433
130		0.488		0.327	0.185	0.438



**Figure 29:** Relative measurement error  $x_i$  of turbine meter at participating laboratories - temperature corrected mean values of day #1 and day #2. The values of PTB\_2 were used as the comparison reference value  $SCRV_{Turb}$ .

The degree of equivalence value  $E_N$  is a measure of result agreement of each participating laboratory to the  $SCRV_{Turb}$ . Expressed as the normalized differences of “lab to  $SCRV_{Turb}$ ”, the final  $E_N$  values of turbine meter are summarized in Table 21 and Figure 30. Beside one calibration, all labs passed the  $E_N$  criteria of  $\leq 1.20$ .

**Table 21:** Summary of  $E_N$ -values for turbine meter of each participating laboratory. <sup>a)</sup> represents data at warning level, <sup>b)</sup> represents data with  $E_N$  values  $> 1.20$

Flowrate	CISA	INACAL	IBMETRO	INTI
$m^3/h$	-	-	-	-
10	1.11 <sup>a)</sup>	0.41	3.69 <sup>b)</sup>	0.20
30	0.46	0.42	1.01 <sup>a)</sup>	0.72
60	0.61	0.43	0.54	0.46
100	0.62	0.47	0.62	0.49
130		0.48		0.22

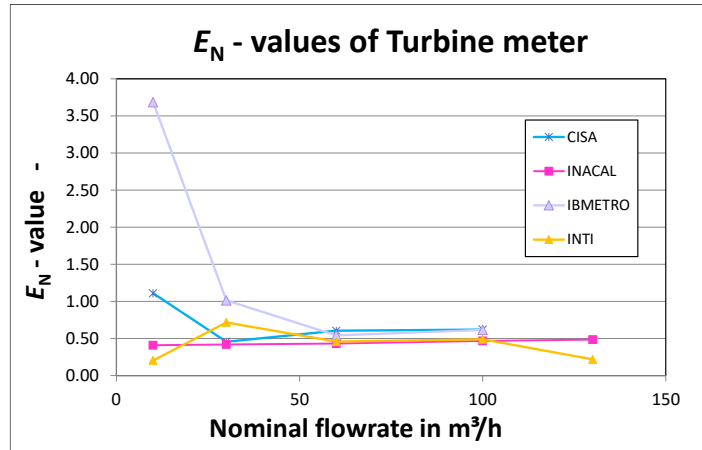


Figure 30: Summarized  $E_N$ -values of participating laboratories for turbine meter

**Conclusive tests of comparison results  $u_{comp}/u_{base,i}$**

Based on [3], for a conclusive proof of participant results and an agreement with the  $SCRV_{Turb}$ , the comparison uncertainty ratio  $u_{comp}/u_{base,i}$  should be  $< 2$ .

Results from all participating laboratories couldn't comply with this limit (Table 22). For the purpose of the presented SC the uncertainty  $u_{comp}$  of turbine meter was too high. A calibration of turbine meter gave for all laboratories inconclusive results. Finally, the meter was not suitable for a confirmation of the declared CMC values.

Table 22: Summarized results of conclusive proof  $u_{comp}/u_{base,i}$  of each participating laboratory for turbine meter  
 - <sup>c)</sup> represents inconclusive data

Flowrate m³/h	CISA	INACAL	IBMETRO	INTI
10	2.80 <sup>c)</sup>	5.67 <sup>c)</sup>	4.29 <sup>c)</sup>	7.83 <sup>c)</sup>
30	2.77 <sup>c)</sup>	5.55 <sup>c)</sup>	5.13 <sup>c)</sup>	7.16 <sup>c)</sup>
60	2.84 <sup>c)</sup>	5.72 <sup>c)</sup>	4.55 <sup>c)</sup>	7.26 <sup>c)</sup>
100	2.87 <sup>c)</sup>	5.74 <sup>c)</sup>	4.31 <sup>c)</sup>	7.18 <sup>c)</sup>
130	-	5.80 <sup>c)</sup>	-	7.29 <sup>c)</sup>

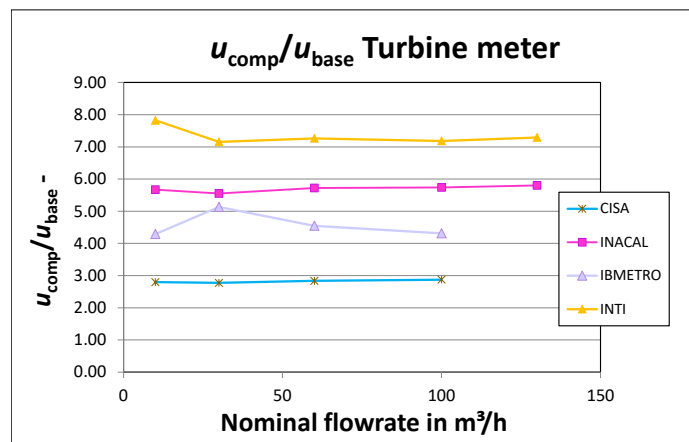


Figure 31: Summarized results of conclusive proof  $u_{comp}/u_{base,i}$  of each participating laboratory for turbine meter

### 8.2.2 Final CMC-decision tables for participating laboratories

#### CISA - laboratory (Chile)

For volume calibration this comparison couldn't support the declared base uncertainties of the participant (Table 23), because of inconclusive data - at all calibrated flowrates the ratio of  $u_{comp}/u_{base}$  was  $> 2$ . The turbine meter was not suitable for a confirmation of the declared CMC values.

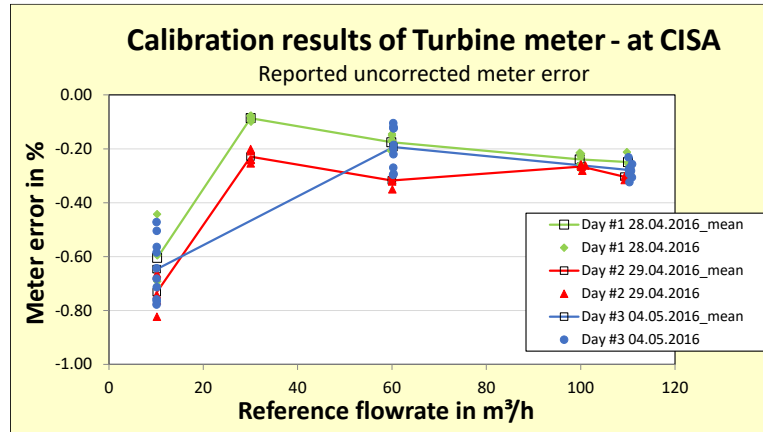


Figure 32: Calibration results of CISA laboratory for turbine meter – reported uncorrected meter error  $e_v$

Table 23: Comparison decision table for CISA (turbine meter), where  $x_i$  is the temperature corrected meter error (mean of day #1 and day #2) - <sup>a)</sup> represents  $E_N$ -values at warning level, <sup>c)</sup> represents inconclusive data

CISA / Chile							
Nominal flowrate	Relative measurement error	Expanded laboratory uncertainty	Expanded measurement uncertainty	Degree of equivalence	Normalized degree of equivalence	$u_{comp}/u_{base,i}$	CMC decision status
	$x_i$	$U_{base,i}$ ( $k = 2$ )	$U(x_i)$ ( $k = 2$ )	$d_i$	$E_{N,i}$		
$m^3/h$	%	%	%	-	-	-	
10	-0.700	0.150	0.445	-0.675	1.11 <sup>a)</sup>	2.80 <sup>c)</sup>	inconclusive
30	-0.140	0.150	0.442	-0.276	0.46	2.77 <sup>c)</sup>	inconclusive
60	-0.220	0.150	0.451	-0.374	0.61	2.84 <sup>c)</sup>	inconclusive
100	-0.230	0.150	0.457	-0.390	0.62	2.87 <sup>c)</sup>	inconclusive
130							

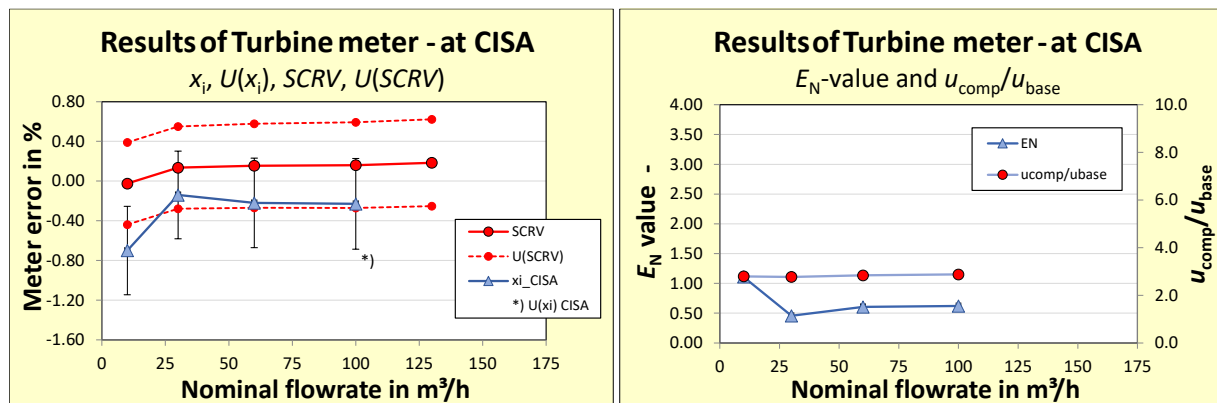
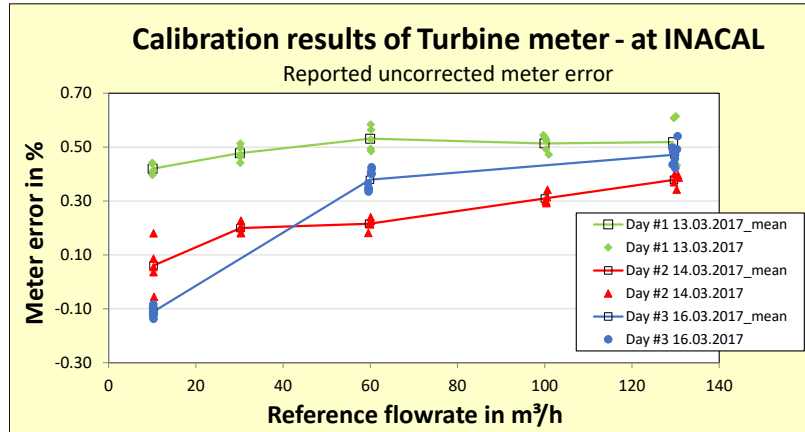


Figure 33: Comparison results of CISA laboratory for turbine meter

**INACAL - laboratory (Peru)**

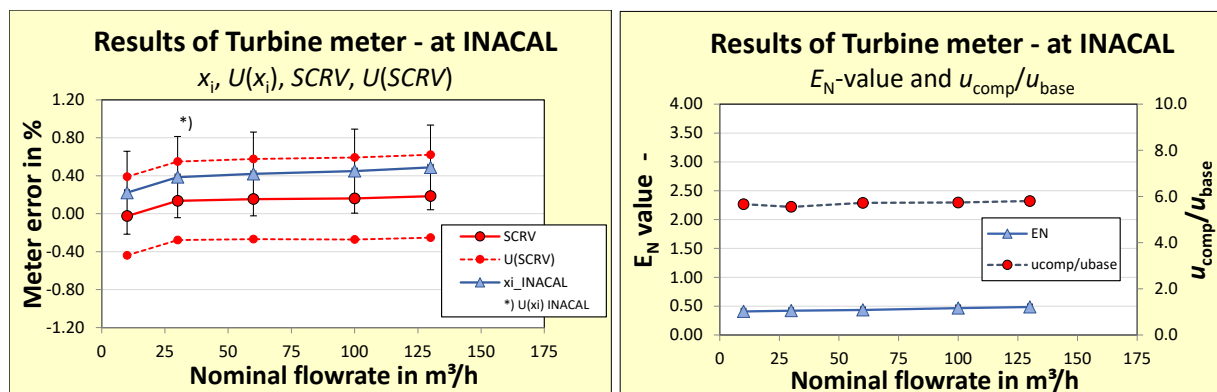
For volume calibration this comparison couldn't support the declared base uncertainties of the participant (Table 24), because of inconclusive data - at all calibrated flowrates the ratio of  $u_{comp}/u_{base}$  was  $> 2$ . The turbine meter was not suitable for a confirmation of the declared CMC values.



**Figure 34:** Calibration results of INACAL laboratory for turbine meter - reported uncorrected meter error  $e_v$

**Table 24:** Comparison decision table for INACAL (turbine meter), where  $x_i$  is the temperature corrected meter error (mean of day #1 and day #2) – <sup>b)</sup> represents  $E_N$  -values  $> 1.20$ , <sup>c)</sup> represents inconclusive data

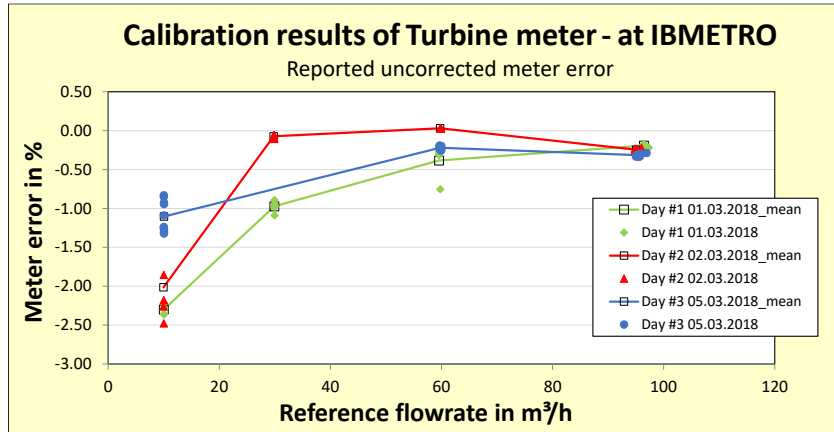
INACAL / Peru							
Nominal flowrate	Relative measurement error	Expanded laboratory uncertainty	Expanded measurement uncertainty	Degree of equivalence	Normalized degree of equivalence	$u_{comp}/u_{base}$	CMC decision status
	$x_i$	$U_{base,i}$ ( $k = 2$ )	$U(x_i)$ ( $k = 2$ )	$d_i$	$E_{N,i}$		
$m^3/h$	%	%	%	-	-	-	
10	0.222	0.076	0.438	0.247	0.41	5.67 <sup>c)</sup>	inconclusive
30	0.386	0.076	0.429	0.251	0.42	5.55 <sup>c)</sup>	inconclusive
60	0.420	0.076	0.442	0.265	0.43	5.72 <sup>c)</sup>	inconclusive
100	0.450	0.076	0.443	0.289	0.47	5.74 <sup>c)</sup>	inconclusive
130	0.488	0.076	0.447	0.304	0.48	5.80 <sup>c)</sup>	inconclusive



**Figure 35:** Comparison results of INACAL laboratory for turbine meter

**IBMETRO - laboratory (Bolivia)**

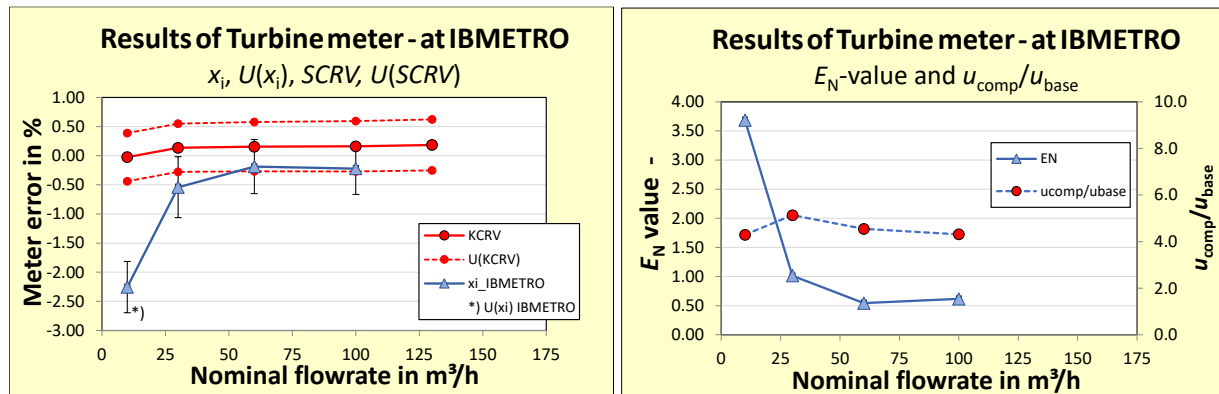
For volume calibration this comparison couldn't support the declared base uncertainties of the participant (Table 25), because of inconclusive data - at all calibrated flowrates the ratio of  $u_{comp}/u_{base}$  was  $> 2$ . The turbine meter was not suitable for a confirmation of the declared CMC values.



**Figure 36:** Calibration results of IBMETRO for turbine meter - reported uncorrected meter error  $e_v$

**Table 25:** Comparison decision table for IBMETRO (turbine meter), where  $x_i$  is the temperature corrected meter error (mean of day #1 and day #2) - <sup>a)</sup> represents  $E_N$ -values at warning level, <sup>b)</sup> represents  $E_N$ -values  $> 1.20$ , <sup>c)</sup> represents inconclusive data

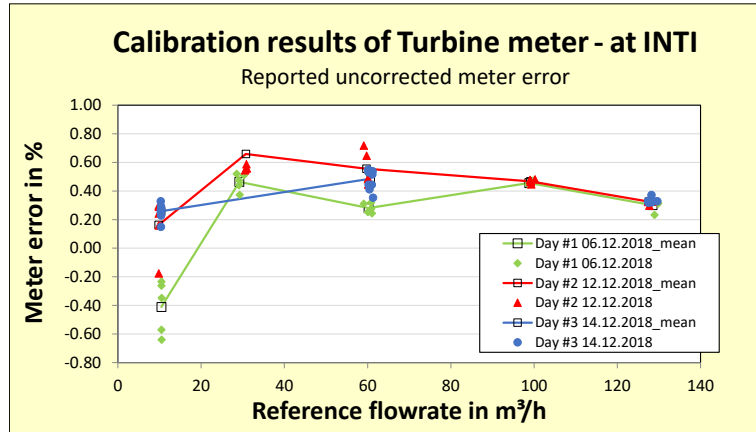
IBMETRO / Bolivia							
Nominal flowrate	Relative measurement error	Expanded laboratory uncertainty	Expanded measurement uncertainty	Degree of equivalence	Normalized degree of equivalence	$u_{comp}/u_{base}$	CMC decision status
	$x_i$	$U_{base,i}$ ( $k = 2$ )	$U(x_i)$ ( $k = 2$ )	$d_i$	$E_{N,i}$		
$m^3/h$	%	%	%	-	-	-	
10	-2.255	0.100	0.441	-2.230	3.69 <sup>b)</sup>	4.29 <sup>c)</sup>	inconclusive
30	-0.541	0.100	0.523	-0.676	1.01 <sup>a)</sup>	5.13 <sup>c)</sup>	inconclusive
60	-0.187	0.100	0.466	-0.341	0.54	4.55 <sup>c)</sup>	inconclusive
100	-0.221	0.100	0.443	-0.382	0.62	4.31 <sup>c)</sup>	inconclusive
130							



**Figure 37:** Comparison results of IBMETRO laboratory for turbine meter

**INTI - laboratory (Argentina)**

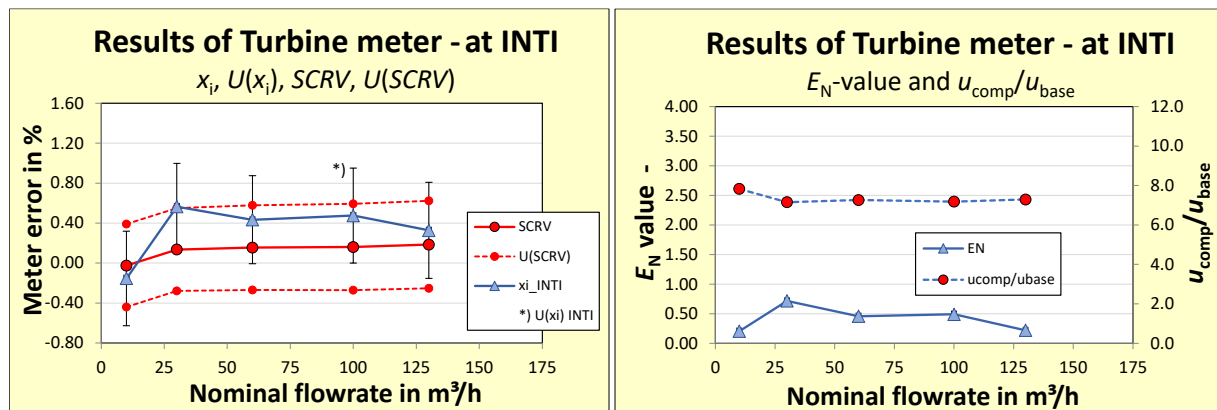
For volume calibration this comparison couldn't support the declared base uncertainties of the participant (Table 26), because of inconclusive data - at all calibrated flowrates the ratio of  $u_{comp}/u_{base}$  was  $> 2$ . The turbine meter was not suitable for a confirmation of the declared CMC values.



**Figure 38:** Calibration results of INTI for turbine meter - reported uncorrected meter error  $e_v$

**Table 26:** Comparison decision table for INTI (turbine meter), where  $x_i$  is the temperature corrected meter error (mean of day #1 and day #2) - <sup>c)</sup> represents inconclusive data

INTI / Argentina							
Nominal flowrate	Relative measurement error	Expanded laboratory uncertainty	Expanded measurement uncertainty	Degree of equivalence	Normalized degree of equivalence	$u_{comp}/u_{base}$	CMC decision status
	$x_i$	$U_{base,i}$ ( $k = 2$ )	$U(x_i)$ ( $k = 2$ )	$d_i$	$E_{N,i}$		
$m^3/h$	%	%	%	-	-	-	
10	-0.153	0.060	0.473	-0.128	0.20	7.83 <sup>c)</sup>	inconclusive
30	0.564	0.060	0.433	0.429	0.72	7.16 <sup>c)</sup>	inconclusive
60	0.433	0.060	0.440	0.279	0.46	7.26 <sup>c)</sup>	inconclusive
100	0.476	0.200	0.475	0.315	0.49	7.18 <sup>c)</sup>	inconclusive
130	0.327	0.200	0.481	0.142	0.22	7.29 <sup>c)</sup>	inconclusive



**Figure 39:** Comparison results of INTI laboratory for turbine meter



### 8.3 Coriolis\_Mass transfer meter

#### 8.3.1 Results of $SCRV_{Cor}$ calculation and $E_N$ values for CENAM and PTB

The comparison reference value for Coriolis meter ( $SCRV_{Cor}$ ) was partially linked to Key Comparison CCM.FF-K1.2015 (KC1) - see Chapter 6.4.1. The data of both pilot laboratories (PTB and CENAM) were used for the calculation of  $SCRV_{Cor}$ . - see Chapter 6.4.2. The input data are given in Table 27, the calculated values of  $SCRV_{Cor}$  and it's uncertainties are presented in Table 28 and Figure 40, the final  $E_N$  values are summarized in Table 29 and Figure 41.

**Table 27:** Input data for calculation of  $SCRV_{Cor}$

Nominal flowrate	SIM comparison data				KC1 comparison data (based on Table 8 and Table 9)			
	Autozero corrected measurement error		Measurement uncertainty of $x_i$		Supplementary comparison correction value		Uncertainty of $SCC_i$	
	CENAM	PTB	CENAM	PTB	CENAM	PTB	CENAM	PTB
	$x_i$	$x_i$	$u(x_i)$ ( $k = 1$ )	$u(x_i)$ ( $k = 1$ )	$SCC_i$	$SCC_i$	$u(SCC_i)$ ( $k = 1$ )	$u(SCC_i)$ ( $k = 1$ )
t/h	%	%	%	%	%	%	%	%
10	-0.049	0.062	0.071	0.070				
30	-0.025	-0.030	0.058	0.057	0.006	0.004	0.025	0.022
60	-0.015	-0.013	0.038	0.036	0.012	0.004	0.018	0.014
100	-0.027	-0.009	0.035	0.033	0.012	-0.001	0.017	0.013
130	-0.027	-0.003	0.036	0.035				

**Table 28:** Calculation of  $SCRV_{Cor}$

Nominal flowrate	SIM comparison data				$SCRV$	$U(SCRV)$
	$SCC_i$ corrected measurement error		Measurement uncertainty of $x_{Cor,i}$			
	CENAM	PTB	CENAM	PTB		
	$x_{Cor,i}$	$x_{Cor,i}$	$u(x_{Cor,i})$ ( $k = 1$ )	$u(x_{Cor,i})$ ( $k = 1$ )		( $k = 2$ )
t/h	%	%	%	%	%	%
10	-0.049	0.062	0.070	0.071	0.007	0.100
30	-0.032	-0.034	0.061	0.063	-0.033	0.088
60	-0.026	-0.017	0.039	0.042	-0.021	0.057
100	-0.039	-0.008	0.035	0.039	-0.022	0.053
130	-0.027	-0.003	0.035	0.036	-0.014	0.050

**Table 29:**  $E_N$ -values for comparison between CENAM and PTB

Nominal flowrate	SIM comparison data					
	$d_i$		$U(d_i)$		$E_N$	
	CENAM	PTB	CENAM	PTB	CENAM	PTB
			( $k = 2$ )	( $k = 2$ )		
t/h	%	%	%	%	-	-
10	-0.056	0.055	0.101	0.099	-0.56	0.56
30	0.001	-0.001	0.090	0.085	0.01	-0.01
60	-0.005	0.004	0.062	0.053	-0.08	0.08
100	-0.017	0.014	0.058	0.048	-0.29	0.29
130	-0.013	0.011	0.053	0.048	-0.24	0.24

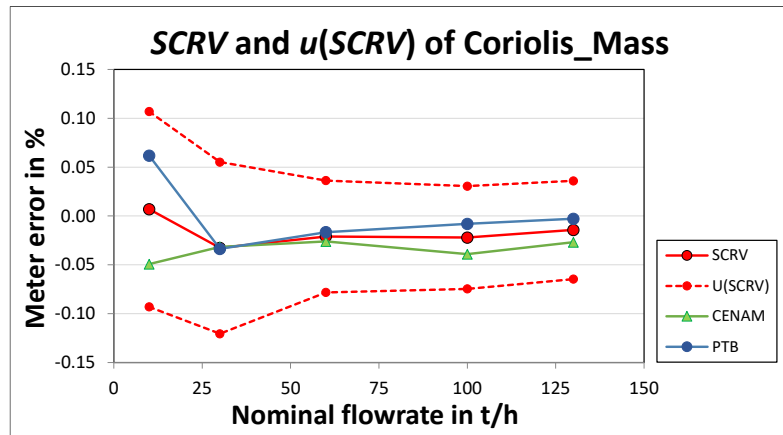


Figure 40: Results of corrected meter error for Coriolis\_Mass and  $SCR_{Cor}$  of the comparison between CENAM and PTB, including  $U(SCR_{Cor})$

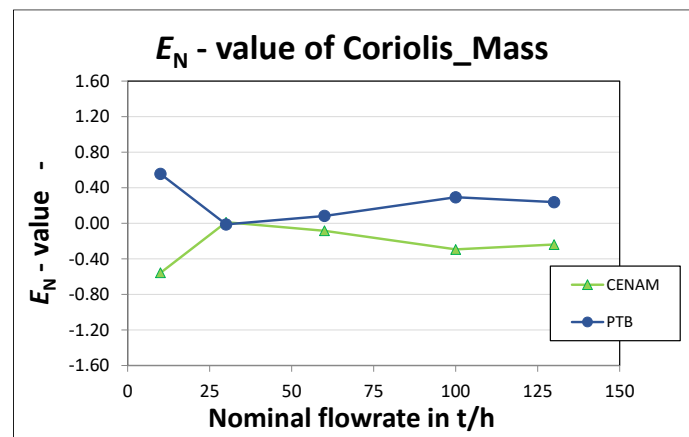


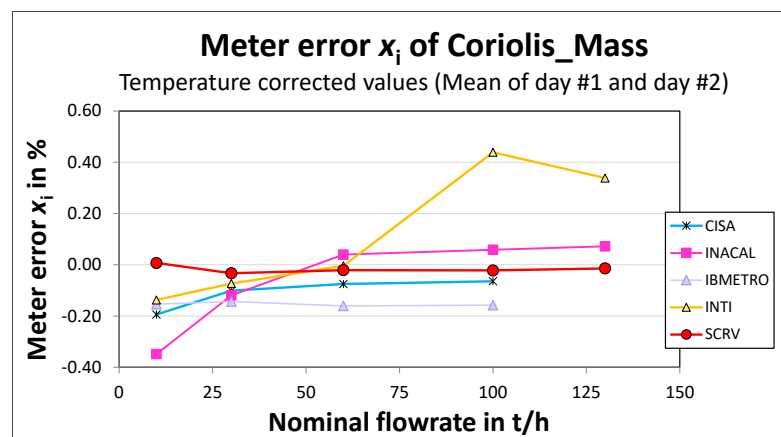
Figure 41:  $E_N$  values of basic comparison between CENAM and PTB

### 8.3.2 Comparison results of participating laboratories

#### Laboratory results

**Table 30:** Relative measurement error  $x_i$  (%) of Coriolis\_Mass at participating laboratories – temperature corrected mean values of day #1 and day #2, comparison reference value  $SCRV_{Cor}$  and  $U(SCRV_{Cor})$

Flowrate	CISA	INACAL	IBMETRO	INTI	$SCRV_{Cor}$	$U(SCRV_{Cor})$ k = 2
t/h	%	%	%	%	%	%
10	-0.194	-0.348	-0.154	-0.137	0.007	0.100
30	-0.101	-0.120	-0.143	-0.073	-0.033	0.088
60	-0.075	0.040	-0.160	-0.004	-0.021	0.057
100	-0.064	0.059	-0.157	0.439	-0.022	0.053
130		0.072		0.338	-0.014	0.050



**Figure 42:** Relative measurement error  $x_i$  of Coriolis\_Mass at participating laboratories - temperature corrected mean values of day #1 and day #2

The  $E_N$  values of participating laboratories are summarized in Table 31 and Figure 43. Beside two calibrations, all laboratories complied with the  $E_N$  criteria of < 1.2. Only at the flowrates of 100 t/h and 130 t/h this critical value.

**Table 31:** Summary of  $E_N$ -values of participating laboratories for Coriolis\_Mass transfer meter - <sup>a)</sup> represents  $E_N$  – values at warning level between 1.00 and 1.20, <sup>b)</sup> represents  $E_N$  -values > 1.20

Flowrate	CISA	INACAL	IBMETRO	INTI
t/h	-	-	-	-
10	0.82	0.91	0.81	0.77
30	0.33	0.47	0.63	0.25
60	0.31	0.47	1.03 <sup>a)</sup>	0.11
100	0.24	0.65	1.04 <sup>a)</sup>	1.96 <sup>b)</sup>
130		0.72		1.50 <sup>b)</sup>

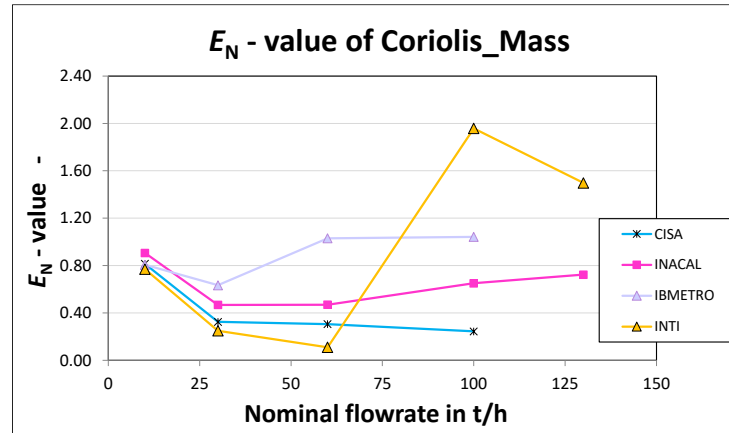


Figure 43: Summarized  $E_N$ -values of participating laboratories for Coriolis\_Mass transfer meter

**Conclusive tests of comparison results  $u_{comp}/u_{base}$**

Based on [3], for a conclusive proof of participant results and an agreement with the  $SCRV_{Cor}$ , the comparison uncertainty ratio  $u_{comp}/u_{base}$  should be  $< 2$ . The results for participating laboratories are summarized in Table 32 and Figure 44.

Beside one calibration, all results complied with this limit. For the final purpose of this SC the uncertainties  $u_{comp}$  of Coriolis\_Mass were sufficiently low enough. Finally, the meter was suitable for a confirmation of the declared CMC values.

Table 32: Summarized results of conclusive proof  $u_{comp}/u_{base}$  of participating laboratories for Coriolis\_Mass transfer meter - <sup>c)</sup> represents inconclusive data

Flowrate t/h	CISA	INACAL	IBMETRO	INTI
t/h	-	-	-	-
10	1.12	4.88 <sup>c)</sup>	1.41	2.00
30	0.79	1.91	1.13	1.66
60	0.50	1.16	0.71	1.76
100	0.44	1.09	0.64	0.93
130		1.02		0.95

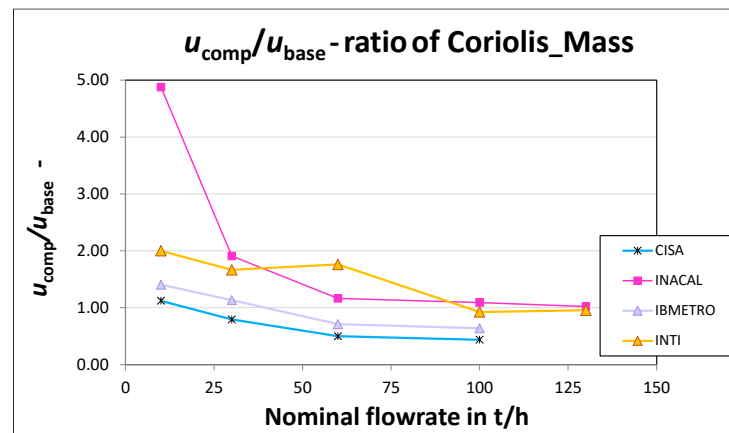


Figure 44: Summarized results of conclusive proof  $u_{comp}/u_{base}$  of participated laboratories for Coriolis\_Mass transfer meter

### 8.3.3 Final CMC-decision tables for participating laboratories

#### CISA - laboratory (Chile)

For mass calibration this comparison supported the declared base uncertainties of the participant (Table 33).

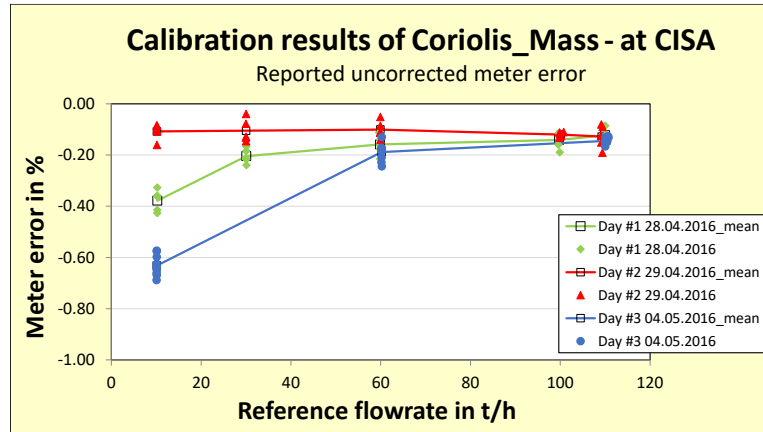


Figure 45: Calibration results of CISA for Coriolis\_Mass transfer meter – reported uncorrected meter error  $e_m$

Table 33: Comparison decision table for CISA (Coriolis\_Mass transfer meter), where  $x_i$  is the temperature corrected meter error (mean of day #1 and day#2)

CISA / Chile							
Nominal flowrate	Relative measurement error	Expanded laboratory uncertainty	Expanded measurement uncertainty	Degree of equivalence	Normalized degree of equivalence	$u_{comp}/u_{base}$	CMC decision status
	$x_i$	$U_{base,i}$ ( $k = 2$ )	$U(x_i)$ ( $k = 2$ )	$d_i$	$E_{N,i}$		
t/h	%	%	%	-	-	-	
10	-0.194	0.150	0.225	-0.201	0.82	1.12	acceptable
30	-0.101	0.150	0.192	-0.069	0.33	0.79	acceptable
60	-0.075	0.150	0.168	-0.054	0.31	0.50	acceptable
100	-0.064	0.150	0.164	-0.042	0.24	0.44	acceptable

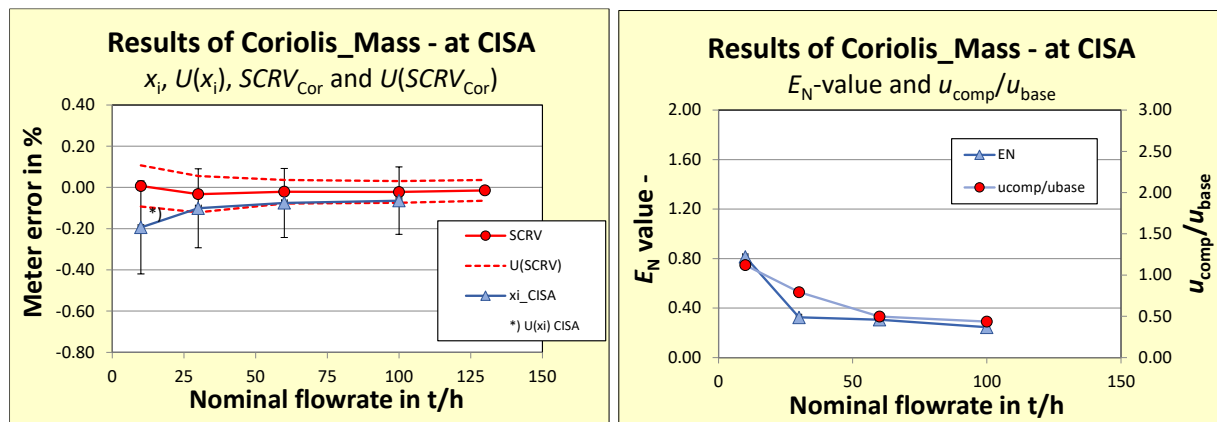
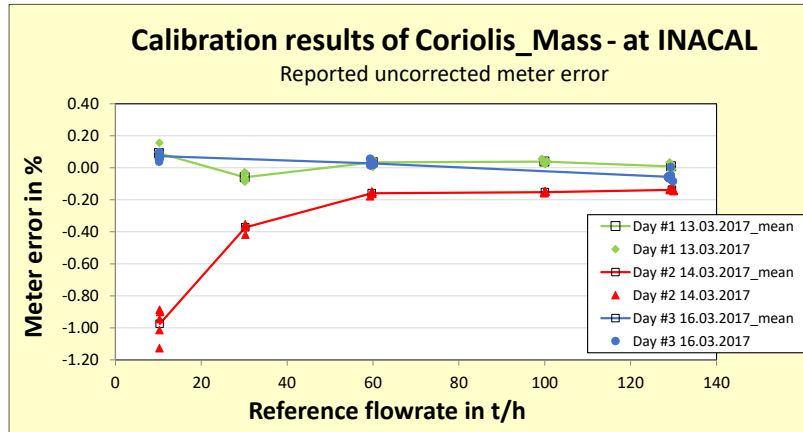


Figure 46: Comparison results of CISA laboratory for Coriolis\_Mass transfer meter

**INACAL - laboratory (Peru)**

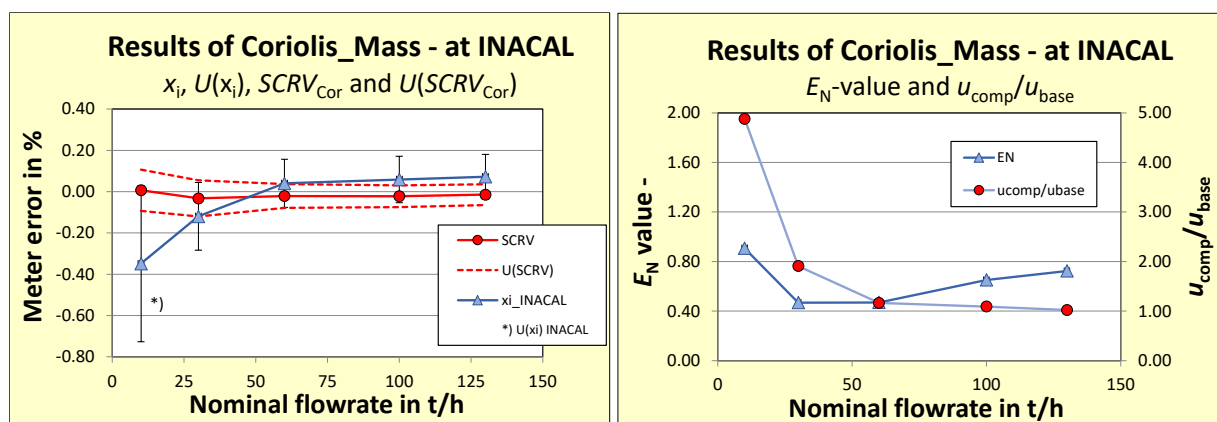
Beside the flowrate of 10 t/h, for mass calibration this comparison supported the declared base uncertainties of the participant (Table 34). The calibrations with Coriolis meter were not suitable for a confirmation of the declared CMC at the flowrate of 10 t/h, because the ratio of  $u_{comp}/u_{base}$  was  $> 2$ .



**Figure 47:** Calibration results of INACAL for Coriolis\_Mass transfer meter – reported uncorrected meter error  $e_m$

**Table 34:** Comparison decision table for INACAL laboratory (Coriolis\_Mass transfer meter), where  $x_i$  is the temperature corrected meter error (mean of day #1 and day#2) - <sup>c)</sup> represents inconclusive data

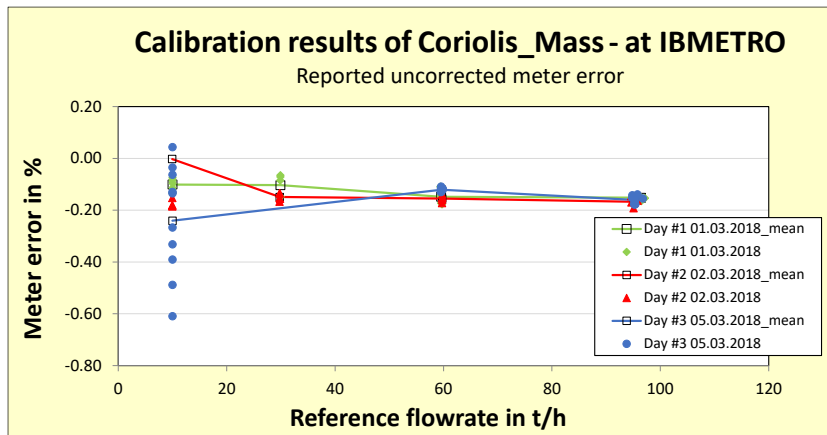
INACAL / Peru							
Nominal flowrate	Relative measurement error	Expanded laboratory uncertainty	Expanded measurement uncertainty	Degree of equivalence	Normalized degree of equivalence	$u_{comp}/u_{base}$	CMC decision status
	$x_i$	$U_{base,i} (k=2)$	$U(x_i) (k=2)$	$d_i$	$E_{N,i}$		
t/h	%	%	%	-	-	-	
10	-0.348	0.076	0.378	-0.355	0.91	4.88 <sup>c)</sup>	inconclusive
30	-0.120	0.076	0.164	-0.087	0.47	1.91	acceptable
60	0.040	0.076	0.117	0.061	0.47	1.16	acceptable
100	0.059	0.076	0.113	0.081	0.65	1.09	acceptable
130	0.072	0.076	0.109	0.087	0.72	1.02	acceptable



**Figure 48:** Comparison results of INACAL laboratory for Coriolis\_Mass transfer meter

**IBMETRO - laboratory (Bolivia)**

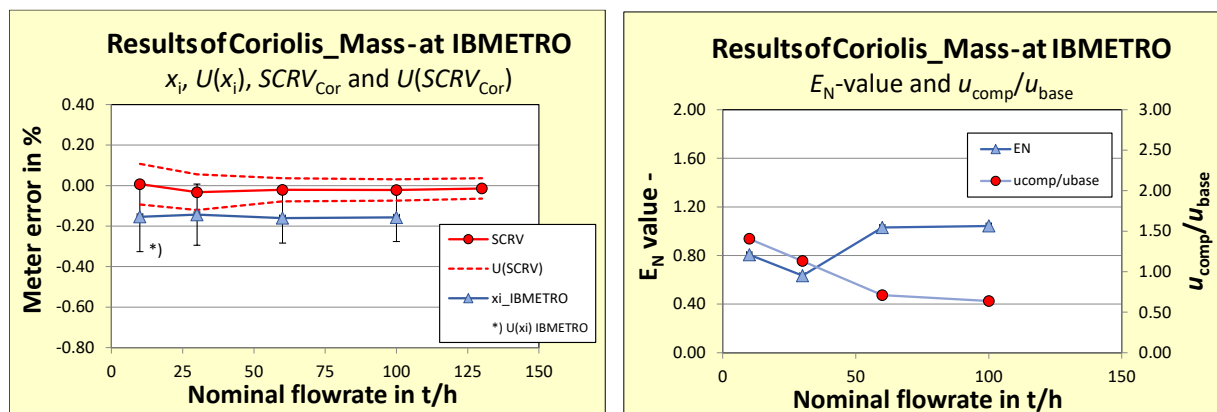
For mass calibration this comparison supported the declared base uncertainties of the participant (Table 35).



**Figure 49:** Calibration results of IBMETRO for Coriolis\_Mass transfer meter - reported uncorrected meter error  $e_m$

**Table 35:** Comparison decision table for IBMETRO laboratory (Coriolis\_Mass transfer meter), where  $x_i$  is the temperature corrected meter error (mean of day #1 and day#2) -  $a)$  represents  $E_N$  - values at warning level between 1.00 and 1.20

IBMETRO / Bolivia							
Nominal flowrate	Relative measurement error	Expanded laboratory uncertainty	Expanded measurement uncertainty	Degree of equivalence	Normalized degree of equivalence	$u_{comp}/u_{base}$	CMC decision status
	$x_i$	$U_{base,i}$ ( $k = 2$ )	$U(x_i)$ ( $k = 2$ )	$d_i$	$E_{N,i}$		
t/h	%	%	%	-	-	-	
10	-0.154	0.100	0.172	-0.161	0.81	1.40	acceptable
30	-0.143	0.100	0.151	-0.111	0.63	1.12	acceptable
60	-0.160	0.100	0.123	-0.139	1.03 <sup>a)</sup>	0.70	warning level
100	-0.157	0.100	0.119	-0.135	1.04 <sup>a)</sup>	0.64	warning level



**Figure 50:** Comparison results of IBMETRO laboratory for Coriolis\_Mass transfer meter

**INTI - laboratory (Argentina)**

For mass calibration between flowrates of 10 t/h and 60 t/h this comparison supported the declared base uncertainties of the participant (Table 36). The laboratory uncertainties for mass calibration at 100 t/h and 130 t/h must be declined, because the  $E_N$  value at both flowrates were  $> 1.20$ .

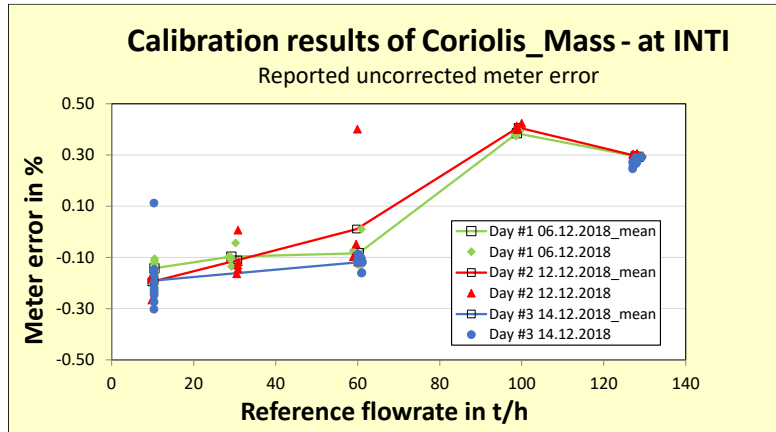


Figure 51: Calibration results of INTI for Coriolis\_Mass transfer meter – reported uncorrected meter error  $e_m$

Table 36: Comparison decision table for INTI laboratory (Coriolis\_Mass transfer meter), where  $x_i$  is the temperature corrected meter error (mean of day #1 and day#2) -  $b)$  represents  $E_N$  -values  $> 1.20$

Nominal flowrate	INTI / Argentina						
	Relative measurement error	Expanded laboratory uncertainty	Expanded measurement uncertainty	Degree of equivalence	Normalized degree of equivalence	$u_{comp}/u_{base}$	CMC decision status
	$x_i$	$U_{base,i} (k=2)$	$U(x_i) (k=2)$	$d_i$	$E_{N,i}$		
t/h	%	%	%	-	-	-	
10	-0.137	0.070	0.158	-0.144	0.77	2.00	acceptable
30	-0.073	0.070	0.136	-0.040	0.25	1.66	acceptable
60	-0.004	0.070	0.142	0.017	0.11	1.76	acceptable
100	0.439	0.220	0.229	0.461	1.96 <sup>b)</sup>	0.93	not accepted
130	0.338	0.220	0.230	0.353	1.50 <sup>b)</sup>	0.95	not accepted

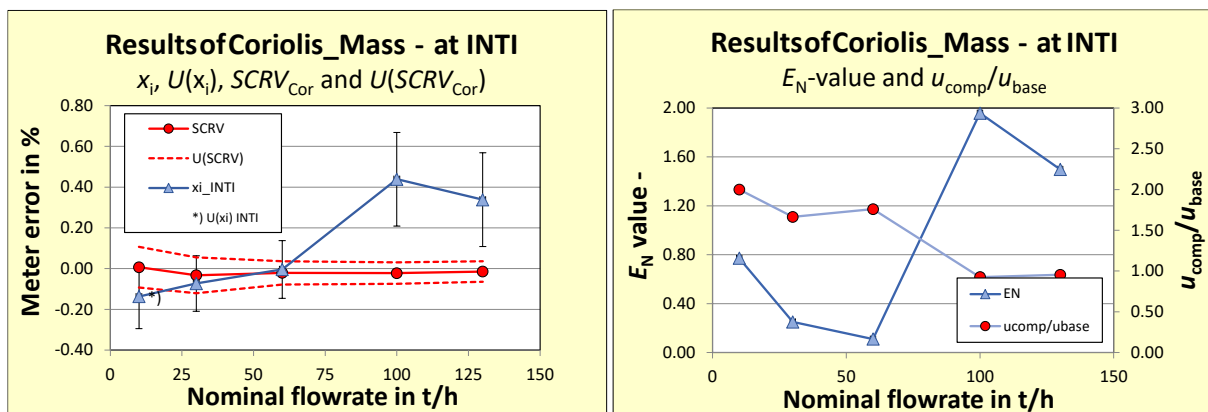


Figure 52: Comparison results of INTI laboratory for Coriolis\_Mass transfer meter



## 9 Nomenclature and unit symbols

### Terms and abbreviations

BIPM	Bureau International des Poids et Mesures
CCM	Consultative Committee for Mass and Related Quantities
CCM.FF-K1.2015	Official identifier of Key Comparison CCM-K1.2015
CENAM	Centro Nacional de Metrología - Mexico
CIPM	International Committee for Weights and Measures
CISA	Calibraciones Industriales S.A. - Chile
CMC	Calibration and Measurement Capabilities
DN	Inner pipe diameter (mm)
DoE	Degree of Equivalence
EURAMET	The European Association of National Metrology Institutes
GUM	Guide to the Expression of Uncertainty in Measurement
IBMETRO	Instituto Boliviano de Metrología - Bolivia
INACAL	Instituto Nacional de Calidad - Peru
KC1	Key comparison CCM.FF-K1.2015
KCRV	Key comparison reference value
MRA	(CIPM) Mutual Recognition Arrangement
NMI	National Metrology Institute
PTB	Physikalisch-Technische Bundesanstalt - Germany
RMO	Regional Metrology Organisation
SC	Supplementary Comparison
SIM	Sistema Interamericano de Metrología
TP	Technical Protocol
WGFF	(CCM) Working Group on Fluid Flow

### Symbols and units

$d_i$	Degree of equivalence (DoE) as the difference of SIM-participant $i$ to $SCRV_{cor}$ (%)
$\Delta e_{nom}$	Difference of meter error (%)
$e$	Meter error at current temperature conditions (%)
$e_{cor}$	Temperature corrected meter error (%)
$\Delta e_{cor}$	Correction value of meter error (%)
$e_{mean}$	Mean values of meter error at one flow rate over all temperatures (%)
$E_{N,i}$	Normalized Degree of Equivalence as the difference of SIM-participant $i$ to $SCRV$ (%)
$e_{nom}$	Meter error at nominal temperature of 20 °C (%)
$e_m$	Relative measurement error of Coriolis meter – mass (%)
$e_{m,cor}$	Temperature corrected measurement error of Coriolis meter (%)
$e_{residual}$	Model residuals (%)
$e_v$	Relative measurement error of turbine meter – volume (%)
$e_{v,cor}$	Temperature corrected measurement error of turbine meter (%)
$i$	Laboratory index

$k$	Coverage factor (-)
$KCRV$	Key Comparison Reference value of KC1 (%)
$K_m$	meter $K$ -factor - mass-related output (Coriolis meter) (pulses/kg)
$K_{m,nom}$	Nominal $K$ -factor of Coriolis meter - mass output (pulses/kg)
$K_V$	meter $K$ -factor - volume-related output (turbine meter) (pulses/L)
$\Delta K_V$	Difference in meter $K$ -factor of turbine meter (%)
$K_{V,nom}$	Nominal $K$ -factor of turbine meter (pulses/L)
$m_{ref}$	Mass, measured by the reference standard (kg)
$n$	Number of measurements at calibrated test point (-)
$N$	Counted number of pulses by the transfer meter (pulses)
$p_{fluid}$	Line pressure (bar)
$s$	Standard deviation of the mean of measurements at one flowrate point (%)
$SCC_i$	Supplementary comparison correction for laboratory $i$ (%)
$SCRV$	Supplementary Comparison Reference value (%)
$SCRV_{Cor}$	Reference value of the comparison for Coriolis_Mass meter (%)
$SCRV_{Turb}$	Reference value of the comparison for turbine meter (%)
$T_{air}$	Air temperature ( $^{\circ}C$ )
$T_{fluid}$	Fluid temperature ( $^{\circ}C$ )
$\Delta T_{fluid}$	Difference of current fluid temperature to nominal temperature of 20 $^{\circ}C$ ( $^{\circ}C$ )
$T_{nom}$	Nominal fluid temperature of 20 $^{\circ}C$
$u_{base,i}$	Standard uncertainty of laboratory reference (%)
$u_{comp}$	Standard uncertainty of transfer meter measurements (%)
$u_{TS}$	Standard uncertainty of transfer meter (%)
$U_{d,i}$	Extended uncertainty of $d_i$ of participant $i$ during SIM comparison (%)
$u_{drift}$	Standard uncertainty due to drift of transfer meter (%)
$u_{reprod}$	Standard uncertainty due to reproducibility characteristics of transfer meter (%)
$u_{SCC_i}$	Uncertainty of $SCC$ for laboratory $i$ (%)
$u_{temp}$	Standard uncertainty caused by temperature characteristics of transfer meter (%)
$u_{pres}$	Standard uncertainty caused by pressure characteristics of transfer meter (%)
$u_{flow}$	Standard uncertainty due to sensitivity of transfer meter to instable flow conditions (%)
$u_{inflow}$	Standard uncertainty due to sensitivity of turbine meter to different inflow conditions (%)
$u_{KCRV}$	Standard uncertainty of Key comparison reference value during KC1 (%)
$u_{SCRV,Cor}$	Standard uncertainty of $SCRV_{Cor}$ (%)
$u_{x,i}$	Standard uncertainty of reported and temperature corrected meter error (%)
$u_{x,Cor,i}$	Uncertainty of $x_{Cor,i}$ for reference laboratory $i$ during SIM comparison (%)
$u_{x,KC1,i}$	Uncertainty of calibration results of laboratory $i$ during KC1 (%)
$V_{ref}$	Volume, measured by the reference standard ( $m^3$ )
$x_i$	Temperature corrected meter error for $E_N$ -value evaluation
$x_{KC1,i}$	Results of laboratory $i$ during KC1 (%)
$x_{Cor,i}$	By $SCC_i$ corrected results of reference laboratory $i$ during SIM comparison (%)

## 10 References

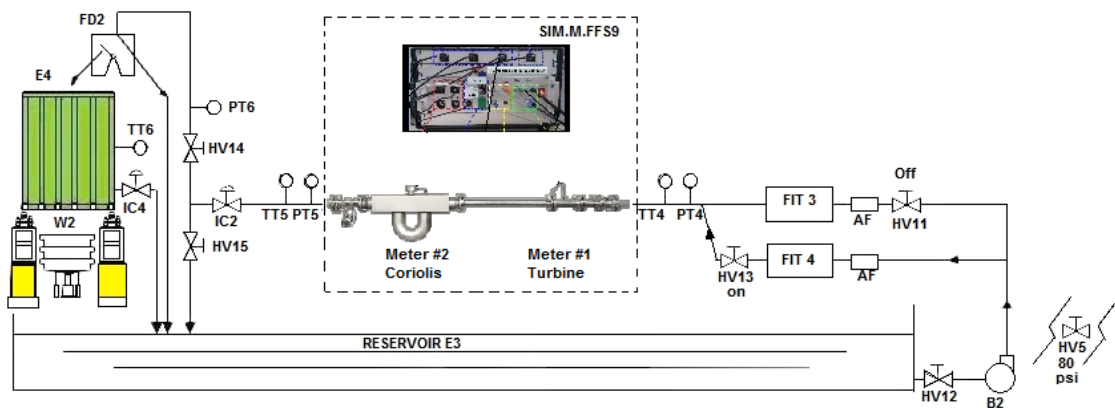
- [1] *Technical Protocol for Key Comparison CCM.FF-K1.2015*. Draft 5/3. Unpublished. 23.01.2017
- [2] Personal communications
- [3] GUM – *Guide to the Expression of Uncertainty in Measurement*, JCGM 100:2008.
- [4] BIPM: *WGFF Guidelines for CMC Uncertainty and Calibration Report Uncertainty*. 21.10.2013, <http://www.bipm.org/utis/en/pdf/ccm-wgff-guidelines.pdf>
- [5] WRIGHT, J. et al. (2016): *Transfer standard uncertainty can cause inconclusive inter-laboratory comparisons*. In: *Metrologia* 53 (2016) 1243 - 1258
- [6] Cox M. G.: *Evaluation of key comparison data*, *Metrologia* 39 (2002) 589 - 595

## 11 Appendices

### 11.1 Information about participating laboratories

NMI/DI	Country	RMO	Contact	Address
<b>PTB</b>	Germany	EURAMET	Enrico Frahm enrico.frahm@ptb.de	<b>PTB - Physikalisch-Technische Bundesanstalt</b> Department 1.5 Liquid Flow Bundesallee 100 38116 Braunschweig, Germany
<b>CENAM</b>	Mexico	SIM/ Noramet	Roberto Arias Romero rarias@cenam.mx	<b>CENAM - Centro Nacional de Metrología</b> km 4.5 carretera a los Cués, El Marqués, Querétaro México, 76246
<b>CISA</b>	Chile	SIM	Jeny Vargas Angel j.vargas@ci-sa.com	<b>Calibraciones Industriales S.A.</b> Nacional Flujo Líquido Barros Arana 73 Iquique República de Chile
<b>INACAL</b>	Peru	SIM	Adriel Arredondo aarredondo@inacal.gob.pe	<b>Instituto Nacional de Calidad</b> Laboratorio de Flujo de Líquidos Calle De La Prosa 150, San Borja, Lima 41 Perú
<b>IBMETRO</b>	Bolivia	SIM	Juan José Mendoza Aguirre jjmendoza@ibmetro.gob.bo	<b>Instituto Boliviano de Metrología</b> Av. Camacho Nro. 1488 La Paz Bolivia
<b>INTI</b>	Argentina	SIM	Marcelo Alejandro Silvosa msilvosa@inti.gob.ar	<b>INSTITUTO NACIONAL DE TECNOLOGÍA INDUSTRIAL</b> Dirección Técnica de Eficiencia Energética Subgerencia de Áreas de Conocimiento Parque Tecnológico Miquelete Av. General Paz 5445 B1650WAB San Martín Buenos Aires Argentina

Characteristic information of primary standard used during SC	Working procedure																
<p><b>CISA – Chile</b></p> <table border="1"> <tr> <td>Range of flowrate</td> <td>8 to 300 t/h</td> </tr> <tr> <td>Fluid temperature</td> <td>17 °C to 28 °C</td> </tr> <tr> <td>Line pressure</td> <td>3 bar</td> </tr> <tr> <td>Uncertainty (k = 2)</td> <td>0.15 % (Reading)</td> </tr> <tr> <td>Reference</td> <td>Weighing System Max. Cap: 3000 kg</td> </tr> <tr> <td>Operating method</td> <td>Diverter-operated flying start and finish</td> </tr> <tr> <td>Calibration line diameter</td> <td>80 mm (used during SC) Note: Max Diameter 250 mm</td> </tr> <tr> <td>Test fluid</td> <td>Cold water</td> </tr> </table>	Range of flowrate	8 to 300 t/h	Fluid temperature	17 °C to 28 °C	Line pressure	3 bar	Uncertainty (k = 2)	0.15 % (Reading)	Reference	Weighing System Max. Cap: 3000 kg	Operating method	Diverter-operated flying start and finish	Calibration line diameter	80 mm (used during SC) Note: Max Diameter 250 mm	Test fluid	Cold water	<p>Gravimetric calibration – static weighing – method.</p> <p>The used method for flowmeter calibration (Coriolis and Turbine) is Gravimetric Method.</p> <p>The gravimetric method comprises weighing the collected water, and time registration. The initial mass (<math>m_0</math>) is automatically registered before the diverter turns the flow towards the weighing tank, starting the measurement of time. After collecting an appropriate amount of liquid, the diverter is activated in the opposed direction, turning aside the water towards the reserve tank; automatically, the measurement of the time stops. Thus, the time of filling (<math>t</math>) of the weighing tank is determined. When the movement of the water in the weighing tank has stopped, the final mass (<math>m_1</math>) is registered. Then, the weighing tank is drained.</p>
Range of flowrate	8 to 300 t/h																
Fluid temperature	17 °C to 28 °C																
Line pressure	3 bar																
Uncertainty (k = 2)	0.15 % (Reading)																
Reference	Weighing System Max. Cap: 3000 kg																
Operating method	Diverter-operated flying start and finish																
Calibration line diameter	80 mm (used during SC) Note: Max Diameter 250 mm																
Test fluid	Cold water																



Characteristic information of primary standard used during SC		Working procedure																
<b>INACAL – Peru</b> <table border="1"> <tr> <td>Range of flowrate</td> <td>0.26 m<sup>3</sup>/h – 130 m<sup>3</sup>/h</td> </tr> <tr> <td>Fluid temperature</td> <td>15 °C – 30 °C</td> </tr> <tr> <td>Line pressure</td> <td>up to 3 bar</td> </tr> <tr> <td>Uncertainty (k = 2)</td> <td>0.26 m<sup>3</sup>/h – 10 m<sup>3</sup>/h : 0.11 % 10 m<sup>3</sup>/h – 130 m<sup>3</sup>/h : 0.08 % mass, volume</td> </tr> <tr> <td>Reference</td> <td>Weighing method</td> </tr> <tr> <td>Operating method</td> <td>Flying start and stop</td> </tr> <tr> <td>Calibration line diameter</td> <td>DN06 – DN100</td> </tr> <tr> <td>Test fluid</td> <td>Water</td> </tr> </table>		Range of flowrate	0.26 m <sup>3</sup> /h – 130 m <sup>3</sup> /h	Fluid temperature	15 °C – 30 °C	Line pressure	up to 3 bar	Uncertainty (k = 2)	0.26 m <sup>3</sup> /h – 10 m <sup>3</sup> /h : 0.11 % 10 m <sup>3</sup> /h – 130 m <sup>3</sup> /h : 0.08 % mass, volume	Reference	Weighing method	Operating method	Flying start and stop	Calibration line diameter	DN06 – DN100	Test fluid	Water	The static weighing system for flow determination represents the National Liquid Flow Standard of Peru. The static weighing system has two independent flow measurement lines; each one consists of a diverter, a set of nozzles for every flow interval and a weighing system, with maximum load capacities of 500 kg and 2000 kg, respectively. The test flow is established by means of frequency converters. Piping lengths upstream of 15D and downstream of 10D are available. The temperature of the test water is not controlled.
Range of flowrate	0.26 m <sup>3</sup> /h – 130 m <sup>3</sup> /h																	
Fluid temperature	15 °C – 30 °C																	
Line pressure	up to 3 bar																	
Uncertainty (k = 2)	0.26 m <sup>3</sup> /h – 10 m <sup>3</sup> /h : 0.11 % 10 m <sup>3</sup> /h – 130 m <sup>3</sup> /h : 0.08 % mass, volume																	
Reference	Weighing method																	
Operating method	Flying start and stop																	
Calibration line diameter	DN06 – DN100																	
Test fluid	Water																	



Fig. 1: Diverter and nozzle

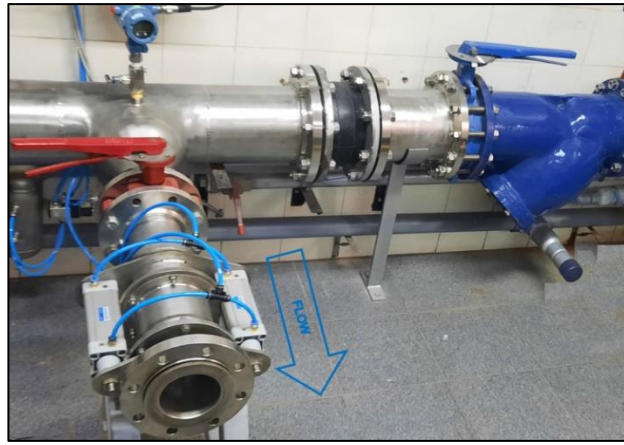


Fig. 2: Water flow entry

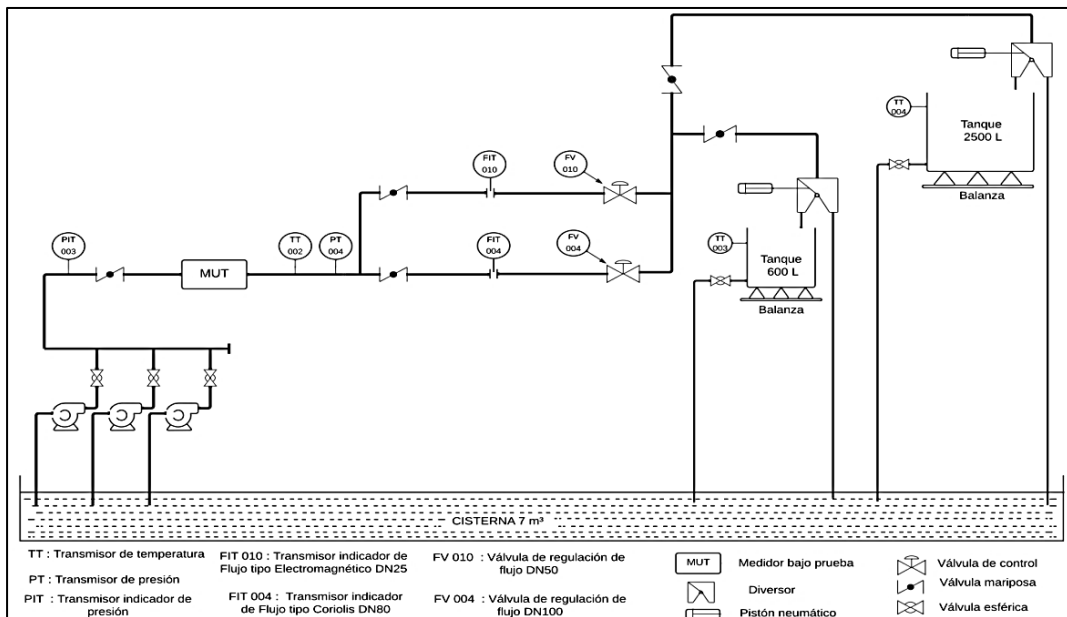
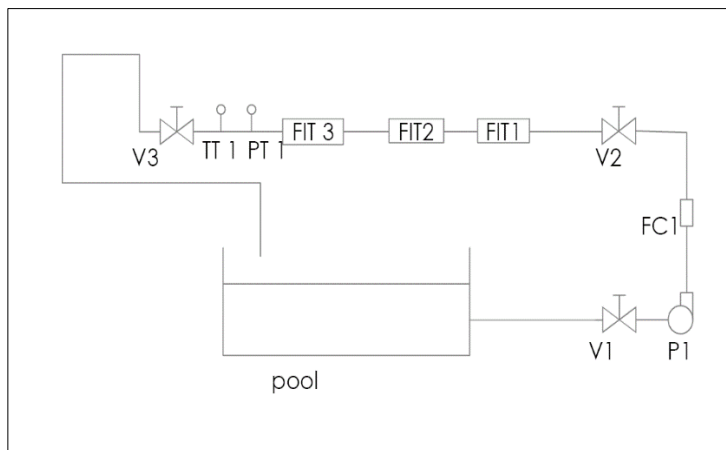


Fig. 3: Instrumentation diagram and the main components of the Static Weighing System

Characteristic information of primary standard used during SC	Working procedure																
<p><b>IBMETRO – Bolivia</b></p> <table border="1"> <tr> <td>Range of flowrate</td> <td>3 m<sup>3</sup>/h – 100 m<sup>3</sup>/h</td> </tr> <tr> <td>Fluid temperature</td> <td>16 °C – 28 °C</td> </tr> <tr> <td>Line pressure</td> <td>up to 3 bar</td> </tr> <tr> <td>Uncertainty (k = 2)</td> <td>0.10 %</td> </tr> <tr> <td>Reference</td> <td>master meter (Electromagnetic Flow meter)</td> </tr> <tr> <td>Operating method</td> <td>flying start stop</td> </tr> <tr> <td>Calibration line diameter</td> <td>50 mm ... 125 mm</td> </tr> <tr> <td>Test fluid</td> <td>water</td> </tr> </table>	Range of flowrate	3 m <sup>3</sup> /h – 100 m <sup>3</sup> /h	Fluid temperature	16 °C – 28 °C	Line pressure	up to 3 bar	Uncertainty (k = 2)	0.10 %	Reference	master meter (Electromagnetic Flow meter)	Operating method	flying start stop	Calibration line diameter	50 mm ... 125 mm	Test fluid	water	<p>The calibration points of the flow meter under test (MUT) are established according to the comparison standards. Start the data acquisition program in the computer to determine the number of pulses to capture. The pulses were collected from MUT and the Electromagnetic Flow meter (reference meter). For each measurement, record the number of pulses from the reference meter and MUT. Also, fluid temperature, line pressure and measurement time were recorded. The ambient conditions at the beginning and at the end of each test flow were recorded.</p>
Range of flowrate	3 m <sup>3</sup> /h – 100 m <sup>3</sup> /h																
Fluid temperature	16 °C – 28 °C																
Line pressure	up to 3 bar																
Uncertainty (k = 2)	0.10 %																
Reference	master meter (Electromagnetic Flow meter)																
Operating method	flying start stop																
Calibration line diameter	50 mm ... 125 mm																
Test fluid	water																



Calibration line



Schematic diagram of the flow line

TAG	DESCRIPTION
V1	Valve
P1	Pump
FC1	Flow stabilizer
V2	Valve
FIT 1	Meter under Test Turbine
FIT 2	Meter under Test Coriolis
FIT 3	Flow meter Krohne
PT 1	Pressure Sensor
TT 1	Temperature Sensor
V3	Valve
pool	Recipe

Characteristic information of primary standard used during SC		Working procedure
<b>INTI - Argentina</b>		The calibration system consists of two reference systems, a volumetric tank and a reference meter. Flow and line pressure are regulated by pump and valves. The calibration starts at zero flow with an enabled pump, the manual tank inlet valve will be opened at the same time as the time count begins. To calculate the density and the corrected volume of the tank, the temperature of the water is measured as well as the temperature difference compared to the reference temperature of 20 °C at which the tank was calibrated.
Range of flowrate	0.12 m <sup>3</sup> /h – 130 m <sup>3</sup> /h	
Fluid temperature	15 °C – 30 °C	
Line pressure	up to 3 bar	
Uncertainty (k = 2)	Volumetric tank mass: 0.07 % volume: 0.06 % Master meter mass: 0.22 % volume: 0.20 %	
Reference	Volumetric tank Master meter (turbine meter)	
Operating method	standing-start-stop	
Calibration line diameter	25 mm, 50 mm, 100 mm, 150 mm	
Test fluid	water	



Installed MUT during comparison calibration



Reference turbine meter

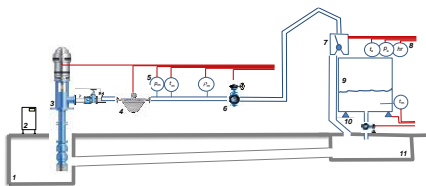


Calibration test rig





Characteristic information of primary standard used during KC	Working procedure																
<p><b>CENAM – Mexico</b></p> <table border="1"> <tr> <td data-bbox="204 353 427 387">Range of flow rate</td> <td data-bbox="443 353 778 387">(100... 12 000) kg/min</td> </tr> <tr> <td data-bbox="204 387 427 421">Fluid temperature</td> <td data-bbox="443 387 778 454">Ambient (not controlled) (15...27) °C</td> </tr> <tr> <td data-bbox="204 454 427 488">Line pressure</td> <td data-bbox="443 454 778 488">up to 10 bar</td> </tr> <tr> <td data-bbox="204 488 427 589">Uncertainty</td> <td data-bbox="443 488 778 589"><math>U(q_m)/\% = 0.030</math> <math>U(q_v)/\% = 0.038</math> <math>k = 2</math></td> </tr> <tr> <td data-bbox="204 589 427 622">Reference</td> <td data-bbox="443 589 778 622">Gravimetric</td> </tr> <tr> <td data-bbox="204 622 427 656">Operating method</td> <td data-bbox="443 622 778 656">Flying-start-stop</td> </tr> <tr> <td data-bbox="204 656 427 723">Calibration line diameter</td> <td data-bbox="443 656 778 723">100 mm 200 mm</td> </tr> <tr> <td data-bbox="204 723 427 757">Test fluid</td> <td data-bbox="443 723 778 757">Water</td> </tr> </table>	Range of flow rate	(100... 12 000) kg/min	Fluid temperature	Ambient (not controlled) (15...27) °C	Line pressure	up to 10 bar	Uncertainty	$U(q_m)/\% = 0.030$ $U(q_v)/\% = 0.038$ $k = 2$	Reference	Gravimetric	Operating method	Flying-start-stop	Calibration line diameter	100 mm 200 mm	Test fluid	Water	<p>The Mexican Primary Measurement System for Water Flow is of the Static Weighing Design.</p> <p>The gravimetric reference consists of two independent diverter and weighing systems; which maximum load capacities are 1500 kg and 10 000 kg, respectively.</p> <p>Flow is controlled by means of frequency converter and throttling valves.</p> <p>More than <math>100D</math> upstream pipe length is available for calibrations.</p> <p>No fluid temperature control available.</p>
Range of flow rate	(100... 12 000) kg/min																
Fluid temperature	Ambient (not controlled) (15...27) °C																
Line pressure	up to 10 bar																
Uncertainty	$U(q_m)/\% = 0.030$ $U(q_v)/\% = 0.038$ $k = 2$																
Reference	Gravimetric																
Operating method	Flying-start-stop																
Calibration line diameter	100 mm 200 mm																
Test fluid	Water																



**Fig. 1:** Schematic diagram of CENAM water flow facility



**Fig. 2:** A view of the load cell at the 10 000 kg tank



**Fig. 3:** Front view of the static weighing system at CENAM Primary System for Water Flow

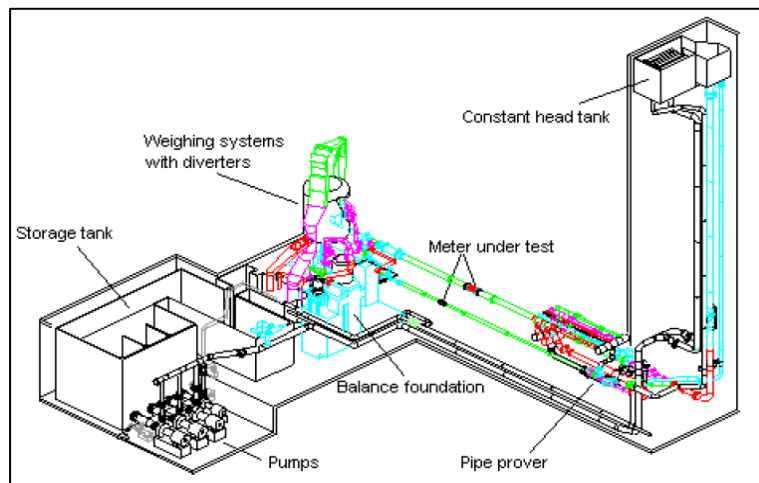
Characteristic information of primary standard used during KC		Working procedure																
<b>PTB – Germany</b> <table border="1"> <tr> <td>Range of flowrate</td> <td>0.3 m<sup>3</sup>/h ... 2,100 m<sup>3</sup>/h</td> </tr> <tr> <td>Fluid temperature</td> <td>10 °C ... 35 °C</td> </tr> <tr> <td>Line pressure</td> <td>2 bar ... 6 bar</td> </tr> <tr> <td>Uncertainty (k = 2)</td> <td>0.02 volume, mass</td> </tr> <tr> <td>Reference</td> <td>gravimetric</td> </tr> <tr> <td>Operating method</td> <td>Direct pumping , constant head tank flying-/ standing-start-stop</td> </tr> <tr> <td>Calibration line diameter</td> <td>25 mm ... 400 mm</td> </tr> <tr> <td>Test fluid</td> <td>water</td> </tr> </table>		Range of flowrate	0.3 m <sup>3</sup> /h ... 2,100 m <sup>3</sup> /h	Fluid temperature	10 °C ... 35 °C	Line pressure	2 bar ... 6 bar	Uncertainty (k = 2)	0.02 volume, mass	Reference	gravimetric	Operating method	Direct pumping , constant head tank flying-/ standing-start-stop	Calibration line diameter	25 mm ... 400 mm	Test fluid	water	<p>The PTB hydrodynamic test field (HDP) represents the national primary standard of Germany for the realization of the measurands volumetric and mass flow rate as well as the total volume and mass of flowing liquids (water).</p> <p>The gravimetric reference consists of three independent diverter and balance systems with max. loads of 30 t, 3 t and 300 kg. For generating and stabilizing flow rates, the supply system consists of a 400 m<sup>3</sup> storage tank, of a frequency controlled pumping system, a constant head tank (30 m<sup>3</sup>, at a height of 30 m) and two calibration lines. For each diameter an upstream straight pipeline with a length of 50D and downstream of 20D is available. The fluid temperature is adjusted and controlled by two separate heat exchanger systems.</p>
Range of flowrate	0.3 m <sup>3</sup> /h ... 2,100 m <sup>3</sup> /h																	
Fluid temperature	10 °C ... 35 °C																	
Line pressure	2 bar ... 6 bar																	
Uncertainty (k = 2)	0.02 volume, mass																	
Reference	gravimetric																	
Operating method	Direct pumping , constant head tank flying-/ standing-start-stop																	
Calibration line diameter	25 mm ... 400 mm																	
Test fluid	water																	



Upstream view to calibration lines



3 t balance and diverter system



Principle drawing of the Hydrodynamic Test Field







INACAL Laboratory – Day#1

Data report INACAL: Day#1		*Original data set										Temperature correction of meter error																													
Date	Nominal flowrate V <sub>nom</sub> [m³/h]	Laboratory reference										Fluid					Ambient conditions					Turbine meter					Coriolis_Mass					Coriolis_Vol					Corrected meter error				
		Measur-rement time t [s]	Standard mass flowrate m <sup>ref</sup> [l/h]	Standard volume flowrate V <sup>ref</sup> [m³/h]	Mass m <sub>ref</sub> [kg]	Volume V <sub>ref</sub> [m³]	Water density ρ <sub>fluid</sub> [kg/m³]	Line pressure p <sub>fluid</sub> [bar]	Water temp. T <sub>fluid</sub> [°C]	Air temp. T <sub>air</sub> [°C]	Air pressure p <sub>air</sub> [bar]	Pulse count	K-factor	Meter error e <sub>v</sub> [%]	Pulse count	K-factor	Meter error e <sub>m</sub> [%]	Pulse count	K-factor	Meter error e <sub>m</sub> [%]	Pulse count	K-factor	Meter error e <sub>v</sub> [%]	Pulse count	K-factor	Meter error e <sub>v</sub> [%]	ΔT <sub>fluid</sub> [°C]	e <sub>cor,v</sub> [%]	e <sub>cor,m</sub> [%]	T <sub>nom</sub> [°C]	20 [°C]										
13.03.2017	10	116.482	10.273	10.302	338.086	0.339	997.161	2.15	25.57	24.80	992.70	3910	11.5323	0.412	48779	144.2799	0.155	9781	28.8484	0.168	5.572	0.384	0.228																		
13.03.2017	10	141.587	10.210	10.238	401.595	0.403	997.272	2.15	25.15	25.00	992.40	4644	11.5323	0.412	57906	144.1899	0.093	11612	28.8358	0.124	5.146	0.383	0.160																		
13.03.2017	10	133.559	10.061	10.090	373.267	0.374	997.161	2.15	25.57	25.00	992.40	4318	11.5303	0.438	53803	144.1206	0.059	10791	28.8275	0.096	5.572	0.410	0.132																		
13.03.2017	10	141.591	10.042	10.070	394.952	0.396	997.158	2.15	25.58	25.00	992.40	4567	11.5306	0.397	56924	144.1290	0.051	11416	28.8277	0.079	5.583	0.370	0.134																		
13.03.2017	10	134.009	10.008	10.037	372.560	0.374	997.156	2.15	25.59	25.10	992.30	4310	11.5357	0.441	53722	144.1968	0.098	10772	28.8312	0.108	5.594	0.414	0.171																		
13.03.2017	30	231.027	30.141	30.227	1934.260	1.940	997.141	2.19	25.65	25.30	991.80	22393	11.5439	0.513	278399	143.9305	-0.087	55573	28.6487	-0.525	5.649	0.544	-0.013																		
13.03.2017	30	230.808	30.121	30.208	1931.162	1.937	997.120	2.19	25.73	25.40	991.60	22354	11.5421	0.497	277988	143.9486	-0.075	55478	28.6450	-0.538	5.731	0.529	0.001																		
13.03.2017	30	228.048	30.119	30.207	1907.970	1.914	997.096	2.19	25.82	25.40	991.40	22079	11.5384	0.465	274659	143.9535	-0.071	54815	28.6461	-0.535	5.821	0.498	0.005																		
13.03.2017	30	227.785	30.105	30.194	1904.871	1.910	997.076	2.19	25.90	25.60	991.30	22045	11.5391	0.471	274309	144.0040	-0.036	54755	28.6607	-0.484	5.896	0.505	0.041																		
13.03.2017	60	116.970	60.008	60.188	1949.755	1.956	997.001	2.02	26.18	25.70	990.90	22587	11.5408	0.564	280887	144.0627	0.005	55718	28.4912	-1.072	6.178	0.603	0.086																		
13.03.2017	60	117.683	60.011	60.194	1961.751	1.968	996.960	2.02	26.33	25.90	990.80	22709	11.5407	0.485	282661	144.0861	0.021	56077	28.4983	-1.048	6.333	0.524	0.105																		
13.03.2017	60	117.300	59.916	60.101	1952.254	1.958	996.922	2.01	26.47	25.90	990.80	22602	11.5418	0.494	281358	144.1196	0.044	55823	28.5061	-1.020	6.472	0.534	0.130																		
13.03.2017	60	117.230	59.961	60.148	1952.554	1.959	996.884	2.01	26.61	26.00	990.80	22614	11.5457	0.528	281434	144.1261	0.049	55833	28.5058	-1.022	6.613	0.569	0.136																		
13.03.2017	60	119.703	59.909	60.099	1992.040	1.998	996.845	2.01	26.76	26.00	990.60	23085	11.5521	0.584	287118	144.1327	0.053	56864	28.5056	-1.022	6.758	0.626	0.143																		
13.03.2017	100	72.162	99.363	99.685	1991.740	1.998	996.777	2.00	27.01	26.00	990.40	23074	11.5475	0.544	287080	144.1353	0.055	57744	28.8983	0.341	7.005	0.676	0.148																		
13.03.2017	100	70.122	99.986	100.317	1947.556	1.954	996.706	2.02	27.26	26.10	990.30	22552	11.5415	0.492	280663	144.1104	0.038	56444	28.8865	0.300	7.262	0.525	0.135																		
13.03.2017	100	70.300	100.572	100.912	1963.950	1.971	996.630	2.03	27.54	26.20	990.10	22739	11.5392	0.472	283034	144.1147	0.041	56923	28.8863	0.300	7.536	0.506	0.142																		
13.03.2017	100	70.982	99.712	100.055	1966.049	1.973	996.576	2.00	27.73	26.20	990.10	22779	11.5465	0.536	283327	144.1098	0.037	56976	28.8807	0.280	7.728	0.571	0.141																		
13.03.2017	100	70.817	100.051	100.400	1968.148	1.975	996.526	2.01	27.91	26.30	989.90	22802	11.5453	0.525	283586	144.0877	0.022	57084	28.8778	0.270	7.909	0.560	0.129																		
13.03.2017	130	54.974	129.147	129.608	1972.147	1.979	996.446	1.70	28.19	26.30	989.80	22869	11.5548	0.608	284193	144.1034	0.033	57167	28.8842	0.292	8.190	0.641	0.144																		
13.03.2017	130	55.121	129.561	130.034	1983.743	1.991	996.363	1.97	28.48	26.20	990.00	23007	11.5556	0.615	285821	144.0817	0.018	57896	28.8782	0.271	8.481	0.649	0.133																		
13.03.2017	130	54.080	129.332	129.829	1942.857	1.950	996.169	2.00	29.15	26.20	990.00	22498	11.5355	0.440	279923	144.0780	0.015	56326	28.8803	0.279	9.149	0.477	0.141																		
13.03.2017	130	54.571	129.738	130.249	1966.649	1.974	996.078	2.01	29.46	26.30	990.20	22774	11.5347	0.433	283284	144.0440	-0.008	57004	28.8717	0.249	9.461	0.471	0.122																		
13.03.2017	130	54.586	129.332	129.853	1961.051	1.969	995.993	1.99	29.75	26.30	990.20	22726	11.5422	0.498	282459	144.0345	-0.015	56838	28.8673	0.234	9.746	0.538	0.120																		

**INACAL Laboratory – Day#2**

Data report INACAL: Day#2		*Original dataset												Temperature correction of meter error																													
Date	Nominal flowrate $V_{nom}$ [m³/h]	Laboratory reference											Turbine meter			Coriolis_Mass			Coriolis_Vol			Corrected meter error																					
		Measur- ement time	Standard mass flowrate	Standard volume flowrate	Mass	Volume	Water density	Water pressure	Water temp.	Air temp.	Air pressure	Fluid			Pulse count	K-factor	e <sub>v</sub>	Pulse count	K-factor	e <sub>m</sub>	Pulse count	K-factor	e <sub>v</sub>	Pulse count	K-factor	e <sub>m</sub>	(T <sub>fluid</sub> - T <sub>nom</sub> )	ΔT <sub>fluid</sub>	T <sub>nom</sub>	20	1°C												
		t	m <sup>*</sup> <sub>ref</sub>	V <sup>*</sup> <sub>ref</sub>	m <sub>ref</sub>	V <sub>ref</sub>	ρ <sub>fluid</sub>	p <sub>fluid</sub>	T <sub>fluid</sub>	T <sub>air</sub>	p <sub>air</sub>	ρ <sub>fluid</sub>	p <sub>fluid</sub>	T <sub>fluid</sub>	T <sub>air</sub>	p <sub>air</sub>	N	K <sub>v</sub>	e <sub>v</sub>	N	K <sub>m</sub>	e <sub>m</sub>	N	K <sub>v</sub>	e <sub>v</sub>	N	K <sub>v</sub>	e <sub>v</sub>	N	K <sub>v</sub>	e <sub>v</sub>	N	K <sub>v</sub>	e <sub>v</sub>	N	K <sub>v</sub>	e <sub>v</sub>	N	K <sub>v</sub>	e <sub>v</sub>	N	K <sub>v</sub>	e <sub>v</sub>
14.03.2017	10	152.869	10.411	10.449	441.211	0.443	996.354	2.08	28.51	22.70	993.80	5883	11.4786	-0.056	62986	142.7571	-0.902	12659	28.5417	-0.897	8.512	-0.065	-0.786																				
14.03.2017	10	137.512	10.299	10.336	393.385	0.395	996.365	2.08	28.47	23.10	993.90	4537	11.4913	0.055	56167	142.7786	-0.887	11271	28.5472	-0.878	8.473	0.046	-0.771																				
14.03.2017	10	137.043	10.302	10.339	392.160	0.394	996.365	2.08	28.47	22.70	993.70	4522	11.4891	0.036	55959	142.6943	-0.945	11229	28.5296	-0.939	8.473	0.026	-0.830																				
14.03.2017	10	137.791	10.270	10.308	393.086	0.395	996.357	2.08	28.50	22.70	993.70	4335	11.4949	0.086	56052	142.5949	-1.014	11248	28.5104	-1.006	8.503	0.077	-0.899																				
14.03.2017	10	141.501	10.273	10.311	403.801	0.405	996.352	2.08	28.52	22.70	993.70	4663	11.5056	0.180	57514	142.4317	-1.128	11559	28.4717	-1.140	8.520	0.171	-1.012																				
14.03.2017	30	228.894	30.268	30.378	1924.476	1.931	996.365	2.11	28.47	22.80	993.70	22228	11.5082	0.202	276072	143.4631	-0.419	55141	28.5483	-0.874	8.473	0.264	-0.303																				
14.03.2017	30	228.168	30.258	30.369	1917.772	1.925	996.370	2.10	28.46	23.60	993.50	22156	11.5111	0.227	275256	143.5290	-0.366	54983	28.5662	-0.812	8.456	0.289	-0.251																				
14.03.2017	30	230.767	30.241	30.351	1938.485	1.946	996.369	2.10	28.46	23.60	993.50	22385	11.5057	0.181	278232	143.5306	-0.365	55573	28.5642	-0.819	8.459	0.242	-0.250																				
14.03.2017	30	229.294	30.246	30.357	1925.978	1.933	996.356	2.10	28.51	23.80	993.40	22441	11.5058	0.181	276469	143.5474	-0.353	55225	28.5693	-0.801	8.505	0.244	-0.237																				
14.03.2017	60	119.022	59.335	59.553	1961.715	1.969	996.341	2.00	28.56	24.00	993.30	22654	11.5058	0.181	282091	143.7982	-0.179	56000	28.4420	-1.243	8.558	0.233	-0.062																				
14.03.2017	60	118.136	59.716	59.986	1959.613	1.967	996.335	1.99	28.58	23.90	993.10	22638	11.5099	0.217	281868	143.8386	-0.151	55905	28.4444	-1.235	8.580	0.269	-0.034																				
14.03.2017	60	117.376	59.728	59.951	1947.406	1.955	996.295	2.00	28.72	23.90	992.60	22927	11.5095	0.227	280118	143.8416	-0.149	55607	28.4486	-1.220	8.718	0.266	-0.030																				
14.03.2017	60	118.767	59.872	60.099	1975.223	1.983	996.224	2.01	28.96	24.00	992.50	22826	11.5110	0.240	280350	143.8351	-0.153	55652	28.4463	-1.228	8.770	0.279	-0.034																				
14.03.2017	100	71.046	100.112	100.497	1975.711	1.983	996.168	2.06	29.15	24.50	992.10	22850	11.5211	0.315	284199	143.8465	-0.145	57194	28.8376	0.131	9.154	0.356	-0.020																				
14.03.2017	100	69.718	100.020	100.409	1936.986	1.945	996.123	2.05	29.31	24.50	992.10	22998	11.5185	0.292	278618	143.8410	-0.149	56657	28.8281	0.098	9.308	0.333	-0.021																				
14.03.2017	100	72.009	99.845	100.238	1999.926	2.008	996.077	2.05	29.46	24.60	992.10	23129	11.5196	0.301	287643	143.8268	-0.159	57880	28.8275	0.096	9.462	0.343	-0.029																				
14.03.2017	100	71.751	99.967	100.367	1982.422	2.000	996.014	2.05	29.68	24.20	992.10	23043	11.5182	0.298	286566	143.8280	-0.158	57667	28.8278	0.097	9.675	0.341	-0.024																				
14.03.2017	100	69.990	100.234	100.639	1948.694	1.957	995.974	2.06	29.81	24.20	992.10	22548	11.5242	0.342	280300	143.8399	-0.150	56432	28.8423	0.147	9.809	0.386	-0.014																				
14.03.2017	130	55.043	129.703	130.236	1983.116	1.991	995.905	2.01	30.04	24.20	992.10	22948	11.5243	0.342	283317	143.8731	-0.127	57398	28.8248	0.086	10.039	0.383	0.013																				
14.03.2017	130	55.066	129.090	129.637	1974.210	1.983	995.783	2.06	30.44	24.00	992.00	22854	11.5275	0.370	283998	143.8540	-0.140	57164	28.8333	0.116	10.443	0.412	0.006																				
14.03.2017	130	54.736	129.226	129.792	1964.805	1.973	995.642	2.06	30.91	24.00	992.00	22755	11.5308	0.399	282664	143.8637	-0.134	56935	28.8511	0.178	10.905	0.443	0.020																				
14.03.2017	130	53.723	130.141	130.715	1942.090	1.951	995.603	2.08	31.03	23.70	992.00	22900	11.5294	0.386	279369	143.8496	-0.143	56211	28.8163	0.057	11.033	0.430	0.012																				
14.03.2017	130	54.280	129.987	130.565	1959.902	1.969	995.572	2.07	31.13	23.70	992.00	22699	11.5304	0.395	281923	143.8455	-0.146	56736	28.8202	0.070	11.131	0.440	0.011																				





IBMETRO Laboratory – Day#1

Date	Nominal flowrate	V <sub>nom</sub>	Meas-urement time	Laboratory reference							Fluid			Ambient conditions				Turbine meter				Coriolis_Mass				Coriolis_Vol				Temperature correction of meter error																																
				t	m <sup>*</sup> ref	V <sup>*</sup> ref	V <sub>ref</sub>	m <sub>ref</sub>	Volume	Water density	Line pressure	Water temp.	T <sub>fluid</sub>	Air temp.	P <sub>air</sub>	Pulse count	K-factor	e <sub>v</sub>	K <sub>v,nom</sub>	Pulses/Liter	Pulse count	K-factor	e <sub>m</sub>	K <sub>m,nom</sub>	Pulses/kg	Pulse count	K-factor	e <sub>v</sub>	K <sub>v</sub>	Pulses/Liter	Pulse count	K-factor	e <sub>v</sub>	K <sub>v,nom</sub>	Pulses/Liter	T <sub>nom</sub>	Corrected meter error	Coriolis_Mass	e <sub>cor,m</sub>																							
																																								[s]	[m³/h]	[m³]	[m³/h]	[kg]	[m³]	[kg/m³]	[bar]	[°C]	[bar]	[Pulses]	[Pulses/Liter]	[%]	[Pulses]	[Pulses/kg]	[Pulses]	[Pulses/Liter]	[°C]	[%]	[Pulses]	[Pulses/Liter]	[°C]	[%]
01.03.2018	10	301.064	10.009	10.009	10.009	0.839	997.500	2.23	17.10	18.10	0.89	0.89	9425	11.2307	-2.214	120455	143.8921	-0.114	24110	28.7291	-0.246	-2.900	-2.211	-0.142																																						
01.03.2018	10	300.871	10.014	10.039	836.910	0.839	997.500	2.21	16.80	18.00	0.89	0.89	9409	11.2144	-2.356	120446	143.9175	-0.096	24109	28.7351	-0.225	-3.200	-2.349	-0.127																																						
01.03.2018	10	301.337	10.008	10.031	837.727	0.840	997.700	2.23	16.90	18.00	0.89	0.89	9424	11.2236	-2.276	120689	143.9479	-0.075	24136	28.7450	-0.191	-3.100	-2.270	-0.105																																						
01.03.2018	10	300.454	10.014	10.034	835.742	0.837	998.000	2.23	16.90	18.00	0.89	0.89	9398	11.2226	-2.285	120291	143.9331	-0.085	24076	28.7503	-0.173	-3.100	-2.279	-0.116																																						
01.03.2018	10	301.162	10.017	10.035	838.008	0.840	998.200	2.23	17.00	18.00	0.89	0.89	9414	11.2156	-2.363	120558	143.8626	-0.134	24130	28.7426	-0.199	-3.000	-2.359	-0.163																																						
01.03.2018	30	299.817	29.902	29.956	2490.292	2.495	998.200	2.04	16.90	18.10	0.89	0.89	28376	11.3741	-0.965	358507	143.9638	-0.065	71467	28.6466	-0.533	-3.100	-0.988	-0.096																																						
01.03.2018	30	300.843	29.903	29.954	2498.891	2.503	998.300	2.04	17.10	18.10	0.89	0.89	28467	11.3725	-0.980	359724	143.9535	-0.071	71708	28.6471	-0.531	-2.900	-1.002	-0.099																																						
01.03.2018	30	301.602	29.890	29.935	2504.147	2.508	998.500	2.04	17.20	18.10	0.89	0.89	28533	11.3772	-0.939	360431	143.9336	-0.085	71851	28.6498	-0.522	-2.800	-0.961	-0.112																																						
01.03.2018	30	301.830	29.916	29.946	2508.222	2.511	999.000	2.05	17.20	18.10	0.89	0.89	28522	11.3600	-1.088	360789	143.8425	-0.148	71925	28.6470	-0.531	-2.800	-1.110	-0.175																																						
01.03.2018	30	300.953	29.923	29.950	2501.507	2.504	999.100	2.06	17.30	18.10	0.89	0.89	28499	11.3825	-0.893	359825	143.8433	-0.148	71734	28.6505	-0.519	-2.700	-0.914	-0.174																																						
01.03.2018	60	301.088	59.728	59.782	4995.416	5.000	999.100	2.06	17.60	18.30	0.89	0.89	56991	11.3984	-0.754	718343	143.8004	-0.177	142272	28.4549	-1.198	-2.400	-0.775	-0.201																																						
01.03.2018	60	301.136	59.569	59.628	4982.846	4.988	999.000	2.03	17.90	18.40	0.89	0.89	57117	11.4513	-0.294	716572	143.8078	-0.172	141914	28.4520	-1.208	-2.100	-0.312	-0.192																																						
01.03.2018	60	301.185	59.520	59.597	4979.552	4.986	998.700	2.01	18.10	18.40	0.89	0.89	57099	11.4518	-0.289	716357	143.8597	-0.136	141869	28.4533	-1.204	-1.900	-0.306	-0.154																																						
01.03.2018	60	301.161	59.483	59.567	4976.108	4.983	998.600	2.00	18.20	18.50	0.89	0.89	57051	11.4489	-0.314	715797	143.8468	-0.134	141656	28.4274	-1.294	-1.800	-0.330	-0.162																																						
01.03.2018	60	301.642	59.425	59.521	4979.234	4.987	998.400	1.99	18.30	18.50	0.89	0.89	57124	11.4541	-0.269	716505	143.8986	-0.109	141695	28.4117	-1.348	-1.700	-0.294	-0.125																																						
01.03.2018	100	301.361	97.448	97.313	8132.361	8.146	998.300	0.28	18.80	18.20	0.89	0.89	93355	11.4599	-0.218	1169720	143.8352	-0.153	234507	28.7873	-0.044	-1.200	-0.228	-0.164																																						
01.03.2018	100	301.093	96.482	96.656	8069.470	8.084	998.200	0.28	18.90	18.20	0.89	0.89	92669	11.4632	-0.190	1160540	143.8186	-0.165	232667	28.7811	-0.066	-1.100	-0.198	-0.174																																						
01.03.2018	100	301.318	96.143	96.326	8047.091	8.062	998.100	0.27	19.00	18.10	0.89	0.89	92424	11.4686	-0.187	1157520	143.8433	-0.148	232062	28.7832	-0.058	-1.000	-0.195	-0.156																																						
01.03.2018	100	301.432	96.290	96.483	8062.446	8.079	998.000	0.27	19.10	18.00	0.89	0.89	92610	11.4636	-0.186	1159710	143.8410	-0.149	232503	28.7801	-0.069	-0.900	-0.194	-0.157																																						
02.03.2018	100	301.847	96.145	96.337	8061.365	8.078	998.000	0.27	19.30	18.00	0.89	0.89	92606	11.4647	-0.177	1159610	143.8478	-0.144	232512	28.7851	-0.052	-0.700	-0.184	-0.150																																						

IBMETRO Laboratory – Day#2

Data report IBMETRO: Day#2										*Original data set										Temperature correction of meter error									
Date	Nominal flowrate [m³/h]	V <sub>nom</sub> [m³/h]	t [s]	m <sub>ref</sub> [kg]	V <sub>ref</sub> [m³]	m <sub>ref</sub> [kg]	V <sub>ref</sub> [m³]	Laboratory reference		Fluid		Ambient conditions		Turbine meter		Coriolis_Mass		Coriolis_Vol		Corrected meter error									
								Standard mass flowrate [m³/h]	Standard volume flowrate [m³/h]	Water density [kg/m³]	Line pressure [bar]	Water temp. [°C]	Air temp. [°C]	Air pressure [bar]	Pulse count	K-factor	Meter error	Pulse count	K-factor	Meter error	Pulse count	K-factor	Meter error	(T <sub>fluid</sub> - T <sub>nom</sub> ) [°C]	T <sub>nom</sub> [°C]	Corrected turbine meter error	Corbis_Mass error		
02.03.2018	10	301.197	9.980	10.000	834.979	0.837	998.000	2.01	19.00	16.90	0.89	9371	11.2006	-2.476	120064	143.7919	-0.183	28.7372	28.7372	-0.218	-1.000	-2.481	-0.191						
02.03.2018	10	301.007	9.970	9.990	833.596	0.835	998.000	1.99	19.00	17.00	0.89	9384	11.2347	-2.179	119901	143.8558	-0.153	28.7485	28.7485	-0.186	-1.000	-2.193	-0.161						
02.03.2018	10	300.871	9.966	9.984	832.946	0.834	998.200	2.01	19.10	17.00	0.89	9406	11.2721	-1.853	119768	143.7885	-0.186	28.7436	28.7436	-0.196	-0.900	-1.868	-0.193						
02.03.2018	10	301.032	9.962	9.980	833.027	0.835	998.200	2.00	19.20	17.00	0.89	9368	11.2255	-2.239	119786	143.7961	-0.180	28.7444	28.7444	-0.193	-0.800	-2.275	-0.187						
02.03.2018	10																												
02.03.2018	30	301.323	29.839	29.896	2497.573	2.502	998.100	2.01	19.00	17.20	0.89	28709	11.4729	-0.105	359229	143.8312	-0.156	28.6270	28.6270	-0.601	-1.000	-0.121	-0.164						
02.03.2018	30	301.106	29.795	29.852	2492.104	2.497	998.100	2.01	19.10	17.20	0.89	28655	11.4765	-0.074	358516	143.8608	-0.136	28.6333	28.6333	-0.579	-0.900	-0.090	-0.143						
02.03.2018	30	303.546	29.753	29.807	2508.762	2.513	998.200	2.01	19.20	17.20	0.89	28846	11.4774	-0.066	360850	143.8359	-0.153	28.6334	28.6334	-0.578	-0.800	-0.081	-0.159						
02.03.2018	30	301.634	29.777	29.837	2494.949	2.500	998.000	2.01	19.20	17.30	0.89	28696	11.4786	-0.055	358931	143.8631	-0.134	28.6318	28.6318	-0.584	-0.800	-0.070	-0.140						
02.03.2018	30	301.207	29.750	29.800	2488.105	2.493	998.300	1.99	19.30	17.30	0.89	28619	11.4782	-0.060	357971	143.8151	-0.167	28.6318	28.6318	-0.584	-0.700	-0.074	-0.172						
02.03.2018	60	301.093	59.761	59.869	4998.229	5.007	998.200	1.97	19.50	17.50	0.89	57524	11.4882	0.028	719024	143.8557	-0.159	28.4486	28.4486	-1.220	-0.500	0.022	-0.142						
02.03.2018	60	305.268	59.797	59.893	5070.580	5.079	998.400	1.93	19.80	17.70	0.89	58346	11.4884	0.029	729347	143.8390	-0.151	28.4598	28.4598	-1.202	-0.200	0.026	-0.150						
02.03.2018	60	301.362	59.761	59.857	5002.675	5.011	998.400	1.90	19.90	17.70	0.89	57565	11.4884	0.030	719510	143.8251	-0.160	28.4557	28.4557	-1.213	-0.100	0.027	-0.159						
02.03.2018	60	301.288	59.733	59.835	4998.796	5.007	998.300	1.86	20.00	17.80	0.89	57528	11.4888	0.033	718996	143.8338	-0.154	28.4512	28.4512	-1.211	0.000	0.031	-0.151						
02.03.2018	60	302.564	59.721	59.823	5019.278	5.028	998.300	1.90	20.10	17.90	0.89	57764	11.4889	0.034	721811	143.8077	-0.172	28.4463	28.4463	-1.228	0.100	0.032	-0.168						
02.03.2018	100	300.803	95.812	95.994	8005.691	8.021	998.100	0.26	20.60	18.50	0.89	91917	11.4596	-0.221	1151390	143.8214	-0.163	28.7912	28.7912	-0.031	0.600	-0.220	-0.153						
02.03.2018	100	301.012	94.659	94.849	7914.889	7.931	998.000	0.26	20.80	18.80	0.88	90850	11.4554	-0.258	1138250	143.8112	-0.170	28.7866	28.7866	-0.047	0.800	-0.256	-0.158						
02.03.2018	100	300.766	94.631	94.821	7906.057	7.922	998.000	0.26	20.90	18.90	0.88	90771	11.4582	-0.233	1137250	143.8654	-0.146	28.7954	28.7954	-0.016	0.900	-0.231	-0.133						
02.03.2018	100	300.665	94.971	95.152	7931.785	7.947	998.100	0.26	21.00	19.10	0.88	91020	11.4535	-0.274	1140720	143.8663	-0.166	28.7876	28.7876	-0.041	1.000	-0.271	-0.152						
02.03.2018	100	302.445	95.048	95.229	7985.202	8.000	998.100	0.27	21.10	19.20	0.88	91669	11.4580	-0.235	1148100	143.7953	-0.193	28.7841	28.7841	-0.055	1.100	-0.232	-0.177						



INTI Laboratory – Day#1

Data report INTI. Day#1										*Original data set										Temperature correction of meter error											
Date	Nominal flowrate	V <sub>nom</sub> [m³/h]	Measur-ment time [s]	Laboratory reference				Fluid				Ambient conditions				Turbine meter				Coriolis_Mass				Coriolis_Vol				Corrected meter error			
				Standard mass flowrate [t/h]	Standard volume flowrate [m³/h]	V <sub>ref</sub> [m³/h]	M <sub>ref</sub> [kg]	Volume [m³]	Water density [kg/m³]	Line pressure [bar]	Water temp. [°C]	Air temp. [°C]	Air pressure [bar]	Pulse count	K-factor [Pulses/Liter]	Meter error [%]	e <sub>v</sub> [%]	K <sub>m</sub> [Pulses/kg]	K-factor	Meter error [%]	e <sub>m</sub> [%]	Pulse count	K-factor	Meter error [%]	e <sub>v</sub> [%]	K <sub>v</sub> [Pulses/Liter]	K-factor	Meter error [%]	e <sub>v</sub> [%]	(T <sub>fluid</sub> - T <sub>nom</sub> ) [°C]	ΔT <sub>fluid</sub> [°C]
06.12.2018	10	343.780	10.481	10.502	1000.888	1.003	998.024	21.40			11478	11.4452	-0.347	144032	143.9042	-0.105	28776	28.6936	-0.369	1.400	-0.375	-0.086									
06.12.2018	10	344.540	10.465	10.487	1001.603	1.004	997.979	21.60			11453	11.4116	-0.639	144061	143.8304	-0.157	28781	28.6769	-0.428	1.600	-0.668	-0.135									
06.12.2018	10	344.770	10.451	10.472	1000.904	1.003	997.979	21.60			11463	11.4195	-0.570	143878	143.7480	-0.214	28746	28.6620	-0.479	1.600	-0.599	-0.192									
06.12.2018	10	344.930	10.442	10.463	1000.505	1.003	997.979	21.60			11484	11.4550	-0.261	143965	143.8923	-0.114	28764	28.6914	-0.377	1.600	-0.290	-0.092									
06.12.2018	10	345.160	10.437	10.458	1000.655	1.003	997.979	21.60			11489	11.4683	-0.233	143974	143.8798	-0.122	28765	28.6881	-0.389	1.600	-0.261	-0.101									
06.12.2018	30	126.960	28.463	28.521	1003.799	1.006	997.979	21.60			11612	11.5447	0.520	144460	143.9133	-0.099	28756	28.5893	-0.732	1.600	0.518	-0.078									
06.12.2018	30	123.900	29.211	29.270	1005.346	1.007	997.979	21.60			11613	11.5279	0.374	144630	143.8609	-0.135	28790	28.5790	-0.767	1.600	0.372	-0.114									
06.12.2018	30	124.330	29.041	29.099	1002.950	1.005	997.979	21.60			11593	11.5355	0.440	144339	143.9144	-0.098	28723	28.5806	-0.762	1.600	0.438	-0.077									
06.12.2018	30	119.440	30.194	30.270	1001.785	1.004	997.512	23.60			11593	11.5355	0.510	144250	143.9930	-0.044	28745	28.6224	-0.617	3.600	0.523	0.003									
06.12.2018	30	124.490	29.017	29.077	1003.414	1.005	997.934	21.80			11603	11.5396	0.476	144391	143.8997	-0.108	28746	28.5890	-0.733	1.800	0.475	-0.085									
06.12.2018	60	61.000	58.931	59.058	998.553	1.001	997.843	22.20			11529	11.5208	0.312	143741	143.9493	-0.074	28572	28.5517	-0.862	2.200	0.325	-0.045									
06.12.2018	60	59.330	60.732	60.863	1000.898	1.003	997.843	22.20			11552	11.5167	0.276	144048	143.9188	-0.095	28533	28.4459	-1.229	2.200	0.290	-0.066									
06.12.2018	60	59.340	60.897	61.025	1003.779	1.006	997.889	22.00			11581	11.5130	0.244	144616	144.0716	0.011	28510	28.3427	-1.588	2.000	0.256	0.037									
06.12.2018	60	59.950	59.923	60.050	997.880	1.000	997.889	22.00			11514	11.5140	0.252	143568	143.8716	-0.128	28444	28.4440	-1.236	2.000	0.264	-0.102									
06.12.2018	60	59.490	60.696	60.827	1002.994	1.005	997.843	22.20			11581	11.5215	0.318	144296	143.8652	-0.132	28582	28.4352	-1.267	2.200	0.331	-0.104									
06.12.2018	100	184.580	98.414	98.638	5045.900	5.057	997.727	22.70			58342	11.5360	0.444	729652	144.6030	0.380	146282	28.9244	-0.482	2.700	0.455	0.415									
06.12.2018	100	182.550	99.536	99.763	5047.319	5.059	997.727	22.70			58375	11.5393	0.472	729959	144.6231	0.394	146340	28.9277	-0.443	2.700	0.484	0.429									
06.12.2018	100	184.360	98.524	98.748	5045.513	5.057	997.727	22.70			58342	11.5369	0.452	729612	144.6061	0.382	146270	28.9242	-0.431	2.700	0.463	0.417									
06.12.2018	100	183.230	99.160	99.386	5046.979	5.058	997.727	22.70			58365	11.5381	0.462	729922	144.6255	0.395	146317	28.9251	-0.434	2.700	0.473	0.430									
06.12.2018	100	184.380	98.529	98.753	5046.312	5.058	997.727	22.70			58349	11.5364	0.448	729666	144.5939	0.373	146289	28.9234	-0.428	2.700	0.459	0.408									
06.12.2018	130	142.260	128.199	128.494	5065.995	5.078	997.704	22.80			58505	11.5221	0.323	731943	144.4816	0.295	146578	28.8673	-0.234	2.800	0.334	0.332									
06.12.2018	130	141.790	128.616	128.912	5065.668	5.077	997.704	22.80			58449	11.5118	0.233	731882	144.4789	0.294	146341	28.8224	-0.078	2.800	0.245	0.330									
06.12.2018	130	142.500	127.946	128.240	5064.514	5.076	997.704	22.80			58484	11.5213	0.316	731651	144.4662	0.285	146530	28.8663	-0.230	2.800	0.327	0.321									
06.12.2018	130	142.440	128.022	128.297	5064.610	5.076	997.704	22.80			58488	11.5219	0.321	731749	144.4828	0.296	146451	28.8501	-0.174	2.800	0.332	0.333									
06.12.2018	130	140.760	129.535	129.833	5064.805	5.076	997.704	22.80			58485	11.5208	0.312	731761	144.4796	0.294	146649	28.8880	-0.306	2.800	0.323	0.330									

INTI Laboratory – Day#2

Date	Nominal flowrate V <sub>nom</sub> [m <sup>3</sup> /h]	Laboratory reference							Fluid			Ambient conditions			Turbine meter			Coriolis_Mass			Coriolis_Vol			Temperature correction of meter error																				
		Measur- ement time [s]	Standard mass flowrate [t/h]	Standard volume flowrate [m <sup>3</sup> /h]	Mass m <sub>ref</sub> [kg]	Volume V <sub>ref</sub> [m <sup>3</sup> ]	Water density ρ <sub>fluid</sub> [kg/m <sup>3</sup> ]	Water temp. T <sub>fluid</sub> [°C]	Line pressure P <sub>fluid</sub> [bar]	Water temp. T <sub>air</sub> [°C]	Air temp. T <sub>air</sub> [°C]	Air pressure P <sub>air</sub> [bar]	K <sub>V,nom</sub>	K-factor	Meter error	Pulses/ liter	K <sub>m,nom</sub>	K-factor	Meter error	Pulse count	N	ρ <sub>m</sub> [Pulses/kg]	ρ <sub>m</sub> [%]	ε <sub>m</sub> [Pulses/Liter]	ε <sub>m</sub> [%]	K <sub>V,nom</sub>	K-factor	Meter error	Pulses/ liter	K <sub>V,nom</sub>	K-factor	Meter error	Pulse count	N	ρ <sub>v</sub> [Pulses/Liter]	ρ <sub>v</sub> [%]	ε <sub>v</sub> [Pulses/Liter]	ε <sub>v</sub> [%]	(T <sub>fluid</sub> - T <sub>nom</sub> )	ΔT <sub>fluid</sub> [°C]	Corrected meter error	Coriolis _Mass	Coriolis _Vol	T <sub>nom</sub> [°C]
		t	m <sup>3</sup> ref	V <sup>3</sup> ref	m <sup>3</sup> ref	V <sup>3</sup> ref	ρ <sup>3</sup> fluid	T <sup>3</sup> fluid	P <sup>3</sup> fluid	T <sup>3</sup> air	T <sup>3</sup> air	P <sup>3</sup> air	K <sub>V,nom</sub>	K-factor	error	Pulses/Liter	K <sub>m,nom</sub>	K-factor	error	Pulse count	N	ρ <sub>m</sub> [%]	ρ <sub>m</sub> [%]	ε <sub>m</sub> [Pulses/Liter]	ε <sub>m</sub> [%]	K <sub>V,nom</sub>	K-factor	error	Pulses/Liter	K <sub>V,nom</sub>	K-factor	error	Pulse count	N	ρ <sub>v</sub> [Pulses/Liter]	ρ <sub>v</sub> [%]	ε <sub>v</sub> [Pulses/Liter]	ε <sub>v</sub> [%]	(T <sub>fluid</sub> - T <sub>nom</sub> )	ΔT <sub>fluid</sub> [°C]	Corrected meter error	Coriolis _Mass	Coriolis _Vol	T <sub>nom</sub> [°C]
12.12.2018	10	367.640	9.794	9.817	1000.202	1.003	997.656	23.00	11.4647	-0.176	143824	143.7949	-0.181	28767	28.6938	-0.369	3.000	0.211	-0.133																									
12.12.2018	10	366.630	9.810	9.833	998.055	1.001	997.656	23.00	11.5129	0.243	143673	143.8089	-0.172	28735	28.6948	-0.365	3.000	0.211	-0.133																									
12.12.2018	10	368.130	9.784	9.808	1000.457	1.003	997.536	23.50	11.5033	0.159	143871	143.8053	-0.174	28772	28.6880	-0.389	3.500	0.128	-0.129																									
12.12.2018	10	367.430	9.794	9.819	999.659	1.002	997.536	23.50	11.5185	0.292	143741	143.7901	-0.185	28750	28.6889	-0.386	3.500	0.260	-0.139																									
12.12.2018	10	367.600	9.798	9.822	1000.457	1.003	997.536	23.50	11.5193	0.298	143738	143.6724	-0.266	28751	28.6671	-0.462	3.500	0.267	-0.221																									
12.12.2018	30	116.370	30.906	30.975	999.030	1.001	997.751	22.60	11.5492	0.559	143747	143.8866	-0.118	28630	28.5933	-0.718	2.600	0.564	-0.094																									
12.12.2018	30	116.280	30.786	30.855	994.390	0.997	997.751	22.60	11.6051	1.046	143257	144.0652	0.006	28494	28.5903	-0.728	2.600	1.051	0.040																									
12.12.2018	30	117.920	30.501	30.570	998.080	1.001	997.751	22.60	11.5476	0.545	143687	143.8194	-0.164	28619	28.5809	-0.761	2.600	0.550	-0.130																									
12.12.2018	30	116.740	30.794	30.863	998.581	1.001	997.751	22.60	11.5524	0.587	143642	143.8462	-0.146	28608	28.5842	-0.749	2.600	0.592	-0.112																									
12.12.2018	30	116.760	30.739	30.809	996.984	0.999	997.751	22.60	11.5489	0.556	143435	143.8689	-0.130	28677	28.5880	-0.733	2.600	0.561	-0.096																									
12.12.2018	60	60.310	59.929	60.067	1003.982	1.006	997.704	22.80	11.5404	0.482	145209	144.6330	0.401	28698	28.5185	-0.977	2.800	0.500	0.437																									
12.12.2018	60	60.100	60.010	60.148	1001.837	1.004	997.704	22.80	11.5362	0.446	144150	143.8857	-0.118	28560	28.4422	-1.242	2.800	0.463	-0.082																									
12.12.2018	60	60.970	58.954	59.089	998.444	1.001	997.704	22.80	11.5674	0.718	143692	143.9159	-0.097	28469	28.4479	-1.223	2.800	0.735	-0.061																									
12.12.2018	60	60.290	59.988	60.126	1004.631	1.007	997.704	22.80	11.5409	0.486	144603	143.9365	-0.083	28641	28.4435	-1.238	2.800	0.504	-0.047																									
12.12.2018	60	60.260	59.631	59.771	998.157	1.001	997.656	23.00	11.5592	0.646	143721	143.9864	-0.048	28461	28.4467	-1.227	3.000	0.665	-0.009																									
12.12.2018	100	183.880	98.765	99.019	5044.978	5.058	997.438	23.90	11.5399	0.478	729758	144.6504	0.413	146346	28.9339	0.465	3.900	0.495	0.463																									
12.12.2018	100	181.730	99.963	100.220	5046.204	5.059	997.438	23.90	11.5402	0.481	730018	144.6668	0.424	146388	28.9352	0.469	3.900	0.498	0.474																									
12.12.2018	100	183.710	98.849	99.098	5044.338	5.057	997.487	23.70	11.5384	0.465	729575	144.6325	0.400	146308	28.9315	0.457	3.700	0.481	0.448																									
12.12.2018	100	183.530	98.968	99.219	5045.424	5.058	997.463	23.80	11.5386	0.466	729777	144.6315	0.399	146340	28.9309	0.455	3.800	0.483	0.449																									
12.12.2018	100	183.360	99.045	99.302	5044.684	5.058	997.413	24.00	11.5363	0.447	729632	144.6338	0.401	146320	28.9298	0.451	4.000	0.465	0.453																									
12.12.2018	130	142.300	128.113	128.445	5064.024	5.077	997.413	23.90	11.5242	0.341	731734	144.4965	0.306	146358	28.8268	0.093	3.900	0.357	0.356																									
12.12.2018	130	143.210	127.250	127.580	5062.080	5.075	997.413	23.90	11.5241	0.340	731423	144.4906	0.302	146328	28.8319	0.111	3.900	0.356	0.352																									
12.12.2018	130	143.510	127.019	127.349	5063.490	5.077	997.413	23.70	11.5222	0.324	731630	144.4913	0.302	146461	28.8501	0.174	3.700	0.340	0.350																									
12.12.2018	130	143.150	127.351	127.681	5063.970	5.077	997.413	23.80	11.5192	0.297	731587	144.4691	0.287	146494	28.8539	0.187	3.800	0.313	0.336																									
12.12.2018	130	142.280	128.129	128.461	5063.924	5.077	997.413	24.00	11.5224	0.326	731609	144.4747	0.291	146587	28.8724	0.252	4.000	0.342	0.342																									





CENAM Laboratory – Day#2

Data report CENAM: Day#2											*Original dataset															
Date	Nominal flowrate	Laboratory reference			Fluid			Ambient conditions			Turbine meter			Coriolis_Mass			Coriolis_Vol			Correction of autozoero at Coriolis meter			Temperature correction of meter error			
		Meas-urament time	Standard mass flowrate	Standard volume flowrate	Mass	Volume	Water density	Line pressure	Water temp.	Air temp.	Air pressure	Pulse count	K-factor	$K_{vol}$	Pulse count	$K_m$	Pulse count	$K_v$	Meter error	$e_m$	Meter error	$e_v$	Corrected meter error	Corrected meter error	$(T_{fluid} - T_{nom})$	$\Delta T_{fluid}$
04.06.2019	10	423.087	10.099	10.128	1186.877	1.190	997.136	2.89	27.19	25.40	0.81	170629	143.7630	-0.203	34251	28.7754	-0.085	7.190	-0.095	-0.024						
04.06.2019	10	422.992	10.088	10.117	1185.906	1.189	997.128	2.90	27.22	25.40	0.81	170304	143.7443	-0.216	34201	28.7713	-0.100	7.220	-0.073	-0.036						
04.06.2019	10	423.082	10.083	10.112	1184.956	1.188	997.122	2.90	27.24	25.40	0.81	170078	143.7218	-0.232	34186	28.7670	-0.115	7.240	-0.110	-0.051						
04.06.2019	10	422.985	10.057	10.086	1181.634	1.185	997.106	2.90	27.30	25.60	0.81	169801	143.7002	-0.247	34084	28.7613	-0.134	7.300	-0.095	-0.065						
04.06.2019	30	1278.094	30.255	30.342	1496.709	1.501	997.118	2.93	27.26	25.90	0.81	214848	143.8613	-0.135	42940	28.6689	-0.455	7.260	22.552	-0.002						
04.06.2019	30	1279.000	30.206	30.293	1493.438	1.498	997.115	2.92	27.27	26.00	0.81	213736	143.8577	-0.138	42724	28.6730	-0.441	7.270	22.966	-0.010						
04.06.2019	30	176.998	30.399	30.487	1494.618	1.499	997.112	2.93	27.28	26.10	0.81	216999	143.8488	-0.144	42966	28.6641	-0.472	7.280	22.607	-0.019						
04.06.2019	30	178.022	30.042	30.129	1485.605	1.490	997.110	2.93	27.29	26.10	0.81	213640	143.8417	-0.149	42717	28.6708	-0.449	7.290	24.094	-0.023						
04.06.2019	60	89.154	59.962	60.136	1484.959	1.489	997.107	2.88	27.29	26.10	0.81	213635	143.8693	-0.130	42426	28.4878	-1.084	7.290	3.937	-0.018						
04.06.2019	60	89.011	60.058	60.232	1484.939	1.489	997.108	2.89	27.29	26.10	0.81	213474	143.8679	-0.131	42424	28.4869	-1.087	7.290	4.237	-0.019						
04.06.2019	60	88.923	60.074	60.248	1483.868	1.488	997.108	2.89	27.29	26.20	0.81	213187	143.8677	-0.131	42337	28.4880	-1.083	7.310	3.858	-0.019						
04.06.2019	60	89.000	59.999	60.113	1481.827	1.486	997.102	2.88	27.31	26.20	0.81	213124	143.8659	-0.132	42321	28.4853	-1.093	7.310	3.641	-0.020						
04.06.2019	100	53.096	100.648	100.941	1484.436	1.489	997.092	2.73	27.32	26.20	0.81	213523	143.8442	-0.149	42968	28.8615	0.214	7.320	1.148	-0.043						
04.06.2019	100	53.031	100.376	100.669	1478.614	1.483	997.087	2.73	27.34	26.30	0.81	212665	143.8273	-0.159	42797	28.8597	0.207	7.340	1.340	-0.052						
04.06.2019	100	52.974	100.327	100.620	1476.513	1.481	997.090	2.73	27.33	26.40	0.81	212359	143.8442	-0.147	42724	28.8554	0.192	7.350	1.304	-0.040						
04.06.2019	100	52.997	100.354	100.648	1477.342	1.482	997.084	2.73	27.35	26.60	0.81	212504	143.8421	-0.149	42724	28.8562	0.230	7.350	1.286	-0.042						
04.06.2019	130	275.081	129.521	129.913	989.687	9.927	996.984	2.64	27.69	26.89	0.81	1423794	143.8631	-0.134	286598	28.8711	-0.247	7.690	1.072	-0.024						
04.06.2019	130	274.895	129.389	129.781	988.678	9.914	996.980	2.61	27.70	26.80	0.81	1421875	143.8669	-0.135	286210	28.8704	0.244	7.700	1.084	-0.025						
04.06.2019	130	275.080	129.595	129.988	990.673	9.931	996.975	2.62	27.72	26.80	0.81	1424243	143.8531	-0.141	286669	28.8665	0.231	7.720	1.017	-0.030						
04.06.2019	130	275.079	129.563	129.957	989.972	9.930	996.964	2.61	27.76	26.80	0.81	1424136	143.8525	-0.141	286657	28.8674	0.234	7.760	1.137	-0.030						
04.06.2019	150	237.837	150.047	150.510	992.950	9.960	996.926	2.53	27.88	26.70	0.81	1428696	143.8818	-0.121	287621	28.8768	0.267	7.880	0.854	-0.009						
04.06.2019	150	237.813	150.017	150.481	990.959	9.941	996.915	2.48	27.91	26.80	0.81	1425824	143.8779	-0.124	287052	28.8767	0.266	7.910	0.865	-0.011						
04.06.2019	150	237.897	150.021	150.486	991.957	9.949	996.910	2.50	27.93	26.80	0.81	1426969	143.8773	-0.124	287252	28.8733	0.255	7.930	0.766	-0.011						
04.06.2019	150	237.996	149.777	150.243	990.162	9.933	996.898	2.48	27.97	26.80	0.81	1424566	143.8699	-0.129	286741	28.8688	0.239	7.970	0.833	-0.016						
04.06.2019	150	238.000	150.007	150.475	991.718	9.948	996.893	2.49	27.99	26.80	0.81	1426877	143.8796	-0.122	287236	28.8735	0.255	7.990	0.822	-0.009						





PTB Laboratory – Day#1

Data report PTB: Day#1		*Original dataset										Correction of Coriolis meter										Temperature correction of meter error									
Date	Nominal flowrate	Meas. repeat time	Laboratory reference			Fluid			Ambient conditions			Turbine meter			Coriolis_Mass			Coriolis_Vol			Corrected meter error			Corrected meter error							
			$V_{ref}$	$m_{ref}$	$V_{ref}$	$\rho_{fluid}$	$P_{fluid}$	$T_{fluid}$	$T_{air}$	$P_{air}$	$K_{T,ref}$	$K_{V,ref}$	$\epsilon_m$	$K_{C,ref}$	$K_{V,ref}$	$\epsilon_m$	$\Delta T_{fluid}$	$\epsilon_{Cor,M}$	$\epsilon_{Cor,V}$	$\Delta T_{fluid}$	$\epsilon_{Cor,M}$	$\epsilon_{Cor,V}$									
08.08.2019	10	972.108	10.667	10.084	2718.304	2.723	998.311	3.00	20.01	22.25	1.00	31275	11.4859	0.007	392944	144.5548	0.346	0.008	-0.008	-0.014	0.048										
08.08.2019	10	972.106	9.966	9.883	2691.085	2.696	998.313	3.00	20.00	22.28	1.00	30957	11.4841	-0.008	389143	144.6045	0.381	0.000	0.000	-0.090	0.079										
08.08.2019	10	972.132	9.966	9.963	2685.814	2.690	998.314	3.00	20.00	22.32	1.00	30856	11.4840	-0.010	382935	144.5726	0.359	0.000	0.000	-0.091	0.057										
08.08.2019	10	972.109	10.008	10.025	2702.589	2.707	998.314	3.00	20.00	22.32	1.00	31090	11.4844	-0.006	390767	144.5899	0.371	0.000	-0.005	-0.027	0.071										
08.08.2019	10	972.132	10.006	10.023	2701.974	2.707	998.312	3.00	20.00	22.36	1.00	31083	11.4844	-0.006	390701	144.5884	0.377	0.000	0.001	-0.027	0.076										
08.08.2019	30	324.129	30.191	30.242	2718.290	2.723	998.312	2.99	20.00	22.47	1.00	31316	11.5010	0.139	391908	144.1745	0.082	0.005	0.005	0.128	-0.015										
08.08.2019	30	324.111	30.068	30.119	2707.026	2.712	998.314	3.01	19.99	22.49	1.00	31184	11.5002	0.132	390287	144.1746	0.083	-0.009	-0.009	0.121	-0.015										
08.08.2019	30	324.114	30.068	30.108	2706.142	2.711	998.313	3.01	20.00	22.50	1.00	31175	11.5007	0.135	390157	144.1746	0.082	-0.002	-0.002	0.124	-0.016										
08.08.2019	30	324.111	29.986	30.037	2699.682	2.704	998.313	3.02	20.00	22.51	1.00	31101	11.5008	0.137	389263	144.1885	0.082	0.000	0.000	0.126	-0.006										
08.08.2019	30	324.109	30.064	30.105	2705.784	2.710	998.312	3.01	20.00	22.53	1.00	31172	11.5011	0.139	390114	144.1778	0.085	0.004	0.004	0.128	-0.013										
08.08.2019	60	162.117	60.213	60.315	2711.537	2.716	998.298	3.00	20.02	22.53	1.00	31244	11.5031	0.157	390869	144.0839	0.019	0.023	0.023	0.155	-0.028										
08.08.2019	60	162.094	59.890	59.992	2696.594	2.701	998.296	3.01	20.08	22.55	1.00	31071	11.5027	0.153	388548	144.0885	0.023	0.080	0.080	0.151	-0.024										
08.08.2019	60	162.137	60.129	60.231	2708.110	2.713	998.311	3.00	20.01	22.55	1.00	31204	11.5030	0.156	390265	144.1097	0.037	0.006	0.006	0.153	-0.010										
08.08.2019	60	162.095	60.267	60.369	2713.620	2.718	998.310	2.98	20.01	22.57	1.00	31268	11.5031	0.157	391053	144.1075	0.036	0.011	0.011	0.155	-0.012										
08.08.2019	60	162.113	59.771	59.872	2691.568	2.696	998.312	3.02	20.00	22.59	1.00	31013	11.5028	0.154	387857	144.1008	0.031	0.002	0.002	0.152	-0.017										
08.08.2019	100	97.319	99.872	100.043	2699.848	2.704	998.294	3.00	20.09	22.58	1.00	31110	11.5032	0.158	388982	144.0755	0.014	0.091	0.091	0.155	-0.013										
08.08.2019	100	97.318	100.282	100.453	2710.884	2.716	998.294	2.99	20.09	22.61	1.00	31239	11.5038	0.163	390591	144.0820	0.018	0.089	0.089	0.161	-0.008										
08.08.2019	100	97.339	100.416	100.587	2715.092	2.720	998.294	3.02	20.09	22.63	1.00	31287	11.5037	0.162	391202	144.0842	0.020	0.089	0.089	0.160	-0.007										
08.08.2019	100	97.339	100.440	100.612	2715.759	2.720	998.294	2.99	20.09	22.63	1.00	31293	11.5031	0.157	391300	144.0849	0.020	0.089	0.089	0.154	-0.006										
08.08.2019	100	97.319	100.778	100.950	2724.331	2.729	998.293	2.99	20.10	22.62	1.00	31394	11.5039	0.164	392532	144.0838	0.019	0.086	0.086	0.161	-0.007										
08.08.2019	130	74.860	131.330	131.550	2730.918	2.736	998.290	2.95	20.11	22.67	1.00	31476	11.5061	0.183	393472	144.0805	0.017	0.108	0.108	0.182	-0.002										
08.08.2019	130	74.883	131.988	132.214	2745.437	2.750	998.289	2.93	20.11	22.69	1.00	31643	11.5059	0.182	395589	144.0895	0.023	0.000	0.000	0.181	0.004										
08.08.2019	130	74.905	128.615	128.836	2676.072	2.681	998.289	2.99	20.11	22.70	1.00	30844	11.5061	0.183	385562	144.0776	0.015	0.113	0.113	0.183	-0.005										
08.08.2019	130	74.882	128.951	129.172	2682.238	2.687	998.289	3.01	20.11	22.69	1.00	30915	11.5061	0.183	386472	144.0857	0.021	0.113	0.113	0.183	0.001										
08.08.2019	130	74.883	128.900	129.121	2681.206	2.686	998.288	3.01	20.12	22.69	1.00	30993	11.5061	0.182	386328	144.0874	0.022	0.117	0.117	0.182	0.002										



